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USER'S MANUAL

FOR

A COMPUTER PROGRAM FOR THE
EMULATION/SIMULATION OF A SPACE STATION
ENVIRONMENTAL CONTROL AND LIFE SUPPORT SYSTEM
(ESCM)

BY

HAMILTON STANDARD
DIVISION OF UNITED TECHNOLOGIES CORPORATION
WINDSOR LOCKS, CONNECTICUT
PREPARED UNDER CONTRACT NO. NAS 1-17397

FOR

NATIONAL AERONAUTICS AND SPACE ADMINISTRATION
LANGLEY RESEARCH CENTER
HAMPTON, VIRGINIA

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COMPUTER PROGRAM FOR THE
EMULATION/SIMULATION OF A SPACE STATION
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SYSTEM (ESCM) (Hamilton Standard Div.)

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ABSTRACT

This manual describes how to use the Emulation/Simulation Computer Model, ESCM. Based on G189A, ESCM computes the transient performance of a Space Station atmospheric revitalization subsystem (ARS) with CO₂ removal provided by a solid amine water desorbed subsystem called SAWD. Many performance parameters are computed some of which are cabin CO₂ partial pressure, relative humidity, temperature, O₂ partial pressure, and dew point. The program allows the user to simulate various possible combinations of man loading, metabolic profiles, cabin volumes and certain hypothesized failures that could occur.

FOREWARD

This User's Manual has been prepared by Hamilton Standard, Division of United Technologies Corporation for the National Aeronautics and Space Administration's Langley Research Center in accordance with Contract NAS 1-17397, "Development of an Emulation/Simulation Computer Model of a Space Station Environmental Control and Life Support System (ECLSS)". This manual describes the use of the computer model.

Appreciation is expressed to the Technical Monitors Messrs. John B. Hall, Jr. and Lawrence F. Rowell of the NASA Langley Research Center for their guidance and advice.

This manual was prepared by Mr. James L. Yanosy, Program Engineer. The program was conducted under the direction of Mr. Harlan Brose, Program Manager and Mr. Albert Boehm, Assistant Program Manager. Special thanks is given to Mr. Gordon Allen for his contributions to the development of the analytical model of the Solid Amine Water Desorbed process. Thanks are also extended to Messrs. Raymond Trusch and Edward O'Connor for their assistance and technical advice.

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1.0 INTRODUCTION

1.1 Background

ESCM is a computer model which was developed to demonstrate the utility of a major portion of the Emulation/Simulation, Sizing, and Technology Assessment Program (ESSTAP). See Reference 1. ESSTAP is a concept for software tools that will support the total engineering process of the Space Station beginning with concept definition and continuing on through mission operations. The interaction of the software tools with the design and operational phases of a flight system is shown in Figure 1. The philosophy of this software concept is to have the analysis software for each step in the design process precede development of hardware in order to provide the greatest design and cost benefits.

Of the many systems in the Space Station, the Environmental Control and Life Support System (ECLSS) was selected to demonstrate the utility of the ESSTAP concept because of its complexity (number of components and dynamic operational capability), availability of operational data for checkout, and growth potential. The ESCM program was targeted to evaluate and demonstrate the benefits of phases 2 through 4 software. For this purpose, an evaluation of the six major ECLSS functions was performed as published in the program document "ESCM-EM-02". As a result of this study, a subgroup of the Air Revitalization Subsystem (ARS) shown in Figure 2 was selected for modelling because of its dynamic complexity, growth potential, design tool utility, and the independent nature of the ARS compared to other subsystems.

The resulting ESCM model has been used to demonstrate the use of a computer program in the design, development, and test of applicable development hardware. Specifically, through the use of the program, design hardware and software can be verified, Failure Mode and Effect Analysis (FMEA) can be assisted, and test planning can be technically improved.

1.2 Computer Program Overview

The ESCM Computer Program consists of five parts, as shown in Figure 3. Like a generalized heat transfer program, ESCM uses the G189A framework to set up the input data, uses the G189A subroutine library for models of many of the components, and lastly, uses the G189A executive routines to take the input data and component subroutines and compute the solution. However, particular to the ESCM program are: (1) the GPOLY1 and GPOLY2 subroutines which

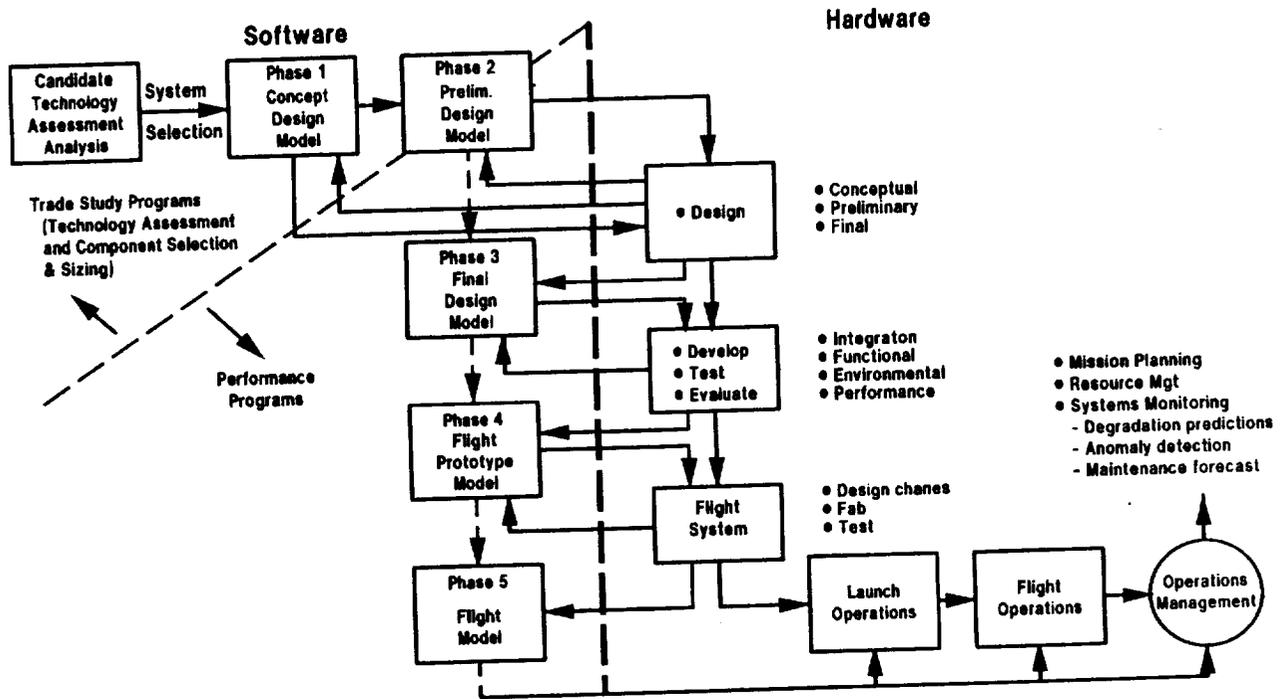


Figure 1
 Application Of Software Tools To The Design
 And Operational Phases Of A Flight System

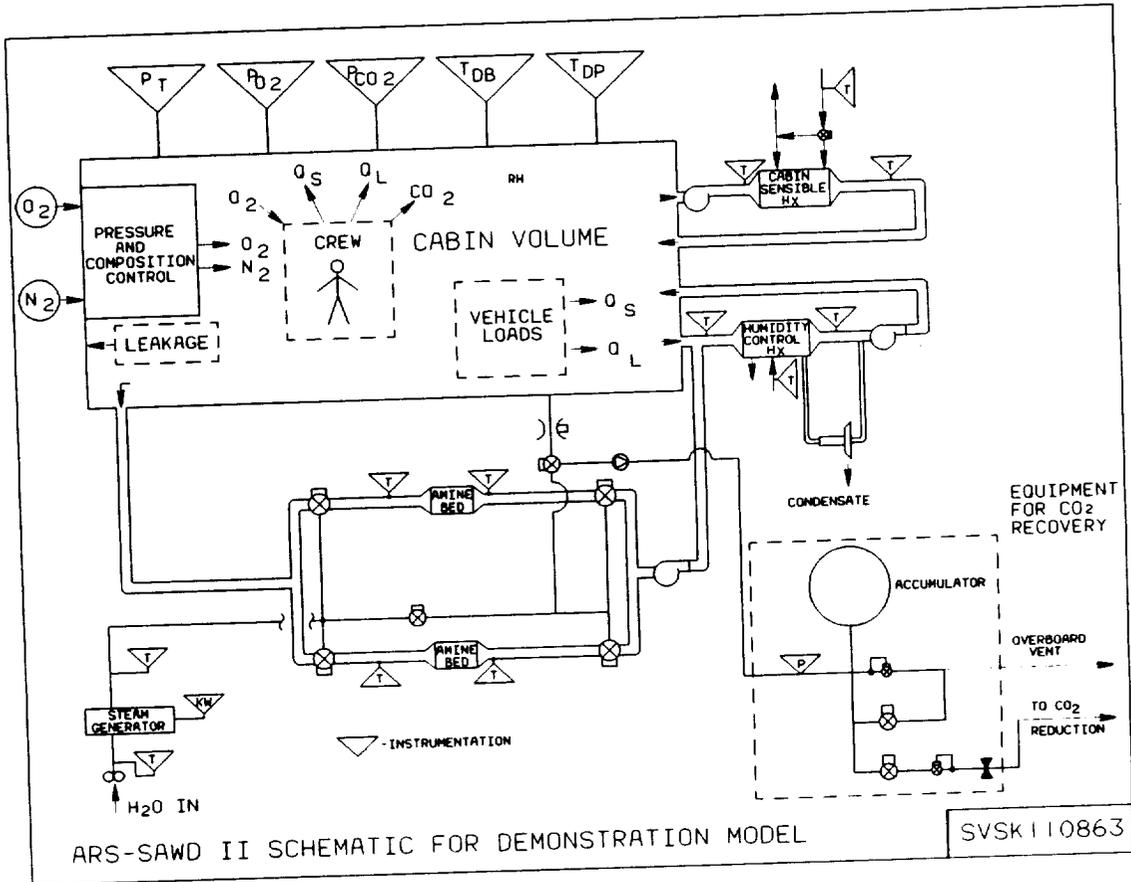


Figure 2
 ARS - SAWD II Schematic For Demonstration Model

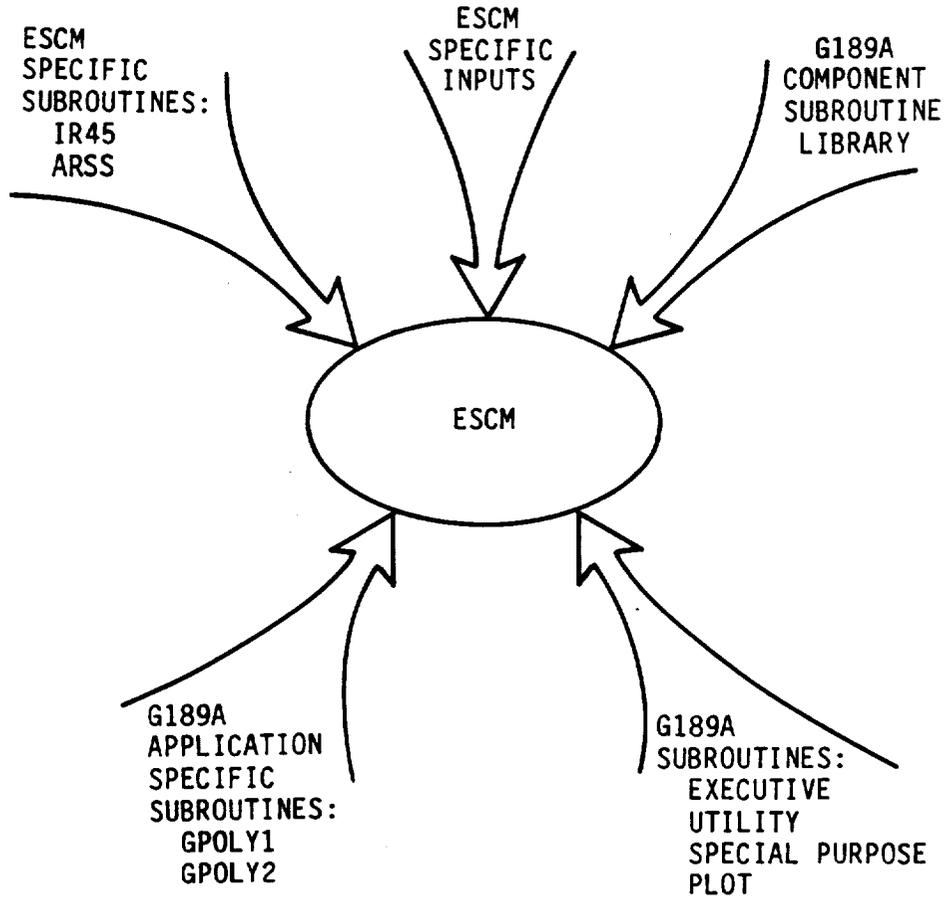


Figure 3
Overview Of ESCM Computer Program



1.2 Computer Program Overview (Continued)

define the control logic for the ARS subgroup, (2) the newly developed component subroutine for the Solid Amine Water Desorbed (SAWD) bed, (3) the ARS subroutine which provides computer generated schematics of the ARS subgroup with important performance parameters and tabular printoff to a terminal screen for interactive operation, and (4) the input data file which defines the ARS subgroup for G189A and which contains many performance constants and input parameters.

ESCM starts with input data which defines the ARS subgroup components and plumbing and combines this data with various program options. Typical input parameters are:

- | | |
|-----------------------|-------------------------|
| (1) Number of men | (4) Equipment heat load |
| (2) Cabin volume | (5) Cabin leakage |
| (3) Cabin temperature | (6) Metabolic profiles |

ESCM then solves each of the components in turn per the sequence specified by the user. After all components have been solved for a particular time step, typical performance parameters are displayed to the screen and a schematic of the ARS subgroup is saved for a hardcopy printoff. Of course, the user may select the frequency of printoff. Typical computed performance parameters are:

- (1) Cabin CO₂ mmHg
- (2) Cabin O₂ Partial pressure
- (3) Cabin relative humidity
- (4) Cabin temperature
- (5) Cabin total pressure

After the display to the screen, the time step is incremented, GPOLY1 is solved, all the component subroutines are solved again per the specified sequence, GPOLY2 is solved, and lastly ARS subroutine is invoked to display and save important performance parameters. The process is repeated until the time specified by the user is reached.

2.0 DESCRIPTION OF HARDWARE AND MODEL

ESCM is a computer program which emulates/simulates a Space Station Environmental Control and Life Support System (ECLSS). To demonstrate its utility only a portion of the ECLSS had to be modeled. The portion modeled is a subgroup of the ARS and is shown in Figure 2. This section will provide a description of the system to be modeled and give a description of the ESCM computer program.

2.1 Description of System to be Modeled

As stated above, the system modeled is a subgroup of the atmospheric revitalization subsystem. The major elements are the cabin, the crew, a sensible heat exchanger, a humidity control heat exchanger, fans, a SAWD carbon dioxide removal system, and a two gas controller.

The cabin is a volume of user specified size which houses the crew, two gas controller, and certain user specified vehicle loads representative of test equipment. The user may also specify air leakage out of the cabin.

The crew of user specified size and metabolic loading breathes in oxygen from the cabin air and releases carbon dioxide and water vapor. The crew also gives off sensible heat to the cabin air.

Cabin air is drawn off by one fan to pass the air through a heat exchanger which removes sensible heat from the air. In the heat exchanger, the air gives off its heat to coolant water which enters the heat exchanger at a user specified temperature. The cabin air temperature controller will control the flow of water to maintain the desired cabin air temperature. The heat exchanger is a plate-fin type similar to that on the Shuttle.

Another fan is used to draw air from the cabin to send it in turn to a humidity control heat exchanger. Air in this heat exchanger loses its heat to coolant water which enters the heat exchanger at a user specified flow and temperature. Water vapor in the air is condensed in this heat exchanger. A portion of the main air stream with condensed vapor is sent to a water separator where the condensed vapor is removed. This humidity control heat exchanger also receives air flow directly from the SAWD carbon dioxide removal system. Thus the effect of any moisture from the SAWD system on cabin relative humidity is lessened.

The last fan draws air from the cabin for use by the SAWD carbon dioxide removal system. This carbon dioxide removal system contains two amine beds, solenoid valves, an accumulator, a water pump, steam generator, a controller, and necessary plumbing and instrumentation. In general, the system operates to remove carbon dioxide continuously by alternately absorbing and desorbing each bed. The sequence of operation is shown in Table 1 for the startup cycle and the first full cycle. At startup, bed #2 desorbs while bed #1 is on standby. Initial flow from the desorbing bed #2 flows to the cabin until the flow reaches 0.01 cfm as detected by the flow sensor. Then, the flow is directed to an accumulator. Pressure builds in the accumulator until 24 psia is reached. At this pressure, flow is permitted to leave at a controlled rate to a carbon dioxide reduction process. If pressure builds beyond 30 psia, carbon dioxide is dumped overboard to lower the pressure below 30 psia. During desorb, the pressure in the accumulator back pressures the desorbing bed. A check valve prevents any back flow from the accumulator to the beds.

Table 1
 SAWD Operation From Startup

	Bed #1	Bed #2	Fan	Steam	Desorb Flow To Cabin Or Accumulator	Event To Switch To Next Stop
Startup Cycle	---	Desorb	Off	On	Cabin	Flow Sensor \geq 0.01 cfm
	---	Desorb	Off	On	Accumulator	Bed #2 exit temp \geq 180°F
	---	Bleed to #1	Off	Off	---	Time in bleed = 120 sec.
	---	Energy Trans	On	Off	---	Time in E.T. = 300 sec or Bed #1 exit temp \geq 130°F
Cycle #1	Desorb	Absorb	On	On	Cabin	Flow Sensor \geq 0.01 cfm
	Desorb	Absorb	On	On	Accumulator	Bed #1 exit temp \geq 180°F
	Standby	Absorb	On	Off	---	Absorb time reaches tab = f(Cabin RH)
#1	Bleed to #2	---	Off	Off	---	Bleed time = 120 sec
	Energy Trans	---	On	Off	---	E.T. time = 300 sec or Bed #2 exit temp \geq 130°F
	Absorb	Desorb	On	On	Cabin	Flow Sensor \geq 0.01 cfm
	Absorb	Desorb	On	On	Accumulator	Bed #2 exit temp \geq 180°F
	Absorb	Standby	On	Off	---	Absorb time reaches tab = f(Cabin RH)



2.1 Description of System to be Modeled (Continued)

Desorbing in bed #2 continues until its exit temperature reaches 180°F. At that point, fan flow and steam flow cease and the pressure in bed #2 slowly bleeds to bed #1 for 120 seconds. Then, the fan starts flowing cabin air through bed #2 to bed #1 and then back to the cabin. As the air passes through bed #2 it pushes the steam in bed #2 ahead to bed #1 and thereby heats bed #1. This energy transfer continues for five minutes or until the bed #1 exit temperature reaches 130°F, whichever occurs first.

After energy transfer is completed, steam begins to flow to bed #1 to desorb it while valve positions are changed to direct air flow exiting bed #2 back to the cabin. Desorbing continues in bed #1 with any flow directed back to the cabin until the flow reaches 0.01 cfm. Then, the desorb flow is directed to the accumulator. The process continues as described previously but with bed #1 desorbing and bed #2 absorbing. Absorbing in bed #2 continues for a time which is determined directly from the average cabin relative humidity measured during the past desorption of bed #2. The time for successive absorption cycles is determined from the average cabin relative humidity measured during the previous absorption cycle. The beds then alternate through this absorbing-desorbing sequence as directed by the SAWD controller.

Air from the SAWD system enters the humidity control heat exchanger where any moisture is removed. The air returning to the cabin from the SAWD system now has less carbon dioxide.

Cabin air total pressure and oxygen partial pressure are controlled by a two gas controller patterned after that used by the Space Shuttle. It admits oxygen and nitrogen as required to maintain the total pressure at 14.7 psia and the oxygen partial pressure at 3.09 to 3.23 psia. Details of the control logic are shown in Table 2. The opening and closing curves are input by the user as part of the input table data. See Section 4.0.

2.2 Description of Model

The previously described system is modeled for use in the ESCM computer program as shown in Figure 4. Since ESCM uses G189A as a basis, the Figure 4 schematic is set up in G189A format. Therefore, each component is given a number, and the entering and exit flow paths are given a letter P or S to designate the path into or out of the component as primary or secondary.

Table 3 identifies the component subroutine used for each component and also presents the G189A subroutine number. All components are labelled in Figure 4 except those indicated by a small circle or small square. If the small circle has two flows entering and one leaving, the component is a mixer. It simply mixes the two entering flows. If the small circle has one entering flow and two leaving, the component is a splitter. It splits the entering flow into the two paths per a user provided split ratio. Of course, all the

Table 2
Controller Logic For 14.5 psi Shuttle Two Gas Controller

-----Condition-----					-----Action-----			
Initial Oxygen Valve Status	Initial Nitrogen Valve Status	Last Valve Opened	PT (psia)	P _{O₂} (psia)	Oxygen Valve Status	Nitrogen Valve Status	O ₂ Flow Per Opening Or Closing Curve	N ₂ Flow Per Opening Or Closing Curve
N/A	N/A	N/A	≥14.819	---	Closed	Closed	---	---
N/A	N/A	N/A	≥14.813	≥3.23	Closed	Closed	---	---
Closed	N/A	N/A	<14.819	<3.09	Open	Closed	Opening	---
Open	N/A	N/A	<14.819	<3.09	Open ¹	Closed	Closing ¹	---
Closed	N/A	Oxygen	<14.819	3.09<P _{O₂} <3.23	Open	Closed	Opening	---
Open	N/A	Oxygen	<14.819	3.09<P _{O₂} <3.23	Open ¹	Closed	Closing ¹	---
N/A	Closed	Nitrogen	<14.819	3.09<P _{O₂} <3.23	Closed	Open	---	Opening
N/A	Open	Nitrogen	<14.819	3.09<P _{O₂} <3.23	Closed	Open ¹	---	Closing ¹
N/A	Closed	N/A	<14.813	≥3.23	Closed	Open	---	Opening
N/A	Open	N/A	<14.813	≥3.23	Closed	Open ¹	---	Closing ¹

¹ When flow calculated by closing curve = 0.0, valve closes.

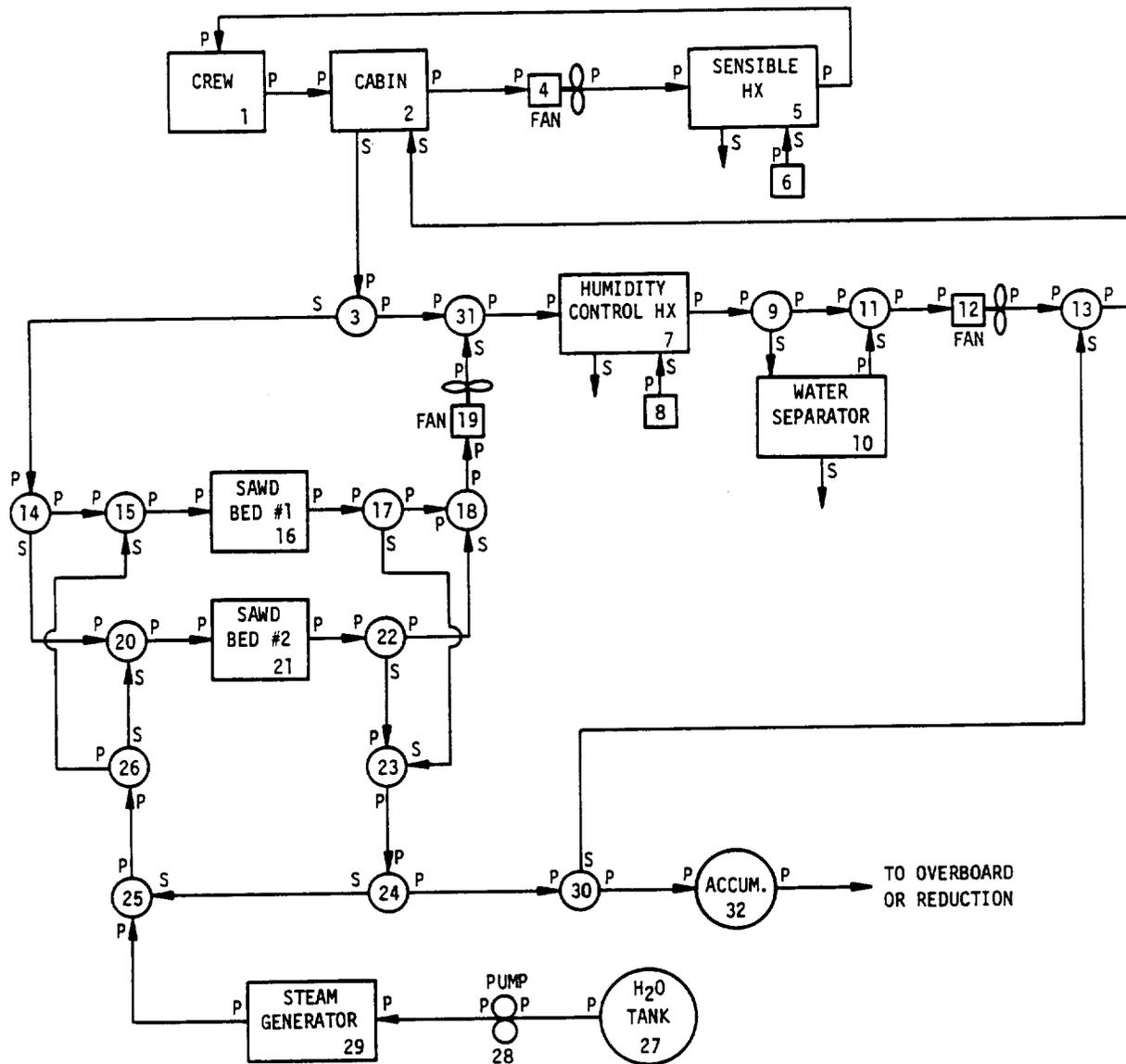


Figure 4

ARS - SAWD II Schematic As Modeled In The ESCM

Table 3
ESCM Component Number - Subroutine Cross Reference Table

<u>Component No.</u>	<u>Component Description</u>	<u>Subroutine Name</u>	<u>Subroutine No.</u>
1	Crew in cabin	SUITS	2
2	Cabin	CABIN	1
3	Split to humidity control HX or SAWD	SPLIT	10
4	Cabin Sensible HX fan	FAN	23
5	Cabin sensible HX	ANYHX	4
6	Cabin sensible HX cooling fluid boundary	ALTCOM	49
7	Cabin condensing HX	ANYHX	4
8	Condensing HX cooling fluid boundary	ALTCOM	49
9	Split to water separator or bypass	SPLIT	10
10	Water separator	ALTCOM	49
11	Mix water separator and bypass	GASMIX	6
12	Condensing HX fan	FAN	23
13	Mix SAWD and condensing HX flows	GASMIX	6
14	Split to SAWD bed #1 or #2	SPLIT	10
15	Mix steam or cabin air to bed #1	GASMIX	6
16	SAWD bed #1	IR45	73
17	Split to cond. HX or CO2 recovery	SPLIT	10
18	Mix bed #1 and bed #2 flows	GASMIX	6
19	SAWD fan	FAN	23
20	Mix steam or cabin air to bed #2	GASMIX	6
21	SAWD bed #2	IR45	73
22	Split to cond. HX or CO2 recovery	SPLIT	10
23	Mix bed #1 and bed #2 exit gases	GASMIX	6
24	Split to preheat or CO2 accumulator	SPLIT	10
25	Mix steam generator and preheat streams	GASMIX	6
26	Split to SAWD bed #1 or #2	SPLIT	10
27	Water supply tank	TANKG	30
28	Water supply pump	PUMP	22
29	Steam generator	SMGEN	27
30	Split desorbed gas to cabin or CO2 accumulator	SPLIT	10
31	Mix cabin air and SAWD air	GASMIX	6
32	Carbon dioxide accumulator tank	TANKG	30



2.2 Description of Model (Continued)

entering flow could be directed to take one of the exiting flow paths. Splitters and mixers are used to represent valve functions. The small square components are alternate components and simply provide boundary condition water flows and temperatures to the two heat exchangers.

3.0 DESCRIPTION OF ESCM COMPUTER PROGRAM

The total ESCM program consists of eight entities:

- G189A executive subroutines
- G189A utility subroutines
- G189A special purpose subroutines
- G189A plot subroutines
- G189A component subroutines
- G189A application specific subroutines GPOLY1 and GPOLY2
- G189A subroutine additions for ESCM: IR45, ARSS
- G189A input specific for ESCM

While a detailed discussion of the sequence of operation G189A can be found in Reference 3 for the interested user, a brief description is presented here and shown in Figure 5.

- (1) At the start of execution, the G189 executive subroutines process the input data by allocating the data storage space and dynamically loading the integer and floating point data into a large single array; the K and V array.
- (2) After the input data is processed, a printoff of the component initial values and the solution path is generated.
- (3) From the input solution path, the executive subroutines retrieve and unpack from the large single array the first component's integer instruction data; and the executive subroutines retrieve from the large single array and store into small working arrays the component floating point data.
- (4) Thermophysical property data (specific heat, molecular weight, thermal conductivity, and viscosity) for the component source streams are evaluated using G189A utility subroutines.
- (5) A transfer to the user coded subroutine GPOLY1 is made to allow data modifications or logic changes to be incorporated prior to component solution.
- (6) The executive routines then transfer computer operation to the proper subroutine for the component.
- (7) Following component solution, a transfer to the user coded subroutine GPOLY2 is made to allow data modifications or logic changes after component solution.

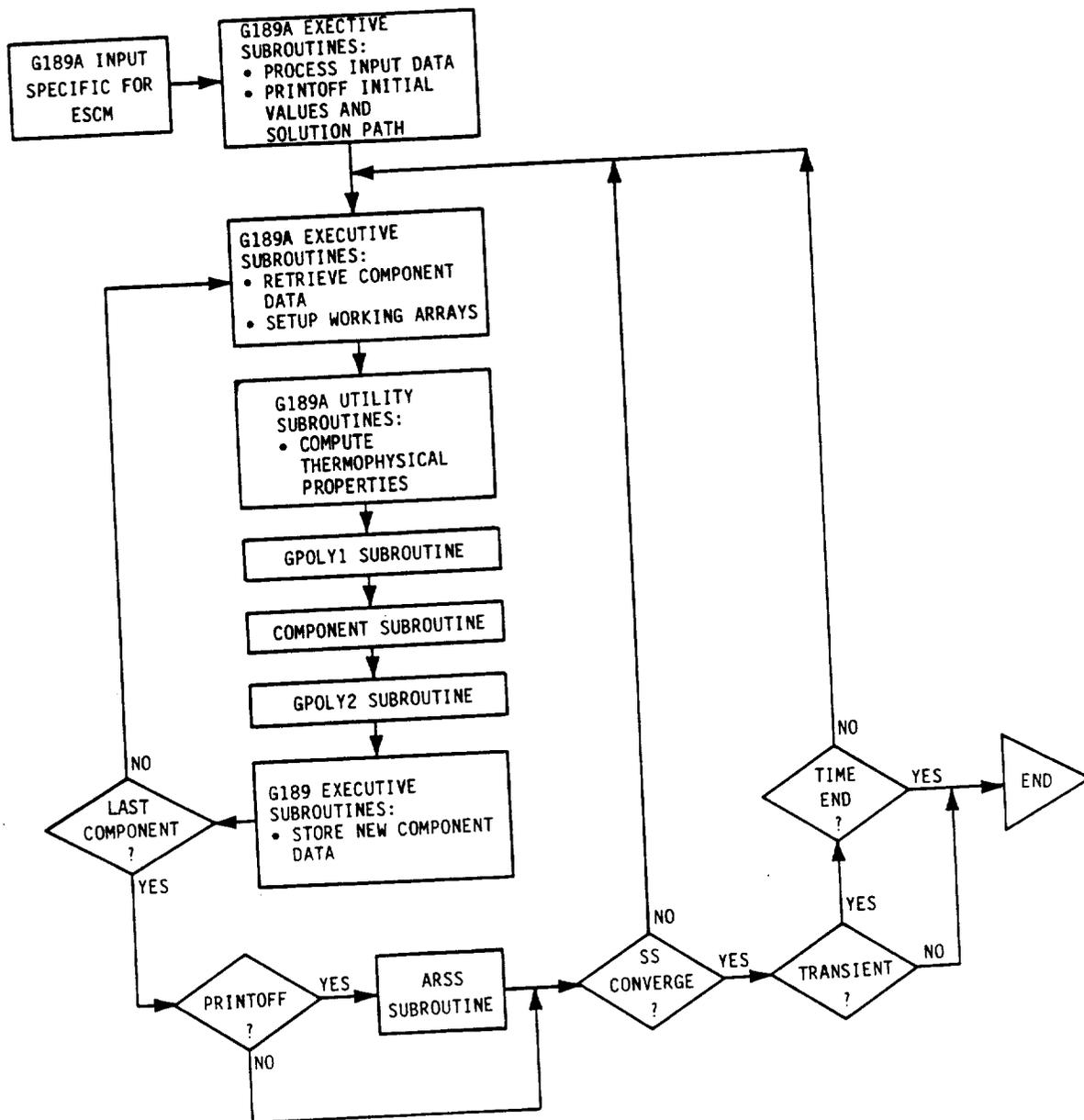


Figure 5
 Flow Chart Of ESCM Computer Program Operation



3.0 DESCRIPTION OF ESCM COMPUTER PROGRAM (Continued)

- (8) The new component status and data are returned to the large single array.
- (9) Steps (3) through (8) are repeated for each component in the solution path.
- (10) A printoff of the ARS subgroup schematic is made by subroutine ARSS for every steady state pass and after every user specified number of time steps in transient runs.
- (11) Steps (3) through (10) are repeated until a steady state solution is achieved; then, if specified, a transient begins and will end at the user specified time.

The following sections present a description of the seven entities previously mentioned.

3.1 G189A Executive Subroutines

The executive subroutines consist of the master control block subroutine ECLST and the input editor subroutines: IEDIT, CASDAT, BASDAT, MERGEC, KVREAD, TABLRD, SCRUP, ENKODE/DEKODE, IVBLOK, ULOSE, UWIN, and DBLOCK.

The main program is called X189#A and simply transfers operation to the master control block subroutine ECLST.

Complete descriptions of these subroutines can be found in Reference 3.

3.2 G189A Utility Subroutines

Utility subroutines are those subroutines which are general enough in form and application that they could be used by a number of subroutines. The utility subroutines used by ESCM are presented in Table 4; a complete description of these subroutines can be found in Reference 3.

3.3 G189A Special Purpose Subroutines

Special purpose subroutines are lower level subroutines which are generally called by either the executive subroutines or by a component subroutine. These subroutines were created for one particular purpose and are not general enough to be classified as a Utility Subroutine. The special purpose routines used by ESCM are presented in Table 5; a complete description of these subroutines can be found in Reference 3.

3.4 G189A Component Subroutines

Each particular type of component in an Environmental Control and Life Support System is simulated by a component subroutine. The G189A component subroutines used by ESCM are presented in Table 6, a complete description of these subroutines can be found in Reference 3.

Table 4
G189A Utility Subroutines

<u>Subroutine Name</u>	<u>Description</u>
ABRPRT	A, B, and R Array Printout
CYCLE	Cycle Displacement Time
ELAPSE	Central Processor and Peripheral Processor Elapsed Times
ESTIM	Reestimator for Iterative Calculations
FLØARY	Selects and Stores Component Flow Data into 19 Member Flow Array
FLØSUM	Sums Constituent Flows to Obtain Total Flows within a 19 Member Flow Array
HBALNC	Computes Adiabatic Mixture Conditions for a 19 Member Flow Array
HF	Computes Specific Enthalpy of Liquid Water
HG	Computes Specific Enthalpy of Water Vapor
KK	Locates and Returns Value Stored in Specified Component K Array Reference Location
LK	Calculates and Returns K Array Address of Specified Component K Array Reference Location
LV	Calculates and Returns V Array Address of Specified Component V Array Reference Location
PRØP	Calculates Thermo-Physical Property Data for a 19 Member Flow Array
PRTIME	Accesses and Prints Computer Clock Time
PSAT	Determines Water Vapor Pressure at a Specified Temperature
QSURR	Determines Heat Loss to the Surroundings for a Component
RH	Calculates Relative Humidity and Dew Point of a 19 Member Flow Array
SHELL	Unpacks Modular K Array Data

Table 4 (Continued)
 G189A Utility Subroutines

<u>Subroutine None</u>	<u>Description</u>
SK	Stores Integer Data into a Specified Component K Array Reference Location
STØPIT	Places End-of-File Mark on Output Tape (Normal Run Termination Subroutine)
SV	Stores Floating Point Data into a Specified Component V Array Reference Location
TAPEIT	Used to Dump D/V Array Data onto File
TSAT	Determine Saturation Temperature of Water Vapor at a Specified Pressure
VALUE	Table Interpolation Function
VARPRT	Labelled Printout of all Components' K and V Array Data
VDATPT	Component's V Array Data Printout
VV	Locates and Returns Value Stored in Specified Component V Array Reference Location
WASP	Calculates Thermodynamic and Transport Properties of Water and Steam

Table 5
G189A Special Purpose Subroutines

<u>Subroutine None</u>	<u>Description</u>
ALFRED	Error Mode Output Format
CØMSØL	Component Subroutine Selector
CØ2CP	Computes Effective Specific Heat for Precipitation of Carbon Dioxide in a Heat Exchanger
EFFCP	Effective Specific Heat for Heat Exchanger Calculations
HXPER	Steady State Heat Exchanger Performance
VLH2Ø	Calculates Equilibrium Pressure of Water Vapor on IR-45 Solid Amine Resin

Table 6
G189A Component Subroutines

<u>Subroutine None</u>	<u>Description</u>
ALTCØM	Alternate Component
ANYHX	Compact Heat Exchanger
CABIN	Cabin or Compartment
DUCT	Length of Gas Circuit Ducting
FAN	Fan, Blower, or Compressor
GASMIX	Gas Mix
LIQMIX	Liquid Mix
PUMP	Pump
SMGEN	Steam Generator
SPLIT	Generalized Split
SUITS	Crewmen in Suits or Cabin
TANKG	Storage Tank
VACPMP	Vacuum Pump

3.5 G189A Plot Subroutines

Two subroutines are used to save data for use by a separate plotting routine. These subroutines are MAINPL and PLEDIT both of which are described in Reference 3.

3.6 GPOLY1 and GPOLY2 for ESCM

GPOLY1 and GPOLY2 are coded for the ESCM application to make data modifications, logic changes, and solution path changes. GPOLY1 is executed before the component subroutine while GPOLY2 is executed after the component subroutine.

Both GPOLY subroutines are setup in the same manner. The standard construction is:

```

      IF (N .NE. 3) GO TO 399
      .
      .
      .
      399 CONTINUE
  
```

N is the component number which is about to be or just was analyzed. This construction causes logic to be performed only for the component presently being analyzed. A construction of this type is written for each component where desired by the user.

3.6.1 GPOLY1

The GPOLY1 subroutine in ESCM essentially simulates the control functions required for the ARS subgroup modelled. These control functions are:

- (1) control of oxygen and nitrogen addition to maintain desired levels of oxygen partial pressure and cabin total pressure.
- (2) control of cooling flow to sensible heat exchanger to maintain desired cabin temperature.
- (3) control cycling and total operation of SAWD carbon dioxide removal system.

The following are input once at the first execution of GPOLY1:

DTIME	= Time step, seconds
VV(2,184)	= Printoff frequency, time steps per printoff
VV(16,93)	= Total weight of foam in bed #1, lbm
VV(16,94)	= Specific heat of foam in bed #1, Btu/lbm-F
VV(16,79)	= Total canister thermal mass in bed #1, lbm
VV(16,84)	= Specific heat of canister in bed #1, Btu/lbm-F
VV(16,78)	= Total dry resin weight in bed #1, lbm
VV(16,66)	= Specific heat of dry resin in bed #1, Btu/lbm-F

3.6.1 GPOLY1 (Continued)

The following are input and output from GPOLY1 before solution of component number 1 (the crew):

Input:

TIME = Time in transient, seconds
VV(2,104) = Cabin temperature, °F

Output:

R(66) = Crew total sensible heat, Btu/hr
R(67) = Crew total latent heat, Btu/hr
R(82) = Crew total metabolic rate, Btu/hr

The following are input and output from GPOLY1 before the solution of component number 2 (the cabin):

Input:

STEADY = Logical variable denoting if steady state calculations are now being performed or not.
KSYSPAS = Integer variable which counts the number of passes of the computer program through the solution of all the components.
IFREQ = The number of computer passes to be performed per printoff using ARSS subroutine.
DTIME = Current time step, seconds.
R(4) = Total pressure of flow leaving cabin via the primary flow path.
R(94) = Cabin partial pressure of oxygen, psia.
R(180) = Flag denoting whether oxygen or nitrogen was last gas admitted through two gas controller. 1 = nitrogen, 0 = oxygen.

Output:

R(165) = Flow oxygen into cabin, lb/hr
R(166) = Flow of nitrogen into cabin, lb/hr

The following are input to and output from GPOLY1 before the solution of component number 3 (Splitter for flow from cabin):

3.6.1 GPOLY1 (Continued)

Input:

- STEADY = Logical variable denoting if steady state calculations are now being performed or not.
 KSYPAS = Integer variable which counts the number of passes of the computer program through the solution of all the components.
 VV(19,1) = Total gas flow through SAWD fan, lb/hr.
 VV(24,1) = Total flow to splitter from SAWD beds, lb/hr. Flow goes to other bed or to CO₂ accumulator.
 VV(12,1) = Total flow (lb/hr) through cabin condenser heat exchanger fan.
 VV(10,67) = Condensate removed (lb/hr) in cabin condenser heat exchanger.

Output:

- R(65) = Splitting ratio in splitter (ratio of flow to SAWD to total secondary flow from cabin).

The following are input to and output from GPOLY1 before the solution of component number 5 (main cabin sensible heat exchanger):

Input:

- STEADY = Logical variable denoting if steady state calculations are now being performed or not.
 KSYPAS = Integer variable which counts the number of passes of the computer program through the solution of all the components.
 VV(2,104) = Main cabin gas mixture temperature, °F
 VV(2,87) = Main cabin gas design temperature, °F

Output:

- B(1) = Cooling flow to sensible heat exchanger, lbm/hr

The following are input to and output from GPOLY1 before the solution of component number 7 (humidity control heat exchanger):

Input:

- A(1) = Total primary (gas) flow into humidity control heat exchanger.
 R(72) = Effective specific heat (Cp) of gas flow into humidity control heat exchanger, Btu/lb-°F
 B(1) = Water cooling flow into humidity control heat exchanger, lbm/hr
 CPA = Specific heat of total air flow entering the humidity control heat exchanger, Btu/lbm-°F



3.6.1 GPOLY1 (Continued)

Output:

R(66) = Calculated overall heat transfer coefficient of humidity control heat exchanger, Btu/hr-°F

The following are input to and output from GPOLY1 before the solution of component number 10 (water separator for cabin condenser heat exchanger).

Input:

A(7) = Condensable entrained liquid flow, lb/hr
 A(1) = Total primary flow into water separator, lb/hr
 A(5) = Non-condensables flow into water separator, lb/hr
 A(8) = Non-condensables specific heat, Btu/lb-°F
 A(6) = Condensable vapor flow into water separator, lb/hr
 CPONV = Specific heat of condensable vapor flow into separator, Btu/lb-°F

Output:

R(67) = Condensable entrained liquid flow, lb/hr
 A(1) = Total flow into water separator after removal of entrained liquid, lbm/hr
 CPA = Specific heat of total flow into water separator, Btu/lbm-°F
 R(65) = Power added to water separator, Btu/hr
 A(7) = New entrained liquid flow which is set to 0.0 lb/hr.

The following are input to and output from GPOLY1 before the solution of component number 14 (splitter for gas flow from main cabin to SAWD bed #1 or SAWD bed #2). This section of GPOLY1 is where all the control logic for the operation of the SAWD carbon dioxide removal system is performed.

Input:

STEADY = Logical variable denoting if steady state calculations are now being performed or not.
 TIMEMX = Length of time the transient case is to run, seconds.
 TIME = Length of time into transient, seconds.
 DTIME = Time step between iterations, seconds.
 RHAvg = Average relative humidity (decimal form) in cabin during absorption cycle.
 TABOLD = Length of absorption cycle before present iteration, seconds.
 VV(2,89) = Cabin gas relative humidity (decimal form).
 VV(21,2) = Temperature of flow exiting SAWD bed #2, °F
 VV(21,85) = Exit temp. from SAWD bed to end desorption, °F.

3.6.1 GPOLY1 (Continued)

Input:

- VV(2,183) = SAWD absorption cycle time curve multiplication factor.
- KK(21,16) = Absorb/desorb flag for SAWD bed #2 (0=absorb, 1=desorb)
- TBSET = Length of time during which the bed which just finished desorbing bleeds its pressure to the other bed, seconds.
- TEXCHG = Maximum length of time (seconds) during which the bed which just finished desorbing will transfer energy to the other bed if the other bed does not reach a set temperature.
- KK(16,16) = Absorb/desorb flag for SAWD bed #1 (0=absorb, 1=desorb)
- TPEND = Temperature of SAWD bed receiving energy at which energy transfer from the other SAWD bed is terminated, °F.
- VV(16,2) = Temperature exiting SAWD bed #1, °F
- A(1) = Total flow into splitter (splitter for flow to beds), lb/hr.
- RHOA = Density of gas flowing from cabin to beds, lb/ft³.
- VV(2,20) = Total secondary flow from cabin to humidity control splitter, lb/hr.
- V(IS+I) = This statement denotes various portions of the cabin secondary flow. The flows that are calculated (lb/hr) include: oxygen, diluent = nitrogen, carbon dioxide, trace contaminant flow.
- V(IS+6) = Condensable vapor secondary flow from cabin, lb/hr.
- V(IS+7) = Condensable entrained liquid flow from cabin secondary flow, lb/hr.

Output:

- A(I) = Separate flows of oxygen, nitrogen, carbon dioxide and trace contaminants to SAWD bed splitter, lb/hr.
- WSTM = Flow of steam needed for a particular desorption cycle, lb/hr.
- CFM = Flow through SAWD bed fan, ft³/min.
- A(1) = Total flow to humidity control splitter from cabin, lb/hr.
- VV(14,65) = Ratio of secondary exit flow to inlet flow for splitter #14.
- VV(17,65) = Ratio of secondary exit flow to inlet flow for splitter #17.
- VV(22,65) = Ratio of secondary exit flow to inlet flow for splitter #22.
- VV(24,65) = Ratio of secondary exit flow to inlet flow for splitter #24.

3.6.1 GPOLY1 (Continued)

VV(26,65)	= Ratio of secondary exit flow to inlet flow for splitter #26.
VV(30,65)	= Ratio of secondary exit flow to inlet flow for splitter #30.
KK(17,8)	= Number of component to be solved after component #17.
KK(22,8)	= Number of component to be solved after component #22.
KK(24,8)	= Number of component to be solved after component #24.
KK(26,8)	= Number of component to be solved after component #26.
KK(29,8)	= Number of component to be solved after component #29.

The following are input to and output from GPOLY1 before the solution of component 15 (gas mixer - steam or cabin gas to SAWD bed #1 inlet):

Input:

BLEED	= Flag is true if SAWD cycle is in pressure bleed phase.
KK(16,16)	= Absorb/desorb flag for SAWD bed #1 (0=absorb, 1=desorb).

Output:

B(I)	= Secondary side inlet flows which are set equal to zero during bed #1 pressure bleed down to bed #2.
------	---

The following are input to and output from GPOLY1 before the solution of component 16 (SAWD bed #1). Here is calculated the pressure decay in bed #1 during its pressure bleed to bed #2.

Input:

KK(16,16)	= Absorb/desorb flag for SAWD bed #1 (0=absorb, 1=desorb).
VV(3,23)	= Outlet pressure from humidity control splitter on secondary side (to beds), psia.
KK(16,19)	= Number of SAWD bed segments used in calculations in SAWD bed #1.
V(IV+J)	= Void volume of segment "j" in SAWD bed #1, ft ³
R(4)	= Outlet pressure at bed #1 for bleeddown, psia
R(2)	= Temperature of fluid exiting bed #1, °F
R(5)	= Non-condensable flow from bed #1, lb/hr
R(6)	= Condensable vapor flow from bed #1, lb/hr
R(9)	= Molecular weight of non-condensables, lb/mol.

3.6.1 GPOLY1 (Continued)
Output:

PNEW = Inlet pressure to SAWD bed #1, psia

The following are input to and output from GPOLY1 before the solution of component number 20 (gas mixer - steam or cabin gas to SAWD bed #2 inlet):

Input:

BLEED = Flag is true if SAWD cycle is in pressure bleed phase.

KK(21,16) = Absorb/desorb flag for SAWD bed #2 (0=absorb, 1=desorb).

Output:

B(I) = Secondary side inlet flows which are set equal to zero during bed #2 pressure bleed down to bed #1.

The following are input to and output from GPOLY1 before the solution of component number 21 (SAWD bed #2). Here is calculated the pressure decay in bed #2 during its pressure bleed to bed #1.

Input:

KK(21,16) = Absorb/desorb flag for SAWD bed #2 (0=absorb, 1=desorb).

KK(21,19) = Number of SAWD bed segments used in calculations in SAWD bed #2.

 V(IV+J) = Void volume of segment "j" in SAWD bed #2, ft³

VV(3,23) = Outlet pressure from humidity control splitter on secondary side (to beds), psia.

R(4) = Outlet pressure at bed #2 for bleeddown, psia

R(2) = Temperature of fluid exiting bed #2, psia

R(5) = Non-condensable flow from bed #2, lb/hr

R(6) = Condensable vapor flow from bed #2, lb/hr

R(9) = Molecular weight of non-condensables, lb/mol.

Output:

PNEW = Inlet pressure to SAWD bed #2, psia.

The following are input to and output from GPOLY1 before the solution of component 25 (mixer of flows from steam generator and from a SAWD bed during energy transfer). Here the secondary side inlet flow (i.e., the flow which would come from a SAWD bed during energy transfer or bleed) is set equal to zero whenever the SAWD is not in the energy transfer or bleed portions of its cycle.

3.6.1 GPOLY1 (Continued)

Input:

PREHET = Flag is true if SAWD is in energy transfer portion of its cycle.
 BLEED = Flag is true if SAWD is in bleed portion of its cycle.

Output:

B(I) = Flows into secondary side of mixer.

The following are input to and output from GPOLY1 before the solution of component 27 (water supply tank for steam generator). Here is calculated the water flow to be used for desorbing a SAWD bed.

Input:

VV(2,105) = Cabin gas mixture total pressure, psia
 VV(32,72) = Pressure in carbon dioxide accumulator, psia
 VV(30,65) = Split ratio in component 30 (splitter for flow to CO₂ accumulator or to cabin).
 STEADY = Logical variable denoting if steady state calculations are now being performed or not.
 R(100) = Steam flow, pph.
 KK(16,16) = Absorb/desorb flag for SAWD bed #1 (0=absorb, 1=desorb)
 VV(16,2) = Temp exiting SAWD bed #1, °F
 VV(16,85) = Exit temperature to end desorption, °F
 KK(21,16) = Absorb/desorb flag for SAWD bed #2 (0=absorb, 1=desorb).
 BLEED = Flag is true if SAWD is in bleed portion of cycle.
 PREHET = Flag is true if SAWD is in energy transfer portion of cycle.
 VV(21,2) = Temp exiting SAWD bed #2, °F
 VV(21,85) = Exit temperature to end desorption, °F

Output:

R(1) = Total flow from water tank, lb/hr

The following are input to and output from GPOLY1 before the solution of component 30 (splitter for desorbed gas - to cabin or CO₂ accumulator). Here is the control logic to simulate the flow sensor sensing flow and to direct the desorbed flow to the accumulator when the flow reaches the setpoint.



3.6.1 GPOLY1 (Continued)

Input:

RHOA = Density of flow to splitter, lbm/ft³
 A(1) = Total flow to splitter, lb/hr
 KK(16,16) = Absorb/desorb flag for SAWD bed #1 (0=absorb, 1=desorb).
 KK(21,16) = Absorb/desorb flag for SAWD bed #2 (0=absorb, 1=desorb).

Output:

R(65) = Split ratio in splitter which is ratio of flow directed to cabin to total entering flow.

The following are input to and output from GPOLY1 before the solution of component 32 (CO₂ accumulator tank). Here is the logic to determine the flow leaving the accumulator depending on whether the flow is to go overboard or to another system for reduction of the carbon dioxide.

Input:

STEADY = Logical variable denoting if steady state calculations are now being performed or not.
 R(72) = Pressure in accumulator, psia.
 KK(32,16) = Carbon dioxide delivery (0=overboard, 1=CO₂ reduction).
 A(1) = Total flow to CO₂ accumulator, lb/hr
 R(71) = CO₂ accumulator tank volume, ft³
 R(70) = CO₂ temperature, °F

Output:

R(1) = Total flow out of CO₂ accumulator, lb/hr

3.6.2 GPOLY2

The GPOLY2 subroutine in ESCM performs several calculations to tally the rate of change in oxygen, carbon dioxide, and water vapor in the cabin, to compute the water and carbon dioxide loadings in both SAWD beds, and lastly to tally with time the total water used for SAWD bed desorption, and the total condensate removed from the cabin air.

Input and output from the GPOLY2 subroutine are made through the R and K arrays of the G189A framework. All transfer of data in and out of the subroutine is performed in the appropriate COMMON blocks.

3.6.2 GPOLY2 (Continued)

The following are input and output from GPOLY2 after component 1 (crew) is analyzed:

Input:

KK(21,16) = SAWD bed #2 absorb/desorb flag: 0=absorb,
 1=desorb.
 VV(16,72) = Total SAWD bed #1 CO₂ absorption rate, lbm/hr.
 VV(16,73) = Total SAWD bed #1 H₂O evaporation rate, lbm/hr.
 VV(24,65) = SAWD exit flow control valve 1.0 = flow goes to
 opposite bed for energy transfer; 0.0 = flow goes
 to accumulator. See Figure 4.
 VV(21,72) = Total SAWD bed #2 CO₂ absorption rate, lbm/hr.
 VV(21,73) = Total SAWD bed #2 water evaporation rate, lbm/hr.
 R(70) = Total crew water vapor generation rate, lbm/hr
 VV(10,67) = Rate of condensate removal from cabin, lbm/hr
 R(68) = Total crew oxygen usage rate, lbm/hr
 R(69) = Total crew carbon dioxide generation rate, lbm/hr

Output:

VV(2,137) = Net water vapor flow into cabin, lbm/hr
 VV(2,175) = Net oxygen addition rate to cabin, lbm/hr
 VV(2,177) = Net carbon dioxide addition rate to cabin, lbm/hr

The following are input and output for GPOLY2 after component 16 (bed #1) or 21 (bed #2) are analyzed. Here bed loadings are calculated, and during steady state, the proper air temperature and mass flows of vapor and entrained liquid are computed.

Input:

R(78) = Total dry bed #1/#2 resin weight, lbm
 R(80) = Total water in bed #1/#2 resin, lbm
 R(81) = Total carbon dioxide in bed #1/#2 resin, lbm
 A(2) = Bed #1 or bed #2 inlet flow temperature, °F
 A(5) = Bed #1 or bed #2 inlet non-condensable flow, lbm/hr
 A(6) = Bed #1 or bed #2 inlet water vapor flow, lbm/hr
 A(7) = Bed #1 or bed #2 inlet entrained liquid flow,
 lbm/hr
 A(8) = Specific heat of non-condensable flow entering bed
 #1 or bed #2, Btu/lbm-°F
 STEADY = Logical variable denoting if steady state calcu-
 lations are now being performed or not.

3.6.2 GPOLY2 (Continued)
Output:

R(82) = Total bed #1 or bed #2 water loading, lbm/lbm
 R(83) = Total bed #1 or bed #2 carbon dioxide loading,
 lbm/lbm of dry resin.
 R(2) = Bed #1/#2 exit flow temperature, °F
 R(6) = Bed #1/#2 exit water vapor flow, lbm/hr
 R(7) = Bed #1/#2 exit entrained liquid flow, lbm/hr

Note: Variables R(2), R(6), and R(7) are output only during steady state calculations.

The following are input to and output from GPOLY2 after component 27 (the water supply tank) is analyzed.

Input:

R(1) = Total flow exiting water supply tank, lbm/hr
 R(98) = Previous total water used from tank, lbm
 R(99) = Previous total water added to tank, lbm
 DTIME = Current time step, seconds
 STEADY = Logical variable denoting if steady state calculations are now being performed or not.
 VV(10,67) = Rate of condensate removal from cabin, (i.e., rate of water added to tank), lb/hr

Output:

R(98) = Updated total water used from tank, lbm
 R(98) = Updated total water added to tank, lbm

No error messages are generated by GPOLY2. Lower level functions and subroutines used by GPOLY2 are:

VV KK HG HF HBLANC

3.7

ARSS Subroutine

The ARSS subroutine generates a schematic of the modeled atmospheric revitalization subsystem with performance information such as flow, temperature, and heat load printed near each component. Also printed are total crew loadings and cabin conditions. This subroutine is called from sburoutine ECLST; but whether ARSS is called or not in ECLST is specified by the user through the printoff frequency input variable IFREQ which is equal to VV(2,184). Figure 6 shows a sample schematic generated by ESCM in the ARSS subroutine.

```

1 SPACE STATION AIR REVITALIZATION SUBSYSTEM SAWD II DEMONSTRATION MODEL. MISSION TIME: 3015. SEC ( 0.84 HR) DATE: 01/26/85
2
3 XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
4 X
5 X CABIN (2) CREW (1) FROM CABIN ***** TO CABIN X
6 X M= 9357. M= 70.6 T= 66.4 X
7 X VOLUME = 8000. CU-FT NO OF MEN = 3 T= 69.5 *T= 70.6 T= 66.4 X
8 X AIR MASS = 594.03 LDM TOTAL Q = 1423.5 B/HR A ----- A X
9 X TEMP = 69.5 F METABOLIC Q = 474.5 B/HR/HAN A |SENSIBLE| |SENSIBLE| A X
10 X DEW PT = 51.2 F SEHSIBLE = 330.2 B/HR/HAN A |HX FAN (4) | T= 70.8 |HX (5)| A X
11 X TOTAL PRESS = 14.69 PSIA LATENT = 144.3 B/HR/HAN AAAAAAAAAA|Q = 2843. |AAAAAAAAAAAA|Q=-10105. |AAAAAAAAAAAAAAAAAA X
12 X O2 PRESS = 2.89 PSIA O2 USAGE = 0.2320 PPH -----> |CFM= 2100. | | -----> X
13 X CO2 PRESS = 2.58 MI-HG CO2 PROD = 0.2733 PPH -----> X
14 X GAS LEAKAGE = 0.083 PPH * X
15 X O2 MAKEUP = 0.000 PPH M= 950. * X
16 X N2 MAKEUP = 0.000 PPH T= 60.0 * TO CABIN X
17 X NON ECLSS Q: FROM CABIN ***** M= 1387. X
18 X SENSIBLE = 17065. B/HR M= 1329. *T= 56.6 -----> T= 51.6 X
19 X LATENT = 255. B/HR * A X
20 X ECLSS Q: | A -----> *T= 56.6 A A X
21 X SENSIBLE = 5399. B/HR | A M= 1388. |REL. HUMD. | T= 50.2 M= 1344. M= 1385. |REL. HUMD. | A | X
22 X LATENT = 2607. B/HR | A T= 73.3 |HX (7) | T= 50.2 M= 1344. T= 50.2 |HX FAN (12)| A | X
23 X REL HUMIDITY = 51.82 PCT V A T= 73.3 |HX (7) | T= 50.2 M= 1344. T= 50.2 |HX FAN (12)| A | X
24 X (31)AAAAAAAAAAAA|Q=-11026. |AAAAAAAAAAAA(9)AAAAAAAAAAAAAAAAAAAA(11)AAAAAAAAAAAAAAAAAA|Q = 478. |AAA | X
25 X A -----> | -----> | A -----> A -----> |CFM= 300. | X
26 X A A -----> A X
27 X | A M= 59.17 * | A |HX2O SEP (10)| A M= 41.6 X
28 X | A T=156.2 *M= 950. V AA|Q = 13. |AAA T= 51.5 X
29 X | A *T= 45.0 |CFM = 9. | X
30 X FROM CABIN ***** X
31 X M= 56.92 W -----> H2O INTERFACE: M ADDED = 1.601 X
32 X T= 69.5 WXXXXXXXXXXXX M= 2.9 X
33 X A X
34 X A | [SAWD FAN (19)] -----> X
35 X A | |Q = 171. |AAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAA X
36 X A V |CFM= 13. | P= 22.77 A X
37 X A M= 0.0 M= 1.65 -----> M= 0.0 M= 0.0 A | X
38 X | T=284.5 | AMINE | T=110.4 M= 0.0 A | X
39 X (14)AAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAAA(15)SSSSSSSSSS| BED 1 (16)|CCCCCCCCC(17)AAAAAAAAAAAA(18) X
40 X A H2O INTERFACE S -----> |Q = 1677. | -----> C -----> A TO CABIN X
41 X A M USED = 1.830 S | |MCO2 = 0.195| C | A A M= 0.0 X
42 X A W S | |HM2O = 2.924| C | A T= 78.5 X
43 X A |W M= 1.65 M= 1.65 S | M= 0.0 C | A A X
44 X | A |W M= 1.65 S | C | A A X
45 X | A V W T= 70.0 S | C V | A A X
46 X | A S | C | A A X
47 X | A |PUMP | T= 90.7|STEAM | T=284.5 S M= 0.0 C M= 0.0 A M= 0.0 |CO2 | X
48 X V A (28) |XXXXXXXXXXXXGEN (29)|SSSSSSSS(25/26)SSSSSSSSSSSSSSSSSSSSSSSSSSSS(23/24)CCCCCCCCC(1)CCCC(30)CCCCCCCC X
49 X A |Q= 34. | -----> |Q= 1860. | -----> S -----> C -----> A -----> | M= 0.379 | X
50 X A -----> M= 0.0 S | M= 0.0 C | A A X
51 X A S | C | A | X
52 X A S | C | A | X
53 X A S | P= 14.69 C | A | X
54 X A S V M= 56.92 | AMINE | M= 59.17 C | A | X
55 X A M= 56.92 S T= 69.5 | BED 2 (21)| T=144.9 C M= 59.17 A TO DVBD OR X
56 X AAAAAAAAAAAAA|AAAAAAAAAAAAAAAAAAAAAAAAAAAA(20)AAAAAAAAAAAA|Q = -3745. |AAAAAAAAAAAA(22)AAAAAAAAAAAAA RECOVERY X
57 X -----> |MCO2 = 0.027| -----> M= 0.27 X
58 X |HM2O = 2.797| -----> T= 70.0 X
59 X X
60 XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX

```

Figure 6
Sample Schematic Generated By ESCM

3.7

ARSS Subroutine (Continued)

The following are input into Subroutine ARSS and output from it with no manipulations performed on them except those with asterisks. Those with 1 asterisk are manipulated before they are output. The manipulations are noted below. Those with 2 asterisks are input but not output.

IDATE = Date of transient run (input and output).
 TIME = Time into transient, seconds (input and output).

The following inputs/outputs relate to the crew (component 1):

VV(1,65) = Total metabolic heat from crew, Btu/hr
 V(IV+2) = Sensible heat per crewman, Btu/hr
 V(IV+3) = Latent heat per crewman, Btu/hr
 V(IV+4) = Total oxygen use rate, lb/hr
 V(IV+5) = Total CO₂ generation rate, lb/hr
 KK(1,16) = Number of crewmen

The following inputs/outputs relate to the main cabin:

VV(2,1) = Total flow out of cabin to sensible heat exchanger fan, lb/hr
 V(IP+2) = Temperature of flow exiting cabin and flowing to fan, lb/hr
 V(IV+2) = Equipment, lighting and miscellaneous heat load added to cabin gas, Btu/hr
 *V(IV+25) = Cabin gas relative humidity, decimal form. This is multiplied by 100 to put it in percent form before it is output.
 V(IV+30) = Cabin gas oxygen pressure, psia
 V(IV+34) = Cabin gas dew point, °F
 V(IV+36) = Cabin gas carbon dioxide pressure, mmHg
 V(IV+39) = Cabin gas mixture total mass, lbs
 V(IV+40) = Cabin gas mixture temperature, °F
 V(IV+42) = Cabin gas mixture total pressure, psia
 V(IV+58) = Outboard leakage rate, lb/hr
 **V(IV+64) = Water vapor addition rate, lb/hr
 **V(IV+72) = Net non-condensable flow into cabin, lb/hr
 V(IVT+1) = Cabin free volume, ft³
 V(IVEX+6) = Diluent addition rate, lb/hr
 V(IVEX+7) = Carbon dioxide addition rate, lb/hr

3.7 ARSS Subroutine (Continued)

The following inputs/outputs relate to the splitter (component 3) for flow from the cabin:

VV(3,1)	= Total flow from splitter (3) to gas mixer (31) then to humidity control heat exchanger, lb/hr
V(IP+2)	= Fluid temperature exiting splitter primary side (3), °F
V(IS+1)	= Total flow from splitter (3) to SAWD beds, lb/hr
V(IS+2)	= Fluid temperature exiting splitter (3) to SAWD beds, °F

The following inputs/outputs relate to the main cabin sensible heat exchanger fan (component 4):

VV(4,2)	= Temperature of fluid exiting main cabin sensible heat exchanger fan, °F
V(IV+1)	= Heat added to gas stream at fan, Btu/hr
V(IV+12)	= Cabin fan volumetric flow rate, cfm

The following inputs/outputs relate to the sensible heat exchanger (component 5):

VV(5,1)	= Total flow from sensible heat exchanger (5) (primary side - gas side), lb/hr
V(IP+2)	= Temperature of gas exiting sensible heat exchanger (primary side), °F
V(IS+2)	= Temperature of fluid exiting sensible heat exchanger (secondary side), °F
V(IV+1)	= Heat transferred across heat exchanger between secondary and primary sides, Btu/hr
VV(6,1)	= Coolant flow to cabin sensible heat exchanger (5), lb/hr
VV(6,2)	= Temperature of coolant to cabin sensible heat exchanger, °F

The following inputs/outputs relate to the main cabin condensing heat exchanger (component 7, also known as humidity control heat exchanger):

VV(7,2)	= Temperature (°F) of fluid exiting main cabin condensing heat exchanger 7 (humidity control heat exchanger), °F
V(IS+2)	= Temperature (°F) of fluid exiting main cabin condensing heat exchanger 7, secondary or coolant side.
V(IV+1)	= Heat transferred across condensing heat exchanger 7, Btu/hr
VV(8,1)	= Coolant flow to main cabin condensing heat exchanger 7, lb/hr
VV(8,2)	= Temperature of coolant to cabin condensing heat exchanger, °F



3.7 ARSS Subroutine (Continued)

The following inputs/outputs relate to the splitter (component 9) for flow exiting the condensing heat exchanger:

VV(9,1) = Total flow exiting splitter (9) and flowing to gas mixer (11), lb/hr

The following inputs/outputs relate to the water separator (component 10):

VV(10,1) = Total flow from water separator (10) to gas mixer (11), lb/hr
V(IP+2) = Temperature of fluid exiting water separator (10) and going to gas mixer (11), °F
V(IV+1) = Heat added, Btu/hr
V(IV+3) = Condensate removed in water separator, lb/hr

The following inputs/outputs relate to the gas mixer (component 11) for flow to condenser heat exchanger fan:

VV(11,1) = Total flow from gas mixer (11) to condenser heat exchanger fan (12), lb/hr
VV(IP+2) = Temperature of fluid flowing from gas mixer (11) to condenser heat exchanger fan, °F

The following inputs/outputs relate to the condenser heat exchanger fan:

VV(12,1) = Total flow exiting condenser heat exchanger fan (12), lb/hr
V(IP+2) = Temperature of fluid flowing from condenser heat exchanger fan, °F
V(IV+1) = Total heat added to gas stream, Btu/hr
V(IV+12) = Volumetric flow through fan (12), cfm

The following inputs/outputs relate to the splitter (component 14) for flow to SAWD beds:

VV(14,1) = Total flow to SAWD bed #1 from splitter (14), lb/hr
V(IS+1) = Total flow to SAWD bed #2 from splitter (14), lb/hr
V(IV+1) = Split ratio in splitter (14) for flow to SAWD beds.

The following inputs/outputs relate to the gas mixer (component 15) for flow to SAWD bed #1:

VV(15,1) = Total flow to SAWD bed #1 from gas mixer (15), lb/hr
V(IP+2) = Temperature of fluid exiting gas mixer (15) and going to SAWD bed #1, °F

3.7 ARSS Subroutine (Continued)

The following inputs/outputs relate to SAWD bed #1 (component 16):

VV(16,1) = Total flow exiting SAWD bed #1, lb/hr
 V(IP+2) = Temperature of fluid exiting SAWD bed #1, °F
 V(IP+4) = Outlet pressure at SAWD bed #1, psia
 V(IV+6) = Gas stream total sensible heat change in bed #1,
 Btu/hr
 **KK(16,16) = Absorb/desorb flag (0=absorb, 1=desorb).
 **V(IV+9) = Total water evaporation/condensation rate (pph)
 V(IV+16) = Total water in SAWD bed #1 at start of transient,
 lbs
 V(IV+17) = Total CO₂ in SAWD bed #1 at start of transient, lbs

The following inputs/outputs relate to the splitter (component 17) for flow from SAWD bed #1:

VV(17,1) = Total flow exiting splitter (17) which goes to the
 condenser heat exchanger, lb/hr
 V(IS+1) = Total flow exiting splitter (17) which goes to
 CO₂ recovery, lb/hr
 V(IV+1) = Split ratio in splitter (17).

The following inputs/outputs relate to the SAWD bed fan (component 19):

VV(19,1) = Total flow through SAWD bed fan (19), lbm/hr
 V(IP+2) = Temperature of flow exiting SAWD bed fan, °F
 V(IV+1) = Total heat added to gas stream, Btu/hr
 V(IV+12) = SAWD bed fan volumetric flow rate, cfm

The following inputs/outputs relate to the gas mixer (component 20) for flow to SAWD bed #2:

VV(20,1) = Total flow from gas mixer (20) which sends steam or
 cabin gas to SAWD bed #2 inlet, lb/hr
 V(IV+2) = Temperature of flow from gas mixer (20), °F

The following inputs/outputs relate to SAWD bed #2 (component 21):

VV(21,1) = Total flow exiting SAWD bed #2, lb/hr
 V(IP+2) = Temperature of fluid exiting SAWD bed #2, °F
 V(IP+4) = SAWD bed #2 outlet pressure, psia
 V(IV+6) = Gas stream total sensible heat change, Btu/hr
 **KK(21,16) = Absorb/desorb flag (0=absorb, 1=desorb).
 **V(IV+9) = Total water evaporation/condensation rate, lb/hr
 V(IV+16) = Total water in SAWD bed #2 at start of transient,
 lbs
 V(IV+17) = Total CO₂ in SAWD bed #2 at start of transient, lbs

3.7 ARSS Subroutine (Continued)

The following inputs/outputs relate to the splitter (component 22) for flow from SAWD bed #2:

VV(22,1) = Total flow exiting splitter (22) which goes to condenser heat exchanger, lb/hr
 V(IS+1) = Total flow exiting splitter (22) which goes to CO₂ recovery, lbm/hr
 V(IV+1) = Split ratio in splitter (22)

The following inputs/outputs relate to the splitter (component 24) for flow from gas mixer (23):

VV(24,1) = Total flow exiting splitter (24) to CO₂ accumulator, lb/hr
 V(IS+1) = Total flow exiting splitter (24) to gas mixer (25), lb/hr

The following inputs/outputs relate to the splitter (component 26) for flow from gas mixer (25):

VV(26,1) = Total flow of steam from splitter (26) to SAWD bed #1, lb/hr
 V(IS+1) = Total flow of steam from splitter (26) to SAWD bed #2, lb/hr

The following inputs/outputs relate to the water supply tank (component 27):

VV(27,1) = Total flow from water supply tank (27) to steam generator, lb/hr
 V(IP+2) = Temperature of flow from water supply tank, °F
 V(IEX+1) = Total water used, lb/hr
 V(IEX+2) = Total water added, lb/hr

The following inputs/outputs relate to the water supply pump (component 28):

VV(28,2) = Temperature of water exiting water supply pump (28) for steam generator, °F
 V(IV+1) = Total heat added to water in pump (28), Btu/hr

The following inputs/outputs relate to the steam generator (component 29):

VV(29,2) = Temperature of steam exiting steam generator (29) °F
 *V(IV+4) = Electric energy required by steam generator, watts. It is multiplied by 3.413 to convert it to Btu/hr before it becomes output.

3.7 ARSS Subroutine (Continued)

The following inputs/outputs relate to the splitter (component 30) for flow from gas mixer (24):

VV(30,1) = Total flow exiting splitter (30) to CO₂ accumulator, lb/hr
 V(IS+1) = Total flow exiting splitter (30) to cabin, lb/hr
 V(IS+2) = Temperature of fluid exiting splitter (30) to cabin, °F
 V(IV+1) = Ratio of flow directed to cabin to total inlet flow in splitter (30).

The following inputs/outputs relate to the gas mixer (component 31) for flow to condensing heat exchanger (7):

VV(31,1) = Total flow exiting gas mixer (31) to humidity control heat exchanger (7), lb/hr
 V(IP+2) = Temperature of fluid exiting gas mixer (31) to humidity control heat exchanger, °F

The following inputs/outputs relate to the CO₂ accumulator (component 32):

VV(32,1) = Total flow exiting CO₂ accumulator (32) to overboard or CO₂ reduction, lb/hr
 V(IP+2) = Temperature of fluid exiting CO₂ accumulator, °F
 V(IV+5) = Total fluid weight in CO₂ accumulator, lbm
 V(IV+8) = CO₂ accumulator pressure, psia.

The following input relates to gas mixer (component 18):

**VV(18,6) = Condensable vapor flow exiting gas mixer (18), lb/hr

The following input relates to the splitter (component 3) for flow from the cabin:

**VV(3,25) = Condensable vapor flow exiting splitter (3) and flowing to SAWD system.

The following are output only of ARSS:

TIMEM = Time into transient in minutes. It is calculated by dividing the input TIME (seconds) by 60.
 TIMEH = Time into transient in hours. It is calculated by dividing the input TIME (seconds) by 3600.
 QMET = Total metabolic heat per crewman, Btu/hr. It is the total of the input sensible and latent heats per crewman.

3.7 ARSS Subroutine (Continued)

QNELAT	= Latent heat added to cabin by non-ECLS and non-metabolic sources, ie, vehicle loads, Btu/hr.
V1076	= 9.0 = water separator power, Btu/hr
Q16	= Latent heat released due to condensation during desorption or sensible heat used for evaporation during absorption in SAWD bed #1, Btu/hr
Q21	= Latent heat released due to condensation during desorption or sensible heat used for evaporation during absorption in SAWD bed #2, Btu/hr
QESEN	= Total power required by ECLS components, Btu/hr
QELAT	= Total latent heat added to cabin from ECLS sources, i.e., the SAWD system, Btu/hr

The following are outputs which cause A's, C's or S's which represent air, carbon dioxide, and steam flows, respectively to be printed at the proper places and times on the output schematic:

L1	= Flow stream into SAWD bed #1
L2	= Flow stream out of SAWD bed #1 to splitter (17)
L3	= Flow stream between splitter (17) and gas mixer (23) which ultimately goes to bed #2, the cabin, or the CO ₂ accumulator.
L4	= Flow stream into SAWD bed #2
L5	= Flow stream out of SAWD bed #2 to splitter (22)
L6	= Flow stream between splitter (22) and gas mixer (23) which ultimately goes to bed #1, the cabin, or the CO ₂ accumulator.
L7	= Flow stream between splitter (24) and the CO ₂ accumulator.
L8	= Flow stream between splitter (30) and the cabin.

 3.8 IR45 Subroutines

This group of subroutines computes the transient performance of a SAWD canister which includes the inlet header, the bed, an exit header, and an exit temperature sensor. The bed itself can be divided into as many as five segments.

The computational sequence for subroutine IR45 is shown in Figure 7. At the start of the subroutine, values of resin weight, carbon dioxide weight, water weight, canister weight, void volume, and foam weight are computed for each segment of the bed. This is done only the first time that the IR45 subroutine is called in ESCM. If steady state analyses are to be done, subroutine STAEDY is called; if not, the program begins the transient IR45 analysis with a call to subroutine HEADER. In that subroutine, the mixed temperature and composition of the gases in the inlet header are computed. From there, the gases enter the first segment of the bed. Subroutine BALNCE performs a mass, energy, and pressure balance on the gas and

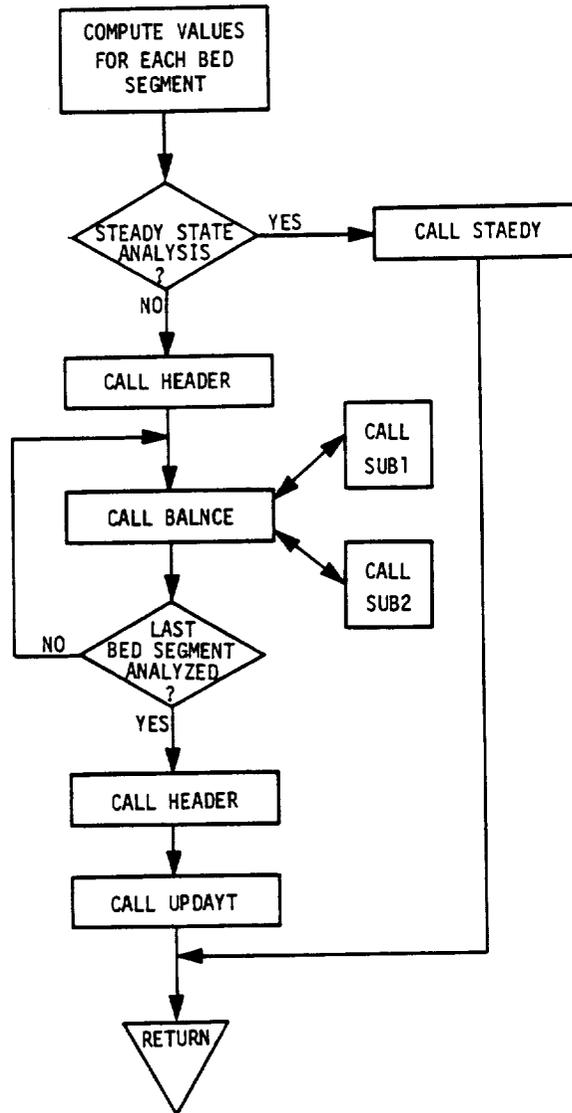


Figure 7
Subroutine IR45 Flow Diagram

3.8 IR45 Subroutines (Continued)

water and carbon dioxide loadings in the resin for a bed segment. BALNCE calls subroutine SUB1 to compute the sum of the enthalpies at any temperature for the entering or exiting gas, resident gas, resin, and canister metal; BALNCE calls SUB2 to compute the partial pressures of water and carbon dioxide in the bed voids, and to compute the rate constant for CO₂ loading. The temperature and composition of the gas leaving the first segment are computed in BALNCE. This subroutine is repeated for all segments. When all the segments have been analyzed, subroutine HEADER is called to compute the temperature and composition of the gas leaving the exit header. The last subroutine called is UPDAYT. There, the "R" array values are updated for the analyzed time step, and the effect of the temperature sensor time constant on sensed temperature is computed.

IR45 is the main subroutine which simulates a SAWD bed; the subroutine calls the other subroutines. Since IR45 is the main subroutine and represents the SAWD bed to the ESCM, only the input and output to this subroutine are presented in the following.

A array data and R array data up to R(64) [R(1) to R(64)] are always the same. Only the component to which they refer changes.

A Array Data (Input/Output)

The A array [A(1) to A(19)] contains the primary source flow data (upstream component flow data which enters the primary side of the component being solved (SAWD bed #1 or #2 in the IR45 subroutine). The specific inputs for each array position may be found in the G189 Manual (Table 2-1, page 2-12).

R Array Data (Input/Output)

R array locations R(1) to R(19) contain the exit flow data for the primary side of the current component being solved (SAWD bed #1 or #2 in IR45). This is the same as the A array data except that it involves exit rather than source flows. The specific inputs for R(1) to R(19) may be found in the G189 Manual (page 2-12 or 2-15).

R(20) to R(62) are not used in the IR45 subroutine. R(63) and R(64) are used. They are always the same as mentioned above. Only the component to which they refer changes (see page 2-19 of G189 Manual). In the IR45 subroutine they refer to SAWD bed #1 or #2.

R(63) = Exterior surface temperature (°F)
R(64) = Conductance between source (bed) and exterior
(Btu/hr-°F)

3.8 IR45 Subroutines (Continued)
R(65) to R(95)

These are subroutine dependent data. Inputs to these positions depend upon the subroutine being used (in this case IR45). In IR45 the R(65) to R(95) refer to the following in the SAWD beds:

R(65)	= Heat of CO ₂ reaction with resin bed (Btu/lb)
R(66)	= Specific heat of dry resin bed (Btu/lb-°F)
R(67)	= Density of dry resin bed (lb/ft ³)
R(68)	= Resin bed void volume fraction (ft ³ /ft ³)
R(69)	= Time required to complete steam desorb (sec)
R(70)	= Gas stream total sensible heat change (Btu/hr)
R(71)	= Gas stream total latent heat change (Btu/hr)
R(72)	= Carbon dioxide absorption rate (lb/hr)
R(73)	= Water absorption rate (lb/hr)
R(74)	= Basepoint absorption/desorption rate (pph of CO ₂ /lb of dry resin/psi of CO ₂ partial pressure difference).
R(75)	= Average steady state desorption steam rate (lb/hr)
R(76)	= Steady state carbon dioxide removal efficiency.
R(77)	= Average steady state bed temperature (°F)
R(78)	= Total dry resin bed weight (lbm)
R(79)	= Total canister weight (lbm)
R(80)	= Total water in bed (lbm)
R(81)	= Total carbon dioxide in bed (lbm)
R(82)	= Total bed water loading (lbm H ₂ O/lb bed)
R(83)	= Total bed carbon dioxide loading (lb CO ₂ /lb bed)
R(84)	= Specific heat of canister (Btu/lbm-°F)
R(85)	= Temperature to end desorption (°F)
R(86)	= Time at which absorption is to end (sec)
R(87)	= Outlet temperature time lag (sec)
R(88)	= Bed inlet dew point (°F)
R(89)	= Bed exit dew point (°F)
R(90)	= Bed inlet carbon dioxide partial pressure (mmHg)
R(91)	= Bed exit carbon dioxide partial pressure (mmHg)
R(92)	= Total bed exit flow (ft ³ /min)
R(93)	= Total foam in bed (lbm)
R(94)	= Specific heat of foam (Btu/lbm-°F)
R(95) to R(99)	= are spare positions in the array.

The following R array positions are used for each segment that the SAWD beds are divided into for calculation purposes: In the following $J=99+30*(k-1)$ and $k=1$ thru number of bed segments used.

R(J+I)	= Same as A(I) array
R(J+20)	= Segment k bed temperature (°F)
R(J+21)	= Segment k bed carbon dioxide weight (lbm)
R(J+22)	= Segment k bed water weight (lbm)
R(J+23)	= Segment k bed weight (lbm)

3.8 IR45 Subroutines (Continued)

R(J+24)	= Segment k canister weight (lbm)
R(J+25)	= Segment k void volume (ft ³)
R(J+26)	= Segment k carbon dioxide loading (lb CO ₂ /lb bed)
R(J+27)	= Segment k water loading (lb H ₂ O/lb bed)
R(J+28)	= Segment k foam weight (lbm)
R(J+29) and R(J+30)	= Spares.

4.0 PROGRAM USE

Instructions to access ESCM and to use the program are presented in this section. ESCM may be run interactively at a terminal or run by submitting batch jobs. Of course the job control language will vary from computer system to computer system. Also, several subroutines will be different from system to system. The job control language and subroutines described in section 4.1 apply to the IBM 3080 series computer with the MVS 3.8 Operating System. Section 4.2 describes how the ESCM program must be modified to operate on the LaRC PRIME computers under FORTRAN 77.

4.1 Operation Using Hamilton Standard's IBM 3080 Series Computer

To run ESCM, use the following sequence of steps:

(1) Access the desired command list:

- | | |
|------------------|----------------------|
| (a) ESCMCN CNTL | (to run batch job) |
| (b) ESCMCL CLIST | (to run interactive) |

(2) Access input data set: ESCM2B.DATA

(3) Make desired changes to ESCM2B.DATA

(4) For batch jobs, SUBMIT ESCMCN; for interactive jobs, EX ESCMCL.

4.1.1 Accessing Desired Job Control List

After logging onto the computer time sharing system, either ESCMCN or ESCMCL must be accessed from the library and brought into the User's file. The following are the commands to do this:

```
LC ESCMCN CNTL SO(G15UARL) RON
LGCL ESCMCL G15UARL RON
```

A listing of each is given in Appendix A. Input output files are allocated by these control lists; Table 7 presents these assignments. The program has been coded in such a fashion as to facilitate changes in I/O assignments to conform to individual computer installations. This was accomplished by using variable unit names

Table 7
ESCM I/O File Assignments For IBM Computer

<u>FORTAN Variable Unit Name</u>	<u>Current FORTAN Logical Unit Number</u>	<u>File Type</u>	<u>Physical Unit Assignment</u>	
NDA	1	Scratch		Contains card images of all input data cards. Editing and processing take place from this file.
NDB	2	Scratch	These four files may use	Used during Basic Case in conjunction with NDC and NDB to process cards. At all other times, contains edited Basic Case K/V array.
NDC	3	Scratch	Tape, Disk or Drum Units	Used during Basic Case input operations with NDB to process K and V Component Data card images. Used to store processed SD-4060 plot data at conclusion of G189A case.
NDD	4	Scratch		Used during Basic Case with NDB to process Table Data card images. May be used for SD-4060 operations.
NDE	16	Output	Tape	Output file for G189A plot data to be processed by post Processor plot package (Section 10 of Reference 3).
NTIN	10	Input	Tape	Input file for the data tape.
NTOUT	11	Output	Tape	Output file for the data tape.
NSTUFF	31	Output	Card Punch	Used to punch card images of the edited simulation data.
---	20	Output	Terminal	Output to terminal screen.

4.1.1 Accessing Desired Job Control List (Continued)

in all FORTRAN I/O statements, eg, WRITE(NDA,30)K. The variable unit names are made available to the appropriate subprograms in the common block /FILES/. The numerical values for the variable unit names are set in the block data subroutine DBLOCK. For more information, see Reference 3. The only file that is not set up in the above fashion is file 20 which is only used in subroutine ARSS.

4.1.2 Input Data

Input to the program is made through the data set ESCM2B. To access this data set from Librarian, enter:

```
LG ESCM2B DATA SO(G15UARL)
```

A copy of ESCM2B is shown in Table 8. The input and values specified in Table 8 are the recommended values and set up for the ESCM application using G189A. The input follows that required for G189A; the user should refer to Reference 3 for more detailed information.

The input is divided into four groups of cards: case data, K and V component data, table data and plot data. The following sections briefly describe the input data required for each of these sections specific for the ESCM, the user again should refer to the G189A Manual, Reference 3, for a complete and general description of the input. For convenience, Figure 8 is provided to show the general input setup and the case data required.

4.1.2.1 Case Data Group

The case data group contains such data as necessary to specify the overall data storage arrangement, describe the model in general, and control the execution of the case. The group also contains fluid property data. Since the publication of Reference 3, an additional input has been added to this group, and it is the first record for the group.

Record 1

	<u>FORMAT</u>	<u>COLS</u>
1) Type of printout desired:	I4	1-4
IOUT=0=print input data and input echo		
IOUT=1=print input data only		
IOUT=2= print input echo only		
IOUT=3=print neither input data nor echo		

Table 8
 Input to ESCM

**** TSO FOREGROUND HARDCOPY **** 14:55:21 85030
 DSNAME=TSOGL156.ESCM2B.DATA

0 0 PRINT INPUT DATA AND SCHEMATICS
 **** NAMELIST, BASIC CASE
 TAPE
 BASIC 1 50 13 2 YEA NAY
 CASE ESCM: BASELINE, VOL=8000 FT-3, PCO2=2.5, .275 PPH AVG

\$CASE1
 KPTINV(1)= 1, KPTINV(2)= 5, KPTINV(3)= 10, KPTINV(4)=30,
 KCHOUT= 0, KPUNCH= 0, KPRNT= 0, KRUN= 1, KSTEDY= 0,
 MAXSLP= 4, MAXSSI= 15, MINSSI= 10, NOLIM=0,
 DTIME=15., START= 0.0, TIMEMX= 86400.,
 TMAX= 325.0, TMIN= 0.0, WTMAX= 1.6E6 \$END

\$PROPI
 CP(1)=1., RHO(1)=62.4, VISC(1)=2.42, WTM(1)=18.016, XK(1)=0.34,
 CP(2)=0.2, RHO(2)=0.00045, VISC(2)=0.378, WTM(2)=44.01, XK(2)=0.0098,
 CPCONL=1., CPCONV=0.445, CPCO2=0.2, CPDIL=0.25, CPOXY=0.22, CPTC=0.2,
 GAMGAS=1.4, VISCAS=.44, WTMCON=18.016, WTM DIL=28.013, WTMTC=20.,
 XKGAS=0.146 \$END

ID** 1 ARS DEMO MODEL FOR SAWD II GENERAL NOTES:
 ID** 1 10 FLUID TYPE CODES --
 ID** 1 11 1 = WATER
 ID** 1 12 2 = CO2 GAS @ 70 F, 3 MM HG
 ID** 1 90
 ID** 1 100 CREW METABOLIC SIMULATION
 KBAS 1 2 1 5 2 14 2
 NSTR 1 0 1 NO TESTS, SS CALCS
 VARY 1 2 50.0 TEMP (F)
 VARY 1 3 14.7 4 PRESS (PSIA)
 VARY 1 6 87.8 H2O VAPOR FLOW (LB/HR)
 VARY 1 10 2046.9 OXYGEN FLOW (LB/HR)
 VARY 1 11 7200.7 NITROGEN FLOW (LB/HR)
 VARY 1 12 46.7 CO2 FLOW (LB/HR)
 KARY 1 16 3 NUMBER OF CREWMEN
 VARY 1 65 TOTAL METABOLIC HEAT - ALL CREWMEN (BTU/HR)
 VARY 1 66 291.7 SENSIBLE HEAT PER CREWMAN (BTU/HR)
 VARY 1 67 175.2 LATENT HEAT PER CREWMAN (BTU/HR)
 VARY 1 68 TOTAL OXYGEN USE RATE (LB/HR)
 VARY 1 69 TOTAL CO2 GENERATION RATE (LB/HR)
 VARY 1 70 TOTAL H2O VAPOR GENERATION RATE (LB/HR)
 VARY 1 75 INLET GAS RELATIVE HUMIDITY (DECIMAL)
 VARY 1 76 INLET GAS DEW POINT (F)
 VARY 1 77 OUTLET GAS RELATIVE HUMIDITY(DECIMAL)
 VARY 1 78 OUTLET GAS DEW PONT (F)
 VARY 1 82 TOTAL METABOLIC RATE PER CREWMAN (BTU/HR)
 ID** 2 MAIN CABIN
 KBAS 2 1 25 1 2 -13 2 3 2
 NSTR 2 151011000 PRI P, 5 RESETS, SPECIFY NET FLOWS
 VARY 2 2 70. CABIN GAS MIXTURE: INITIAL TEMP (F)
 VARY 2 3 14.7 4 TOTAL PRESSURE (PSIA)
 VARY 2 6 89.7 H2O VAPOR FLOW (LB/HR)
 VARY 2 10 2046.8 OXYGEN FLOW (LB/HR)
 VARY 2 11 7199.4 NITROGEN FLOW (LB/HR)
 VARY 2 12 46.3 CO2 FLOW (LB/HR)
 VARY 2 21 70. CABIN GAS MIXTURE: INITIAL TEMP (F)



START OF
 OF K AND V
 COMPONENT
 DATA

Table 8 (Continued)
Input to ESCM

VARY	2	22	14.7	23	TOTAL PRESSURE (PSIA)
VARY	2	25	13.00		H2O VAPOR FLOW (LB/HR)
VARY	2	29	303.76		OXYGEN FLOW (LB/HR)
VARY	2	30	1068.67		NITROGEN FLOW (LB/HR)
VARY	2	31	9.45		CO2 FLOW (LB/HR)
VARY	2	65			TOTAL HEAT ADDED TO CABIN GAS MIXTURE (BTU/HR)
VARY	2	66	17065.		CABIN HEAT LOAD (BTU/HR) = 5 KW
VARY	2	71			HEAT LOSS DUE TO OUTBOARD LEAKAGE (BTU/HR)
VARY	2	72			HEAT GAIN DUE TO MASS ADDITIONS (BTU/HR)
VARY	2	73			HEAT REQ'D TO FLASH ENTRAINED H2O (BTU/HR)
VARY	2	74			FLASH EVAPORATION RATE OF ENTRAINED H2O (LB/HR)
VARY	2	87	70.0		CABIN GAS DESIGN TEMP (F) (4 MEN)
VARY	2	88	10.0		CABIN GAS DESIGN TEMP TOL (F) (4 MEN)
VARY	2	89			CABIN GAS RELATIVE HUMIDITY (DECIMAL)
VARY	2	90	14.7		DESIGN TOTAL PRESSURE (PSIA)
VARY	2	91	0.5		DESIGN TOTAL PRESSURE TOL (PSIA)
VARY	2	92	2.9		DESIGN OXYGEN PRESSURE (PSIA)
VARY	2	93	0.5		DESIGN OXYGEN PRESSURE TOL (PSIA)
VARY	2	94			CABIN GAS OXYGEN PRESSURE (PSIA)
VARY	2	95			CABIN GAS NITROGEN PRESSURE (PSIA)
VARY	2	96	50.0		DESIGN DEW POINT (F)
VARY	2	97	30.0		DESIGN DEW POINT TOL (F)
VARY	2	98			CABIN GAS DEW POINT (F)
VARY	2	99	20.		MAX ALLOWABLE CO2 PRESSURE (MM HG)
VARY	2	100			CABIN GAS CO2 PRESSURE (MM HG)
VARY	2	101	250.		MAX ALLOWABLE TRACE CONTAMINANT LEVEL (PPM)
VARY	2	102			CABIN GAS TRACE CONTAMINANT LEVEL (PPM)
VARY	2	103			CABIN GAS MIXTURE, TOTAL MASS (LB)
VARY	2	104			CABIN GAS MIXTURE, TEMPERATURE (F)
VARY	2	105			CABIN GAS MIXTURE, TOTAL PRESSURE (PSIA)
VARY	2	107			CABIN GAS MIXTURE, NON-CONDENSABLES MASS (LB)
VARY	2	108			CABIN GAS MIXTURE, H2O VAPOR MASS (LB)
VARY	2	109			CABIN GAS MIXTURE, ENTRAINED H2O MASS (LB)
VARY	2	110			CABIN GAS MIXTURE, NON-COND. SPECIFIC HEAT (BTU/LB-F)
VARY	2	111			CABIN GAS MIXTURE, NON-COND. MOL WEIGHT (LB/MOL)
VARY	2	112			CABIN GAS MIXTURE, OXYGEN MASS (LB)
VARY	2	113			CABIN GAS MIXTURE, NITROGEN MASS (LB)
VARY	2	114			CABIN GAS MIXTURE, CO2 MASS (LB)
VARY	2	115			CABIN GAS MIXTURE, TRACE CONTAMINANTS MASS (LB)
VARY	2	122	0.0833		OUTBOARD LEAKAGE RATE (LB/HR)
VARY	2	123			NON-CONDENSABLES LEAKAGE RATE (LB/HR)
VARY	2	124			H2O VAPOR LEAKAGE RATE (LB/HR)
VARY	2	125			ENTRAINED H2O LEAKAGE RATE (LB/HR)
VARY	2	126			TOTAL MASS ADDITION RATE (LB/HR)
VARY	2	127			NON-COND. ADDITION RATE (LB/HR)
VARY	2	128	0.233		H2O VAPOR ADDITION RATE (LB/HR)
VARY	2	129	0.0		ENTRAINED H2O ADDITION RATE (LB/HR)
VARY	2	130			AVERAGE TEMPERATURE OF MASS ADDITIONS (F)
VARY	2	132	70.0		ADD COND VAPOR TEMP (F)
VARY	2	135			NET TOTAL FLOW INTO CABIN (LB/HR)
VARY	2	136			NET NON-COND. FLOW INTO CABIN (LB/HR)
VARY	2	137			NET H2O VAPOR FLOW INTO CABIN - CALC IN GPOLY2
VARY	2	139	8000.		CABIN FREE VOL (FT3)
VARY	2	170	70.0		OXYGEN ADDITION TEMP (F)
VARY	2	171	70.0		NITROGEN ADDITION TEMP (F)
VARY	2	172	70.0		CO2 ADDITION TEMP (F)
VARY	2	173	70.0		TRACE CONTAMINANTS ADDITION TEMP (F)
VARY	2	174	70.0		SPECIAL FLOW NO. 1 ADDITION TEMP (F)
VARY	2	175			NET O2 ADDITION (LB/HR) - GPOLY2 CALC
VARY	2	176			NET N2 ADDITION (LB/HR) - GPOLY2 CALC

 CONTINUATION
OF K AND V
COMPONENT
DATA

Table 8 (Continued)
 Input to ESCM

VARY	2	177	0.0	NET CO2 ADDITION (LB/HR)			
VARY	2	178	0.0	NET TRACE CONTAMINANTS ADDITION (LB/HR)			
VARY	2	179	0.0	NET SPEC FLOW 1 ADDITION (LB/HR)			
VARY	2	180	0.0	O2/N2 REG FLAG = 0.0 IF O2 USED LAST, = 1.0			
VARY	2	181		MISSION TIME (SEC)			
VARY	2	182		MISSION TIME (MIN)			
VARY	2	183	1.0	SAWD ABSORB CYCLE TIME CURVE MULTIPLY FACTOR			
VARY	2	184	8.0	PRINTOFF FREQUENCY, TIME STEPS PER PRINTOFF			
ID**	3			SPLIT - MAIN CABIN HUMIDITY CONTROL HX OR TO SAWD-II		4	2
KBAS	3		10		-2 2	2	
NSTR	3						
VARY	3	65	0.04866	SPLIT RATIO - GPOLY1 CALC			
ID**	4			MAIN CABIN SENSIBLE HX FAN		5	2
KBAS	4		23		2 2		
NSTR	4		1	INPUT CFM & Q			
VARY	4	76	2100.	CABIN FAN VOLUMETRIC FLOW RATE (CFM)			
VARY	4	84	1.0	FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)			
VARY	4	91	833.	FAN HEAT ADDITION (WATTS)			
ID**	5			MAIN CABIN SENSIBLE HX - SENSIBLE HEAT REMOVAL ONLY		1	2
KBAS	5		4		4 2	-6 0 1	
NSTR	5		2 0	COUNTERFLOW, PRI=GAS, SEC=LIQ, SS CALC			
VARY	5	66	6240.	HX COUNTERFLOW UA (BTU/HR-F)			
ID**	6			COOLING FLUID BOUNDARY COND - CABIN SENSIBLE HX			2
KBAS	6		49 2		0 1		
NSTR	6						
VARY	6	1	1350.	COOLANT FLOW (LB/HR) - GPOLY1 CALC			
VARY	6	2	60.0	COOLANT TEMP (F)			
VARY	6	3	50.0	COOLANT PRESSURE (PSIA)	4		
KARY	6	16		KPRNT VALUE AT START OF TRANSIENT (GPOLY1)	0		
KARY	6	17		KCHOUT VALUE AT START OF TRANSIENT (GPOLY1)	0		
ID**	7			MAIN CABIN CONDENSING HX		9	2
KBAS	7		4		31 2	-8 0 1	
NSTR	7		2 0	INPUT EFF, PRI=GAS, SEC=LIQ, SS CALCS			
VARY	7	66	1000.	COUNTERFLOW HX UA (BTU/HR-F) - GPOLY1 CALC			
ID**	8			COOLING FLUID BOUNDARY COND - CABIN COND HX			2
KBAS	8		49		0 1		
NSTR	8						
VARY	8	1	950.	COOLANT FLOW (LB/HR)			
VARY	8	2	45.0	COOLANT TEMP (F)			
VARY	8	3	50.0	COOLANT PRESSURE (PSIA)	4		
ID**	9			SPLIT - COND HX TO WATER SEPARATOR BYPASS, WATER SEPARATOR		10	2
KBAS	9		10 7		7 2	2	
NSTR	9		1	SPECIFY INDIVIDUAL SPLIT RATIOS			
VARY	9	66	0.03	SPLIT RATIO - COND VAPOR			
VARY	9	67	1.00	SPLIT RATIO - COND LIQUID			
VARY	9	68	0.03	SPLIT RATIO - OXYGEN			
VARY	9	69	0.03	SPLIT RATIO - NITROGEN			
VARY	9	70	0.03	SPLIT RATIO - CARBON DIOXIDE			
VARY	9	71	0.03	SPLIT RATIO - TRACE CONTAMINANTS			
VARY	9	72	0.03	SPLIT RATIO - SPECIAL FLOW #1			
ID**	10			WATER SEPARATOR - CABIN COND HX		11	2
KBAS	10		49 1		-9 2		
NSTR	10		2	CALC EXIT TMEP GIVEN Q			
VARY	10	65		HEAT ADDED (BTU/HR) - GPOLY1 CALC			
VARY	10	67		CONDENSATE REMOVED (LB/HR) - GPOLY1 CALC			
ID**	11			GASMIX - COND HX WATER SEPARATOR, WATER SEPARATOR BYPASS		12	2
KBAS	11		6		9 2	-10 2	
NSTR	11						
ID**	12			COND HX FAN		13	2
KBAS	12		23		11 2		

 CONTINUATION
 OF K AND V
 COMPONENT
 DATA

Table 8 (Continued)
Input to ESCM

			INPUT CFM & Q	
NSTR	12	1		
VARY	12	76 300.	CABIN FAN VOLUMETRIC FLOW RATE (CFM)	
VARY	12	84 1.0	FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)	
VARY	12	91 140.	FAN HEAT ADDITION (WATTS)	
ID**	13	GASMIX - SAWD-II AND COND HX FAN	30 2	2 2
KBAS	13	6	12 2	
NSTR	13			
ID**	14	SPLIT - MAIN CABIN TO SAWD BED #1, SAWD BED #2		27 2
KBAS	14	10	-3 2	
NSTR	14			
VARY	14	65 0.0	SPLIT RATIO - GPOLYI CALC	
ID**	15	GASMIX - STEAM OR CABIN GAS TO SAWD BED #1 INLET		16 2
KBAS	15	6	14 2	
NSTR	15			
ID**	16	SAWD BED #1 SIMULATION - ALTCOM		17 2
KBAS	16	73 0 0	15 2	
NSTR	16			
KARY	16	16	0	ABSORB/DESORB FLAG (0 = ABSORB, 1 = DESORB)
KARY	16	17	21	COMPLEMENTARY BED'S COMPONENT NO.
KARY	16	18	0	DESORBING FLOW REVERSAL FLAG: 1=YES, 0=NO
KARY	16	19	5	NUMBER OF BED SEGMENTS
KARY	16	20	15	DOWNSTREAM COMPONENT NUMBER
VARY	16	60 70.0		AMBIENT TEMPERATURE (F)
VARY	16	61 0.8		CAN-TO-AMBIENT KA/X (BTU/HR-F)
VARY	16	63 70.0		EXTERIOR SURFACE TEMPERATURE, (DEG-F)
VARY	16	64 0.800		CONDUCTANCE BETWEEN BED AND EXTERIOR, (BTU/HR-F)
VARY	16	65 1270.		HEAT OF CO2 REACTION WITH RESIN BED (BTU/LB)
VARY	16	66 0.314		SPECIFIC HEAT OF DRY IR45 RESIN, (BTU/LB-F)
VARY	16	67 32.70		DENSITY OF DRY RESIN BED, (PCF)
VARY	16	68 0.319		RESIN BED VOID VOLUME FRACTION
VARY	16	69 10.0		TIME REQUIRED TO COMPLETE STEAM DESORB (SEC)
VARY	16	70		GAS STREAM TOTAL SENSIBLE HEAT CHANGE (BTU/HR)
VARY	16	71		GAS STREAM TOTAL LATENT HEAT CHANGE (BTU/HR)
VARY	16	72		TOTAL CO2 ABSORPTION(+)/DESORPTION(-) RATE (PPH)
VARY	16	73		TOTAL H2O EVAPORATION(+)/CONDENSATION(-) RATE (PPH)
VARY	16	74 1.500		ABSORPTION/DESORPTION RATE (PPH OF CO2/LB-BED/PSI)
VARY	16	75 0.400		AVG. STEADY STATE DESORPTION STEAM RATE (PPH)
VARY	16	76 0.604		STEADY STATE CO2 REMOVAL EFFICIENCY
VARY	16	77 70.00		AVG. STEADY STATE BED TEMPERATURE, (DEG-F)
VARY	16	78 8.500		TOTAL DRY RESIN BED WEIGHT (LBM)
VARY	16	79 7.400		TOTAL CANISTER WEIGHT (LBM)
VARY	16	80 2.550		TOTAL WATER IN BED (LBM)
VARY	16	81 0.005		TOTAL CO2 IN BED (LBM)
VARY	16	82		TOTAL BED H2O LOADING (LB H2O/LB BED)
VARY	16	83		TOTAL BED CO2 LOADING (LB CO2/LB BED)
VARY	16	84 0.120		SPECIFIC HEAT OF CANISTER (BTU/LB-F)
VARY	16	85 180.0		EXIT TEMPERATURE TO END DESORPTION, DEG-F
VARY	16	86 2280.		TIME TO END ABSORPTION, SECONDS
VARY	16	87 240.		TIME LAG FOR OUTLET TEMPERATURE, SECONDS
VARY	16	88		BED INLET DEW POINT, DEG-F
VARY	16	89		BED EXIT DEW POINT, DEG-F
VARY	16	90		BED INLET CO2 PARTIAL PRESSURE, MM-HG
VARY	16	91		BED EXIT CO2 PARTIAL PRESSURE, MM-HG
VARY	16	92		TOTAL BED EXIT FLOW, CFM
VARY	16	93 0.470		TOTAL WEIGHT OF FOAM IN BED, LBM
VARY	16	94 0.330		SPECIFIC HEAT OF FOAM BTU/LB-F
VARY	16	95 100000.		TIME TO BEGIN DEBUG PRINTOFF, SECONDS.
ID**	17	SPLIT - SAWD BED #1 TO COND HX OR CO2 RECOVERY		20 2
KBAS	17	10	16 2	
NSTR	17			

 CONTINUATION
OF K AND V
COMPONENT
DATA

Table 8 (Continued)
 Input to ESCM

VARY	17	65	0.0	SPLIT RATIO - GPOLY1 CALC			
ID**	18	GASMIX - SAWD BED #1, SAWD BED #2				19	2
KBAS	18	6		17	2	-22	2
NSTR	18						
ID**	19	SAWD BED FAN				30	2
KBAS	19	23		18	2		
NSTR	19	003 INPUT Q ONLY					
VARY	19	2	70.	CABIN GAS MIXTURE: INITIAL TEMP (F)			
VARY	19	3	14.7	4 TOTAL PRESSURE (PSIA)			
VARY	19	6	0.78	H2O VAPOR FLOW (LB/HR)			
VARY	19	10	20.55	OXYGEN FLOW (LB/HR)			
VARY	19	11	71.87	NITROGEN FLOW (LB/HR)			
VARY	19	12	0.30	CO2 FLOW (LB/HR)			
VARY	19	76	15.	CABIN FAN VOLUMETRIC FLOW RATE (CFM)			
VARY	19	84	1.0	FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)			
VARY	19	91	50.	FAN HEAT ADDITION (WATTS)			
ID**	20	GASMIX - STEAM OR CABIN GAS TO SAWD BED #2 INLET				21	2
KBAS	20	6		-14	2	26	2
NSTR	20	2					
ID**	21	SAWD BED #2 SIMULATION - ALTCOM				22	2
KBAS	21	73	0 0	20	2		
NSTR	21						
KARY	21	16		1	ABSORB/DESORB FLAG (0 = ABSORB, 1 = DESORB)		
KARY	21	17		16	COMPLEMENTARY BED'S COMPONENT NO.		
KARY	21	18		0	DESORBING FLOW REVERSAL FLAG: 1=YES, 0=NO		
KARY	21	19		5	NUMBER OF BED SEGMENTS		
KARY	21	20		20	DOWNSTREAM COMPONENT NUMBER		
VARY	21	60	70.0	AMBIENT TEMPERATURE (F)			
VARY	21	61	0.8	CAN-TO-AMBIENT KA/X (BTU/HR-F)			
VARY	21	63	70.0	EXTERIOR SURFACE TEMPERATURE, (DEG-F)			
VARY	21	64	0.800	CONDUCTANCE BETWEEN BED AND EXTERIOR, (BTU/HR-F)			
VARY	21	65	1270.	HEAT OF CO2 REACTION WITH RESIN BED (BTU/LB)			
VARY	21	66	0.314	SPECIFIC HEAT OF DRY IR45 RESIN, (BTU/LB-F)			
VARY	21	67	32.70	DENSITY OF DRY RESIN BED, (PCF)			
VARY	21	68	0.319	RESIN BED VOID VOLUME FRACTION			
VARY	21	69	10.0	TIME REQUIRED TO COMPLETE STEAM DESORB (SEC)			
VARY	21	70		GAS STREAM TOTAL SENSIBLE HEAT CHANGE (BTU/HR)			
VARY	21	71		GAS STREAM TOTAL LATENT HEAT CHANGE (BTU/HR)			
VARY	21	72		TOTAL CO2 ABSORPTION(+)/DESORPTION(-) RATE (PPH)			
VARY	21	73		TOTAL H2O EVAPORATION(+)/CONDENSATION(-) RATE (PPH)			
VARY	21	74	1.500	ABSORPTION/DESORPTION RATE (PPH OF CO2/LB-BED/PSI)			
VARY	21	75	0.400	AVG. STEADY STATE DESORPTION STEAM RATE (PPH)			
VARY	21	76	0.604	STEADY STATE CO2 REMOVAL EFFICIENCY			
VARY	21	77	70.00	AVG. STEADY STATE BED TEMPERATURE, (DEG-F)			
VARY	21	78	8.500	TOTAL DRY RESIN BED WEIGHT (LBM)			
VARY	21	79	7.400	TOTAL CANISTER WEIGHT (LBM)			
VARY	21	80	2.080	TOTAL WATER IN BED (LBM)			
VARY	21	81	0.300	TOTAL CO2 IN BED (LBM)			
VARY	21	82		TOTAL BED H2O LOADING (LB H2O/LB BED)			
VARY	21	83		TOTAL BED CO2 LOADING (LB CO2/LB BED)			
VARY	21	84	0.120	SPECIFIC HEAT OF CANISTER (BTU/LB-F)			
VARY	21	85	180.0	EXIT TEMPERATURE TO END DESORPTION, DEG-F			
VARY	21	86	2280.	TIME TO END ABSORPTION, SECONDS			
VARY	21	87	240.	TIME LAG FOR OUTLET TEMPERATURE, SECONDS			
VARY	21	88		BED INLET DEW POINT, DEG-F			
VARY	21	89		BED EXIT DEW POINT, DEG-F			
VARY	21	90		BED INLET CO2 PARTIAL PRESSURE, MM-HG			
VARY	21	91		BED EXIT CO2 PARTIAL PRESSURE, MM-HG			
VARY	21	92		TOTAL BED EXIT FLOW, CFM			
VARY	21	93	0.470	TOTAL WEIGHT OF FOAM IN BED, LBM			

 CONTINUATION
 OF K AND V
 COMPONENT
 DATA

Table 8 (Continued)
 Input to ESCM

VARY	21	94	0.330	SPECIFIC HEAT OF FOAM BTU/LB-F		
VARY	21	95	100000.	TIME TO BEGIN DEBUG PRINTOFF, SECONDS.		
ID**	22			SPLIT - SAWD BED #2 TO COND HX OR CO2 RECOVERY	23	2
KBAS	22	10		21 2		
NSTR	22			2		
VARY	22	65	1.0	SPLIT RATIO - GPOLY1 CALC		
ID**	23			GASMIX - SAWD BED #1 EXIT GAS, SAWD BED #2 EXIT GAS	24	2
KBAS	23	6		-22 2		
NSTR	23			17 2		
ID**	24			SPLIT - SAWD EXIT GAS TO PREHEAT OR TO CO2 ACCUMULATOR	18	2
KBAS	24	10		23 2		
NSTR	24			2		
VARY	24	65	0.0	SPLIT RATIO - GPOLY1 CALC		
ID**	25			GASMIX - STEAM GENERATOR AND PREHEAT STEAMS	26	2
KBAS	25	6		29 2		
NSTR	25			24 2		
ID**	26			SPLIT - STEAM TO SAWD BED #1 OR #2.	15	2
KBAS	26	10		25 2		
NSTR	26			2		
VARY	26	65	1.0	SPLIT RATIO - GPOLY1 CALC		
ID**	27			H2O SUPPLY TANK FOR STEAM GENERATOR	28	2
KBAS	27	30	3	0 1		
NSTR	27	1101		COMPUTE OUTLET FLOW IN GPOLY1		
VARY	27	1	2.55	INITIAL H2O FLOW (LB/HR)		
VARY	27	68	168.3	H2O TANK MAX CAPACITY (LB)		
VARY	27	69	168.3	H2O TANK INITIAL FILL (LB)		
VARY	27	70	70.0	H2O TEMPERATURE (F)		
VARY	27	71		TANK VOLUME (FT3)		
VARY	27	72	30.0	TANK PRESSURE (PSIA)		
VARY	27	98		WATER USED FROM TANK (LB)		
VARY	27	99		WATER ADDED TO TANK (LB)		
VARY	27	100	2.55	H2O FLOW (PPH)		
ID**	28			H2O SUPPLY PUMP FOR STEAM GENERATOR	29	2
KBAS	28	22		27 0 1		
NSTR	28	0002		INPUT PUMP HEAT ADDITION		
VARY	28	79	1.0	PUMP ON/OFF FLAG (1.0=ON)		
VARY	28	85	10.0	HEAT ADDITION (WATTS)		
ID**	29			STEAM GENERATOR FOR SAWD BED DESORPTION	25	2
KBAS	29	27		28 2		
NSTR	29	1		CALC ELEC ENERGY REQUIRED		
VARY	29	66	40.0	DESIRED DEGREES OF SUPERHEAT (F)		
VARY	29	67		TEMP OF SATURATED STEAM (F)		
VARY	29	68		ELEC ENERGY REQUIRED (WATTS)		
ID**	30			SPLIT - DESORBED GAS TO CABIN OR CO2 ACCUMULATOR.	32	2
KBAS	30	10		24 2		
NSTR	30			2		
VARY	30	65	1.0	SPLIT RATIO - GPOLY1 CALC		
ID**	31			GASMIX - CABIN AIR AND SAWD AIR TO HUMD CONTROL HX	7	2
KBAS	31	6		3 2		
NSTR	31			-19 2		
ID**	32			CO2 ACCUMULATOR TANK	31	2
KBAS	32	30	1	30 2		
NSTR	32	01000				
KARY	32	16		CO2 DELIVERY; 0 = OVBD; 1 = CO2 REDUCTION.		
VARY	32	70	70.	CO2 TEMPERATURE (F)		
VARY	32	71	2.0	TANK VOLUME (FT3)		
VARY	32	72	30.0	CO2 PRESSURE (PSIA)		
VARY	32	80	0.4644	MASS OF CO2 IN TANK (LB)		
TABL	1	1	2	16 0 LIN LIN		
TITL	1	2		CREWMAN METABOLIC RATE (BTU/HR) VS MISSION TIME (SEC)		

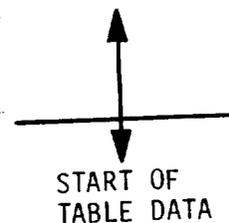
 END OF
 K AND V
 COMPONENT
 DATA




Table 8 (Continued)
Input to ESCM

VALU	1	10	2I	.0	2700.	3600.	7200.	.1800E+05	.1980E+05		
VALU	1	11	2D	450.0	450.0	520.0	650.0	650.0	450.0		
VALU	1	12	2I	.2340E+05	.2520E+05	.3960E+05	.4140E+05	.4320E+05	.4680E+05		
VALU	1	13	2D	450.0	650.0	650.0	520.0	450.0	450.0		
VALU	1	14	2I	.5040E+05	.5400E+05	.5580E+05	.8640E+05				
VALU	1	15	2D	390.0	520.0	300.0	300.0				
TABL	10	1	2		3		LIN	STP			
TITL	10	2	PRESSURE CONTROL SYSTEM OPERATION								
TITL	10	3	PRESSURE MODE VS MISSION TIME (SEC)								
TITL	10	4	=0	14.5 PSI CONTROLLER USED							
TITL	10	5	=1	8.0 PSI CONTROLLER USED							
VALU	10	10	2I	-8400.	15300.	427864.					
VALU	10	11	2D	0.0	0.0	0.0					
TABL	20	1	2		6		LIN	LIN			
TITL	20	2	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE								
TITL	20	3	O2 OPENING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)								
TITL	20	4	O2 OPENING FLOWS VS TOTAL PRESSURE (PSIA)								
VALU	20	10	2I	0.0	14.510	14.565	14.666	14.700	100.0		
VALU	20	11	2D	10.0	10.0	0.85	0.2	0.0	0.0		
TABL	21	1	2		6		LIN	LIN			
TITL	21	2	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE								
TITL	21	3	O2 CLOSING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)								
TITL	21	3	O2 CLOSING FLOWS VS TOTAL PRESSURE (PSIA)								
VALU	21	10	2I	0.0	14.605	14.672	14.745	14.819	100.0		
VALU	21	11	2D	10.0	10.0	0.6	0.25	0.0	0.0		
TABL	22	1	2		8		LIN	LIN			
TITL	22	2	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE								
TITL	22	3	N2 OPENING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)								
TITL	22	4	N2 OPENING FLOWS VS TOTAL PRESSURE (PSIA)								
VALU	22	10	2I	0.0	14.500	14.510	14.563	14.583	14.640		
VALU	22	11	2D	67.0	67.0	25.0	7.0	1.0	0.5		
VALU	22	12	2I	14.748	100.0						
VALU	22	13	2D	0.0	0.0						
TABL	23	1	2		8		LIN	LIN			
TITL	23	2	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE								
TITL	23	3	N2 CLOSING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)								
TITL	23	3	N2 CLOSING FLOWS VS TOTAL PRESSURE (PSIA)								
VALU	23	10	2I	0.0	14.590	14.625	14.658	14.680	14.748		
VALU	23	11	2D	67.0	67.0	11.0	7.0	0.8	0.5		
VALU	23	12	2I	14.813	100.0						
VALU	23	13	2D	0.0	0.0						
TABL	30	1	2		12	0	LIN	LIN			
TITL	30	2	RELATIVE HUMIDITY (DECIMAL) VS ABSORPTION CYCLE DURATION (MIN)								
TITL	30	3	FAN CHARACTERISTIC ADJUSTED - HSD REPORT SVHSER 8921								
VALU	30	10	2I	.15	.25	.35	.45	.50	.55		
VALU	30	11	2D	13.00	28.14	41.00	51.57	56.00	59.85		
VALU	30	12	2I	.60	.70	.80	.85	.95	1.00		
VALU	30	13	2D	63.14	68.00	70.57	70.99	71.01	71.01		
TABL	31	1	2		7	0	LIN	LIN			
TITL	31	2	SAWD FAN FLOW (CFM) VS ELAPSED TIME (SEC) DURING PREHEAT								
TITL	31	3	ESTIMATED VALUES 1-9-85								
VALU	31	10	2I	.0	60.	120.	180.	240.	300.		
VALU	31	11	2D	1.90	1.90	3.50	4.90	5.90	6.70		
VALU	31	12	2I	360.							
VALU	31	13	2D	7.10							
TABL	32	1	2		10	0	LIN	LIN			
TITL	32	2	SAWD FAN FLOW (CFM) VS. ELAPSED ABSORPTION CYCLE TIME (SEC)								
VALU	32	10	2I	.0	60.	120.	240.	360.	480.		
VALU	32	11	2D	0.10	5.00	7.90	11.00	12.80	13.95		
VALU	32	12	2I	600.	720.	900.	7200.				

CONTINUATION
OF TABLE DATA

Table 8 (Continued)
 Input to ESCM

VALU	32	13	2D	14.60	15.00	15.00	15.00		
TABL	33	1	2		10	0	LIN	LIN	
TITL	33	2	ABSORPTION CYCLE TIME (SEC) VS. SAWD FAN FLOW (CFM)						
VALU	33	10	2I	0.10	5.00	7.90	11.00	12.80	13.95
VALU	33	11	2D	.0	60.	120.	240.	360.	480.
VALU	33	12	2I	14.60	15.0	15.0	15.0		
VALU	33	13	2D	600.	720.	900.	7200.		
TABL	41	1	2		16	0	LOG	LIN	
TITL	41	2	MOLE FRACTION OF CO2 IN BED SEGMENT VERSUS LOADING.						
VALU	41	10	2I	0.0	0.01	0.02	0.03	0.04	0.05
VALU	41	11	2D	.0000001	0.000052	0.00048	0.0019	0.0050	0.0105
VALU	41	12	2I	0.06	0.07	0.075	0.0800	0.0825	0.085
VALU	41	13	2D	0.0225	0.044	0.068	0.1100	0.1500	0.250
VALU	41	14	2I	0.0885	0.090	0.094	1.0		
VALU	41	15	2D	0.5100	0.630	1.000	1.0		
TABL	51	1	2		12	0	LIN	LIN	
TITL	51	2	TEMPERATURE FACTOR ON CALCULATION OF EQUIL YCO2.						
VALU	51	10	2I	55.	77.	90.	110.	130.	150.
VALU	51	11	2D	1.20	1.00	0.870	0.790	0.570	0.4400
VALU	51	12	2I	170.	190.	210.0	250.	270.	400.
VALU	51	13	2D	0.2750	0.1550	0.060	0.0300	0.0150	0.0001
TABL	61	1	2		12	0	LIN	LIN	
TITL	61	2	WATER LOADING FACTOR ON CALCULATION OF EQUIL YCO2.						
VALU	61	10	2I	0.0	0.09	0.105	0.125	0.157	0.175
VALU	61	11	2D	0.551	0.550	0.571	0.745	1.034	1.200
VALU	61	12	2I	0.200	0.225	0.250	0.275	0.300	1.000
VALU	61	13	2D	1.360	1.410	1.429	1.440	1.450	1.450
TABL	71	1	2		13	0	LIN	LIN	
TITL	71	2	INFLUENCE OF RELATIVE HUMIDITY ON EQUILIBRIUM WATER LOADING						
VALU	71	10	2I	-10.00	0.000	0.010	0.035	0.060	0.083
VALU	71	11	2D	0.00	0.000	0.100	0.200	0.300	0.400
VALU	71	12	2I	0.104	0.145	0.190	0.230	0.275	0.315
VALU	71	13	2D	0.500	0.600	0.700	0.800	0.900	1.000
VALU	71	14	2I	1.000					0.315
VALU	71	15	2D	1.000					1.000
PLOT0									
PLOT1		2	181						
PLOT1		2	182						
PLOT2		1	66						
PLOT2		1	67						
PLOT2		1	68						
PLOT2		1	69						
PLOT2		1	82						
PLOT2		2	89						
PLOT2		2	94						
PLOT2		2	95						
PLOT2		2	98						
PLOT2		2	100						
PLOT2		2	104						
PLOT2		2	106						
PLOT2		2	165						
PLOT2		2	166						
PLOT2		15	6						
PLOT2		16	6						
PLOT2		15	12						
PLOT2		16	12						
PLOT2		16	2						
PLOT2		16	82						
PLOT2		16	83						
PLOT2		20	6						

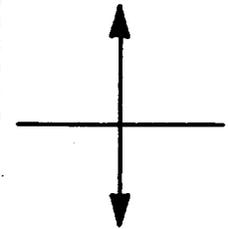
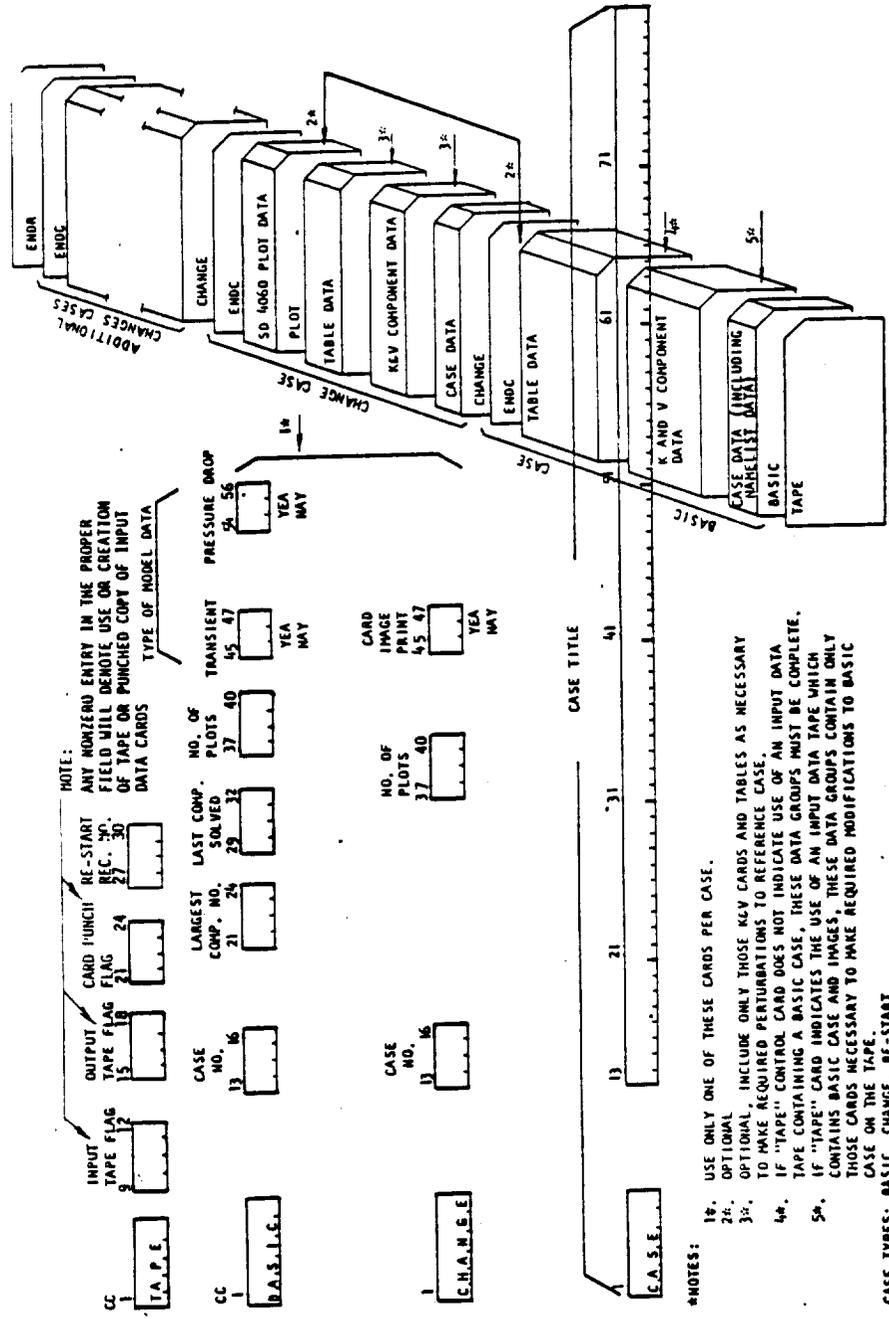
 END OF
 TABLE DATA

 START OF
 PLOT DATA

Table 8 (Continued)
Input to ESCM

PLOT2	21	6	SA-2 H2O OUT (LB/HR)
PLOT2	20	12	SA-2 CO2 IN (LB/HR)
PLOT2	21	12	SA-2 CO2 OUT (LB/HR)
PLOT2	21	2	SA-2 EXIT TEMP (F)
PLOT2	21	82	SA-2 H2O LOAD(LB/LB)
PLOT2	21	83	SA-2 CO2 LOAD(LB/LB)
ENDC			
ENDR			

END OF
PLOT DATA





***NOTES:**

- 1^a. USE ONLY ONE OF THESE CARDS PER CASE.
- 2^a. OPTIONAL.
- 3^a. OPTIONAL, INCLUDE ONLY THOSE KEY CARDS AND TABLES AS NECESSARY TO MAKE REQUIRED PERTURBATIONS TO REFERENCE CASE.
- 4^a. IF "TAPE" CONTROL CARD DOES NOT INDICATE USE OF AN INPUT DATA TAPE CONTAINING A BASIC CASE, THESE DATA GROUPS MUST BE COMPLETE.
- 5^a. IF "TAPE" CARD INDICATES THE USE OF AN INPUT DATA TAPE WHICH CONTAINS BASIC CASE AND IMAGES, THESE DATA GROUPS CONTAIN ONLY THOSE CARDS NECESSARY TO MAKE REQUIRED MODIFICATIONS TO BASIC CASE ON THE TAPE.

CASE TYPES: BASIC, CHANGE, RE-START

Figure 8
 Input Setup And Case Data Loadsheet

4.1.2.1 Case Data Group (Continued)

<u>Record 1</u>	<u>FORMAT</u>	<u>COLS</u>
2) Print selection for Shuttle model using G189A. Not used by ESCM. Input a zero in column 8.	I4	5-8

IPRT=0=print phase instantaneous and average data

IPRT=1=print only instantaneous data

IPRT=2=delete all diagram printouts, do not print average data.

See Figure 8 for the setup of the TAPE, BASIC, and CASE lines of input.

In the case group data, the user need only change the maximum value of time in seconds, TIMEMX, for a transient case. The time increment DTIME should not be changed; the value of 15 seconds has been selected to give the fastest running time while still giving the desired computational accuracy.

In the PROPI NAMELIST, the special fluids array are:

- 1) liquid water at 70°F and 1 atmosphere
- 2) carbon dioxide gas at 70°F and 3 mmHg

The diluent is nitrogen and the condensable is water vapor.

4.1.2.2 K and V Component Data Group

The K and V component data group consists of all the data required to specify and describe each component. These data include the connection and option data entered in integer format and the numerical values entered in floating point format. The former are referred to as K array values while the latter are referred to as V array values.

Five different types of input are required for each component. These input are contained in the ID record, the KBAS record, the NSTR record, the KARY records, and the VARY records. The ID record specifies the component number given by the user and describes what the component is. For example in Figure 4, the ID # of the crew is 1. See Figure 9 for the ID** load sheet which gives the format for the entries required.

CC	CORP. NO.		SEQ. NO.		COMPONENTS DESCRIPTION
	5	8	9	12	
1					14
					21
					31
					41
					51
					61
					71
					80

Figure 9
 ID** Loadsheets

4.1.2.2 K and V Component Data Group (Continued)

The second record is the KBAS record. This input provides the basic input to describe how the components are connected together via fluid flow paths and also provides the solution sequence (i.e., the order in which each component is solved). The format for input to the KBAS record is shown in Figure 10. The input in Table 8 for the KBAS records are for the model shown in Figure 4 and are formatted per Figure 10.

The third record in the K and V component group data is the NSTR record. In this record are input the component specific instructions or options selected that are required by the component subroutine. See Figure 11 for the format. A description of the options are provided in Reference 3 for each subroutine. Also, NSTR(16) through NSTR(18) have general meanings applicable to all subroutines. These general meanings can be found in Chapter 6 of Reference 3.

The fourth and fifth records to be provided are the KARY and VARY records. These input provide the initial values and constants for integer and floating point variables required for each component. The format for inputting these values is given in Figures 12 and 13 respectively for the KARY and VARY records.

All the input for the K and V component group data are constants and should not be changed by the user. The only input that may be changed without affecting the ESCM model and correlation are the following:

<u>Item</u>	<u>Location</u>
1) Number of crewmen	K(1,16)
2) Sensible heat per crewman	V(1,66)
3) Latent heat per crewman	V(1,67)
4) Cabin heat load	V(2,66)
5) Cabin free volume	V(2,139)
6) Printoff frequency	V(2,184)
7) Cabin gas design temperature	V(2,87)
8) Time to begin debug printoff	V(16,95)/V(21,95)
9) CO ₂ delivery:	K(32,16)
0=O ₂ bed	
1=CO ₂ reduction	

Other parameters may of course be changed, but only by a user who understands the ESCM program and the implications of the change.



As a convenience, the Special Flow Type No. 1 entry is also used to define the total flow stream property data for flow codes - 0 or 1 as described below:

PRIMARY SIDE DATA

COMP. NO.	5	B
CC	K.B.A.S	
SUBR. NO.	13	15
EXTRA LOC.	V	K
SOURCE COMP. NO.	28	30
FLOW CODE	33	35
SPECIAL FLOW TYPES	37	39
COMP. NO.	41	43
CR	KR ₁	KR ₂

SECONDARY SIDE DATA

COMP. NO.	47	51
SOURCE COMP. NO.	55	57
FLOW CODE	58	59
SPECIAL FLOW TYPES	60	62
COMP. NO.	64	66
CR	KR ₃	KR ₄

COMP. NO.	70
NEXT COMP.	71
CR	KR ₅

COMP. NO.	75
ASSOC. CABIN	78
CR	KR ₆

COMP. NO.	75
ASSOC. CABIN	78
CR	KR ₇

* If Flow Code = 0: The Special Flow Type No. 1 entry defines the property data for the total liquid flow. If Flow Code = 1: The Special Flow Type No. 1 entry defines the property data for the non-condensables flow.

Figure 10 KBAS Loadsheets

CC	COMP. NO.	5	B	N.S.T.R.	
NSTR		19	21		
NSTR		24	32		
COMMENTS		35	41		
COMMENTS		51	61		
COMMENTS		71	80		

Figure 11
 NSTR Loadsheat

COMP. NO.	START	VALUE	END	DESCRIPTION
CC	1			
5				
8				
	10 12			
	14			
	17			
	25 27			
	31			
	41			
	51			
	61			
	71			
	80			

REFERENCE LOCATION

 Figure 12
 KARY Loadsheet



CORP. NO.		START	VALUE	END	DESCRIPTION
CC					
1	V.A.R.V.	10	14	25	41
5		12	23	27	
6					51
					61
					71
					80

Figure 13
VARY Loadsheat

4.1.2.3 Table Data Group

The table data group contains all the tables or curves required for the ESCM program. These tables relate such variables as metabolic load as a function of time. These table data are not to be altered by the user except for crewman metabolic rate (Btu/hr) vs mission time (sec).

Of course other table data may be changed by the user but should only be done so by a user who understands the program and the implications of the change. The format to input table data is shown in Figure 14.

4.1.2.4 Plot Data Group

The plot data group of input specifies those variables which are to be saved for later use by a plotting program. The variables listed in Table 8 serve as a baseline group from which some can be deleted or others added as desired by the user. The format for each variable to be entered is shown in Figure 15.

4.2 Installation of HS ESCM Program at Langley Research Center

4.2.1 Introduction

The Hamilton Standard (HS) version of the ESCM program is executed at HS on IBM 3080 computers, and several modifications are needed to make it compatible with the Langley Research Center (LaRC) Prime 850 computer. These modifications involve substituting equivalent prime system functions (for example, date and central processor time) for the IBM calls and updating the program to the local FORTRAN 77. The procedure for making these changes to the program as delivered by HS is outlined below. All programs and procedure files are found in the directory SEB>LFR.DIR>EMSIM.DIR.

4.2.2 Program Delivery

HS will provide a nine-track magnetic tape with the program source code and input data at least. In addition, listings of the code and results of a sample simulation run will be needed to verify the correctness of program execution. This tape, with sufficient description of its block size, density, code (probably EBCDIC), word length, and number of files should be taken to the PRIME analyst who will dump the tape to a user directory.

UNI-VARIANT DATA

DATA TYPE	1	2	3	4	5	6
21	X ₁	X ₂	X ₃	X ₄	X ₅	X ₆
2D	Z ₁	Z ₂	Z ₃	Z ₄	Z ₅	Z ₆
21	X ₇	X ₈				
2D	Z ₇	Z ₈				

CC 1 5 8 9 11

T.A.B.L.E. TABLE SEQ. NO. DIMENSIONALITY (ENTER [2 UNIV.] OR 3 [BIVAR.])

BIVARIANT DATA

DATA TYPE	1	2	3	4	5	6
31	X ₁	Y ₁	Y ₂	Y ₃	Y ₄	Y ₅
3D	X ₁	Z ₁₁	Z ₁₂	Z ₁₃	Z ₁₄	Z ₁₅
3D	X ₂	Z ₂₁	Z ₂₂	Z ₂₃	Z ₂₄	Z ₂₅
3D	X ₃	Z ₃₁	Z ₃₂	Z ₃₃	Z ₃₄	Z ₃₅
31		Y ₆	Y ₇			
3D	X ₁	Z ₁₆	Z ₁₇			
3D	X ₂	Z ₂₆	Z ₂₇			
3D	X ₃	Z ₃₆	Z ₃₇			

NOTE: ENTER DATA IN ASCENDING ORDER OF VALUES FOR THE INDEPENDENT VARIABLES, I.E., $K_{i+1} > K_i, Y_{i+1} > Y_i$

1. STEP FUNCTION DATA (2 DIM TABLE ONLY) ENTER "STP" FOR 1ST IND VAR AND "LIN" FOR DEP VAR

NO. OF POINTS SCALE TYPE (ENTER "LIN." OR "LOG") TITLE

26 X 1st IND. VAR 41 Z DEP VAR 55 Y 2nd IND. VAR

33 Y 1st IND. VAR 47 X 1st IND. VAR 51 X 2nd IND. VAR

36 Y 2nd IND. VAR 49 Z DEP VAR 61 Y 2nd IND. VAR

13 33 41 51 61 80

DATA TYPE 13 14 16 21 25 27 38 36 49 58 60 69 80

TABLE SEQ. NO. 5 8 9 11

V.A.L.U.E.

Figure 14
CURVE OR TABLE DATA Loadsheet

N V C	N C C	COMP NO.	REF. LOC.	MIN (X/Y)	MAX (X/Y)	DEP. VAR. LABEL	TITLE (ABSCISSA/ORDINATE)																																																																														
							1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20																																																											
				19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100

Figure 15
PLOT Data Loadsheet

4.2.3 Modification and Checkout

The five subprogram calls that must be satisfied in the ESCM program are: DATEJC, JOBTIM, CORE, RTIME, and ERASE. These subprograms are not delivered with the program in any form since they are IBM-system dependent. ERASE (called from ARSS) clears the interactive screen before data is to be displayed. This equivalent function has been provided by ERASE.F77 and assumes that the terminal is a Tektronix terminal. The library VLBTEK.L must also be loaded to satisfy entry points required by the LaRC subroutine. DATEJC (called from ECLST) provides the date on the format MM/DD/YY. The equivalent function has been provided by DATEJC.F77. These two subroutines should be added to the delivered source code for the ESCM program which is in the file ESCM.F77.

The three remaining functions are called from subroutines as follows: JOBTIM from ELAPSE, CORE from ENKODE (which has an entry DEKODE), and RTIME from PRTIME. In these cases the calling subroutines themselves (which are included in the delivered source code) are to be replaced by source code of the same name, i.e., ELAPSE.F77, ENKODE.F77, and PRTIME.77. These subroutines require that the prime library VAPPLB be loaded.

The procedure file needed to compile this modified source code is called ESCM.CMPL.CPL and is listed below. To execute it, simply do R ESCM.CMPL.

```
/* REPLACE SUBROUTINES ELAPSE, PRTIME, AND  
/* ENKODE WITH THE LRC VERSIONS  
/* ADD SUBROUTINES DATEJC AND ERASE
```

```
F77 ESCM.F77 - 64V - SILENT - DEBUG -XREF - LOUT
```

This will produce a compilation listing on file OUT with variable cross references. FORTRAN errors, if any are encountered, will appear in the listing except for warning (level 1) messages (which can be numerous). When all FORTRAN errors have been corrected, this procedure will produce a binary file ESCM.BIN which can be loaded by procedure ESCM.LOAD.CPL listed below. To execute it, simply do R ESCM.LOAD.

```
/* THIS LOADS THE ESCM BINARY AND LIBRARIES  
SEG -LOAD  
LO ESCM.BIN  
LI VAPPLB  
LI VLBTEK  
LI  
MAP LM Ø  
SA  
Q
```

4.2.3 Modification and Checkout (Continued)

This will produce a full load map on file LM which can be reviewed for unsatisfied entry points. If the load is complete, this will produce an absolute run file called ESCM.SEG. The program can be executed simply by SEG.ESCM. If errors are found, the same file can be run using the prime debugger by DBG.ESCM. Once all errors are corrected and an appropriate check case is verified, the -DEBUG option should be removed from the F77 command line in procedure ESCM.CMPL.CPL and both procedures re-executed to provide a more efficient run file.

4.2.4 File Usage

The ESCM program requires about a dozen files, several of which are site dependent and will not be used (on purpose) at LaRC. A summary table of the files is given below. These are defined by OPEN statements in program MAIN. File numbers are usually identified by integer variables which are usually set by DATA statements. Values for the LaRC prime version of ESCM are reflected in Table 9.

4.3 ESCM Output

Three forms of output are available with the ESCM program - output to the screen, hardcopy output, and plots.

Output to the screen is automatic and will occur at the printoff frequency specified by location V(2,184). For example, if the printoff frequency specified is 8.0 time steps per printoff, then a printoff will be made every 120 seconds when the recommended time step of 15 seconds is used. Values are printed in tabular form on the screen as a function of time. The values printed to the screen are:

- 1) Time of operation, minutes
- 2) Cabin temperature, °F
- 3) Cabin dew point temperature, °F
- 4) Cabin relative humidity, %
- 5) Cabin CO₂ partial pressure, mmHg
- 6) SAWD bed #1 CO₂ loading, % of dry amine wgt
- 8) SAWD bed #1 exit temperature, °F
- 9) SAWD bed #2 CO₂ loading, % of dry amine wgt
- 10) SAWD bed #2 H₂O loading, % of dry amine wgt
- 11) SAWD bed #2 exit temperature, °F

Table 9
ESCM I/O File Assignments For PRIME Computer

<u>Integer Variable</u>	<u>File # Assigned</u>	<u>Where Assigned</u>	<u>Status</u>	<u>Comments</u>
NDA	41	BLOCK DATA	Scratch	Restart file for multiple cases (Also referred to as NOUT in MERGEC)
NDB	42	BLOCK DATA	Scratch	
NDC	43	BLOCK DATA	Scratch	
NDD	44	BLOCK DATA	Scratch	
NDE	45	BLOCK DATA	Saved	
NTIN	10	BLOCK DATA		Read basic case or restart data
NTOUT	11	BLOCK DATA		
NSTUFF	31	BLOCK DATA	Scratch	Card punch file
NOUT	=NDB	MERGEC	Scratch	(Used only in MERGEC)
NIN	=NDC or NDD	MERGEC	Scratch	(used only in MERGEC)
---	5			All input data
---	6		Saved	All output data & schematics
NTERM	1	ARSS		Special output to interactive terminal
---	15	ENKODE	Non-existent	Used for ENCODE/DECODE area
NTAPE	1234	STOPIT	Non-existent	Used by STOPIT to produce error
	30			Used by IEDIT for ?
NDISK				Used in KVREAD
N		Equivalent to NDISK		Used in TABLRD

4.3 ESCM Output (Continued)

The hardcopy output is shown in Appendix B. It includes:

- 1) A mirror image of the input.
- 2) A more readable version of the entire input.
- 3) Schematic printouts of the requested printoff frequency. See Figure 6 or Appendix B.
- 4) Final values in the K and V arrays for all components at the end of the case.
- 5) A list of variables whose time varying data have been saved for use by a plotting program.

Plot output must be generated through the use of another program. At Hamilton Standard, plots are generated using the MERIAM program which will in turn generate a tape for use on the CALCOMP plotter. To generate plots, follow the following steps:

- 1) LG EPLLOT CNTL S0(G15UARL) RON
- 2) LGEF GPLOT DATA G15UARL

Make changes to NAMELIST CASE as required. The definition of the variables in CASE and their type are given in Table 10. Note that ILRCD, NPPTS, TSTART, TEND and NCASE are printed out at the end of the ESCM run. Also make changes to the independent and dependent variable input which defines the plots to be made. Note that if no independent variable card is input, the default independent variable is mission time in hours. See Tables 11 and 12 for the setup for the independent and dependent variable input respectively. A sample setup is shown in Appendix B under GPLOT.DATA.

- 3) SUB EPLLOT

Execution of these steps will generate plots. A sample set of plots is shown in Appendix D.

4.4 Error Messages

Listing of error messages can be found in Reference 3 for G189A supplied subroutines. Subroutines written specific for ESCM are GPOLY1, GPOLY2, IR45, and ARSS. Of these subroutines, only IR45 has error messages. A listing of these error messages follows:

Table 10
 NAMELIST CASE Variables To Make Plots

<u>FORTRAN Format</u>	<u>FORTRAN Name</u>	<u>Definition</u>
I	NCASE	G189 case number (Output by G189).
I	ILRCD	Length of plot tape records (Output by G189).
I	NPPTS	Number of tape time points written for the G189 case. (Output by G189).
E	TSTART	Plot start time (Seconds).
E	TEND	Plot end time (Seconds).
I	IPFREQ	Plot frequency flag. (Default value=1)
I	NUMCAS	Number of G189 tape cases flag. If more than one G189 case is on the input plot tape, set NUMCAS=1. If only one G189 case is on the plot tape, NUMCAS=0. (Refer to G189 Input Data Setup for further details.)
I	IFPLOT	Plot data table generation flag. Must be equal to 0 for the first plotting case. For succeeding plotting cases, set IFPLOT=1 if new plot data cards are not to be input.
I	IEND	End of run flag. IEND=0 If this is not the last plotting case to be executed. IEND=1 If this is the last plotting case to be executed.
I	IPLOT	Plot only option flag. IPLOT=0 Plot editing information will be input. IPLOT=1 Plot only. No plot editing information will be input. (IFPLOT,LOCREF,NVC)
I	IPRINT	Plot file print flag. IPRINT=0 No plot file time point history will be output. IPRINT=1 A plot file time point history (list of time points for which a plot data record has been written) will be output.

Table 11
Independent Variable Input To Make Plots

<u>Card Name</u>	<u>Card Column</u>	<u>FORTRAN Format</u>	<u>FORTRAN Name</u>	<u>Definitions</u>
PLOT	1-4 5	I1	NVC*	Variable type code. NVC=1 for the independent variable. If no independent variable card is input, the default independent variable is mission time (hours).
	13-16	I4	LOCREF*	Tape reference location for the independent variable. [Default independent variable is time (hrs), Tape Location 1.]
	19-28	E10.0	XMIN	Minimum value of the independent variable to be plotted (optional input).
	29-38	E10.0	XMAX	Maximum value of the independent variable to be plotted (optional input).
	39-80	7A6	XINTIT(7)	Abcissa title. This alphanumeric information will appear on the plot frame as the horizontal axis title.

* Do not input if IPLOT=1

Table 12
Dependent Variable Input To Make Plots

<u>Card Name</u>	<u>Card Column</u>	<u>FORTRAN Format</u>	<u>FORTRAN Name</u>	<u>Definitions</u>
PLOT	1-4 5	I1	NVC*	Variable type code. NVC=2 for the dependent variable(s).
	6	I1	NC**	Number of dependent variable curves to be plotted for a frame. Default value is 1 ($1 \leq NC \leq 6$).
	13-16	I4	LOCREF**	Tape reference location for the independent variable. A table of tape reference location vs. V-array location (component number, reference location) is printed by G189. (Do not input on this card if $NC > 1$. Refer to multivariable data cards.)
	19-28	E10.0	YMIN	Minimum value of the dependent variable(s) to be plotted (optional input).
	29-38	E10.0	YMAX	Maximum value of the dependent variable(s) to be plotted (optional input).
39-80	7A6	YTITLE(7)	Ordinate title. This alphanumeric information will appear on the plot as the vertical axis title.	

* Note: When using multivariable plots, the data value range of the dependent variables to be plotted on the frame should not differ significantly.

** Do not input if IPLOT=1

Multivariable plot Data Input

<u>Card Name</u>	<u>Card Column</u>	<u>FORTRAN Format</u>	<u>FORTRAN Name</u>	<u>Definitions</u>
PLOT	1-4 5	I1	NVC	Variable type code. NVC=2 for dependent variable.
	13-16	I4	LOCREF	Tape reference location for the i th dependent variable on a frame ($i \leq 6$).
	39-58	5A4	DVLAB(I)	Label for the i th dependent variable on a plot frame. The variable label and corresponding plot character information are printed at the bottom of the plot frame.

These cards are input only if $NC > 1$ and $IPLOT=0$. Do not input if $IPLOT=1$.

4.4 Error Messages (Continued)

<u>Subroutine</u>	<u>Message</u>
SUB2	Subroutine SUB2 called with a temperature below 55°F by component # ____ Temperature = ____°F Time = ____.
SUB2	Subroutine SUB2 called with a temperature above 300°F by component # ____ Temperature = ____°F Time = ____.

These two messages alert the user that the temperatures tried are outside the range of the correlation for the temperature effect on bed CO₂ loading.

<u>Subroutine</u>	<u>Message</u>
BALNCE	Subroutine IR45 called by component # ____, segment _____. Heat balance did not converge after ____ iterations. The time is ____ seconds. Sum of the energies = _____. Temperature = _____. Vapor mass = _____.

This message alerts the user that convergence could not be achieved after XX iterations when iterating on the temperature in a SAWD bed segment to balance the energy equation. This message may occur from time to time throughout a case and usually is of no consequence. Typically, the temperature error by not reaching convergence is less than 0.5°F.

Lastly, although not an error, the user may request debug printoff to begin occurring at any desired time by specifying this time in location 95 in either SAWD bed input. The information printed is as follows:

Time	= Transient time, seconds
K	= Segment number
ICOUNT	= Iteration number
TBED	= Bed temperature, °F
TEMP	= Gas temperature, °F
TDEW	= Dew point temperature, °F
XLOAD	= equivalent CO ₂ loading, fraction of dry amine weight in time step DTIME, lbm
INERTS	= Total inerts less CO ₂ entering segment in time step DTIME, lb-moles
INERT	= Total inerts less CO ₂ initially in segment void, lb-moles
PTOT	= Total pressure of gas in segment, psia
PIF	= Total pressure of gas in segment that would exist if all gas entering segment were allowed to stay, psia
PH2O	= Equilibrium partial pressure of water, psia

4.4 Error Messages (Continued)

PCO2	= Equilibrium partial pressure of CO ₂ , psia
AE(I)	= Mass of gases exiting segment in time step DTIME, lbm
R2(I)	= Mass of gases resident in void volume at end of time step, lbm
B2(I)	= Mass of CO ₂ in resin, H ₂ O in resin, and dry resin at end of time step, lbm
RATE	= CO ₂ absorption/desorption rate, lb of CO ₂ per lb of dry amine per psi difference between actual and equilibrium CO ₂ pressure.
PCO21	= Initial partial pressure of CO ₂ from subroutine SUB2, psia
MCR1	= Initial calculation of mass of CO ₂ absorbed using PCO21, lbm
MCR2	= Second calculation of mass of CO ₂ absorbed after being limited to the masses of CO ₂ actually present, lbm
MCO21	= Mass of CO ₂ in gas entering plus resident after subtraction of amount absorbed MCR2, lbm
MCO2	= Mass of CO ₂ in gas entering plus resident after absorption and after checks for pressure collapse and minimum CO ₂ available to satisfy PCO ₂ , lbm
MH201	= Mass of H ₂ O in gas entering plus resident after evaporation or condensation but before pressure collapse check, lbm
MH202	= Mass of H ₂ O in gas entering plus resident after evaporation or condensation and after pressure collapse check, lbm
BURP	= Flag to indicate if bed temperature is at saturation temperature. T = true, F = false
PH20IN	= Partial pressure of water vapor entering segment, psia
WTMAIN	= Molecular weight of gas mixture entering segment, lb/lb-mole
PCO2IN	= Partial pressure of CO ₂ in gas entering segment, psia
PUSTRM	= Pressure upstream of segment, psia
PDSTRM	= Pressure downstream of segment, psia
QSUM	= Sum of all energies. When balanced QSUM = 0.0, Btu
HBEGIN	= Sum of energies in existing gas, entering gas, the bed, and tank at the beginning of the time step, Btu
HEND	= Sum of energies in existing gas, exiting gas, the bed, and tank at the end of the time step, Btu
HC02	= Energy change due to absorption or desorption of CO ₂ , Btu
HH20	= Energy change due to evaporation or condensation of water, Btu
HSTOR	= Energy change due to the change in stored energy within the segment, Btu

4.4 Error Messages (Continued)

MFG	= Mass of steam condensed if positive, otherwise mass of steam evaporated.
MCR	= Mass of CO ₂ absorbed if positive, otherwise mass of CO ₂ desorbed.
AI(I)	= Mass of gases entering segment in time step DTIME, lbm I=1=total I=2=total non-condensable I=3=water vapor I=4=oxygen I=5=nitrogen
R1(I)	= Mass of gases resident in void volume at start, lbm
B1(I)	= Initial masses of (1) CO ₂ in resin (2) H ₂ O in resin (3) dry resin, lbm
AIN(1)	= Total mass of gas entering segment in time DTIME, lbm
AIN(5)	= Total non-condensables entering segment in time DTIME, lbm
AIN(6)	= Water vapor entering segment in time, DTIME, lbm
AIN(9)	= Molecular weight of non-condensable gases entering segment, lbm/lb-mole
AIN(12)	= Carbon dioxide gas entering segment in time DTIME, lbm

This information is printed for each segment of the specified SAWD bed and each iteration in every time step following the user specified time.

5.0 FORTRAN NAME - ANALYSIS SYMBOL CROSS REFERENCE

Table 13 is a cross reference list between the FORTRAN variable names used in the ESCM User's Manual and the analysis symbols used in the ESCM Model Description Document in Reference 4. Only those FORTRAN names that have a corresponding symbol in the Model Description Document are listed. In some instances, the general symbol is presented for a specific FORTRAN name because that same symbol is used throughout the Model Description Document (i.e., m_e = exiting mass flow, lbm/hr).

6.0 REFERENCES

- (1) Blakely, Robert L. and Rowell, Lawrence F.; "Environmental Control and Life Support System Analysis Tools for the Space Station Era"; SAE Technical Paper Series 840956; Fourteenth Intersociety Conference on Environmental Systems, San Diego, California; July 16-19, 1984.
- (2) Blakely, Robert "Contract NAS 1-17397, Development of an Emulation/Simulation Computer Model of a Space Station Environmental Control and Life Support System (ECLSS) Task 1 and Task 2 Results", ESCM-EM-02, December 12, 1983.

Table 13
 FORTRAN Name - Analysis Symbol Cross Reference List

<u>FORTRAN Name</u>	<u>Analysis Symbol</u>	<u>Description</u>
CFM	cfm	Flow through fan, cfm
DTIME	Δt	Time step increment, seconds
KK(1,16)	N	Number of people in crew
R(1)	m_T	Total flow exiting a component, lbm/hr
R(2)	T	Temperature of fluid exiting a component, °F
R(3)	P_i	Pressure at component inlet, psia
R(4)	P_e	Pressure at component exit, psia
R(5)	$m_{nc} + m_{CO2}$	Total non-condensable flow, lbm/hr
R(6)	m_v	Vapor flow, lbm/hr
R(7)	m_l	Entrained liquid flow, lbm/hr
R(8)	c_p	Specific heat of non-condensables, Btu/lbm-°F
R(9)	M_w	Molecular weight of non-condensables, lb/lb-mole
R(10)	m_{O2}	Flow of oxygen, lbm/hr
R(11)	m_{N2}	Flow of nitrogen, lbm/hr
R(12)	m_{CO2}	Flow of carbon dioxide, lbm/hr
RHAVG	RH	Average relative humidity (decimal form) in cabin during absorption cycle
VV(1,66)	QSxN	Crew total sensible heat generated, Btu/hr
VV(1,67)	QLxN	Crew total latent heat generated, Btu/hr
VV(1,68)	WO2	Crew oxygen usage rate, lbm/hr
VV(1,69)	WCO2	Crew carbon dioxide generation rate, lbm/hr
VV(1,70)	WH2O	Crew water vapor generation rate, lbm/hr
VV(1,82)	QT	Crew total metabolic rate, Btu/hr
VV(2,4)	P_T	Cabin total pressure, psia
VV(2,87)	T_{set}	Main cabin gas design or setpoint temperature, °F
VV(2,94)	P_{O2}	Cabin partial pressure of oxygen, psia
VV(2,165)	m_{O2}	Flow of oxygen into cabin, lbm/hr
VV(2,166)	m_{N2}	Flow of nitrogen into cabin, lbm/hr

Table 13 (Continued)

FORTRAN Name - Analysis Symbol Cross Reference List

<u>FORTRAN Name</u>	<u>Analysis Symbol</u>	<u>Description</u>
VV(7,1)	m_a	Mass flow of air through humidity control heat exchanger, lbm/hr
VV(7,66)	UA	Calculated overall heat transfer coefficient of humidity control heat exchanger, Btu/hr-°F
VV(7,72)	$(C_p)_{eff}$	Effective specific heat of gas flow into humidity control heat exchanger, Btu/lbm-°F
VV(10,67)	m_l	Condensate removal rate in water separator, lbm/hr
VV(10,65)	Q	Power added to water separator, Btu/hr
VV(19,1)	$(m_T)_e$	Total gas flow exiting SAWD fan, lbm/hr
VV(32,71)	V_o	CO ₂ accumulator tank volume, ft ³
VV(x,65)	SR	Split ratio for splitter "x"

The following apply to either SAWD bed:

R(66)	C_r	Specific heat of dry resin bed, Btu/lbm-°F
R(67)	ρ_r	Density of dry resin bed, lbm/ft ³
R(74)	r_o	Basepoint absorption desorption rate (pph of CO ₂ /lb of dry resin/psi of CO ₂ partial pressure difference)
R(78)	M_r	Total dry resin weight, lbm
R(79)	M_t	Total thermal mass of tank or canister around SAWD resin, lbm
R(82)	L _{H2O}	Total bed water loading
R(83)	L _{CO2}	Total bed carbon dioxide loading
R(84)	c_t	Specific heat of canister, Btu/lbm-°F
R(87)	τ	Outlet temperature sensor time constant, sec
R(93)	M_f	Total foam in bed, lbm
R(94)	c_f	Specific heat of foam, Btu/lbm-°F

6.0 REFERENCES (Continued)

- (3) "G189A Generalied Environmental/Thermal Control and Life Support Systems Computer Program Manual"; McDonnell Douglas Corporation MDAC-G2444; September, 1971.
- (4) Yanosy, J. "Model Description Document for a Computer Program of the Emulation/Simulation of a Space Station Environmental Control and Life Support System (ESCM)"; Hamilton Standard Report SVHSER 9504 for National Aeronautics and Space Administration Langley Research Center; NASA CR-181737, September 1988.

Appendix A

Job Control Lists For IBM

- ESCMCL
- ESCMCN

ESCMCL
JOB CONTROL LIST

```
CONTROL PROMPT NOMSG
N1: DELETE PLOTL.DATA
    DELETE OUTX.DATA
FREE FILE(FT01F001)
FREE FILE(FT02F001)
FREE FILE(FT03F001)
FREE FILE(FT04F001)
FREE FILE(FT05F001)
FREE FILE(FT06F001)
FREE FILE(FT10F001)
FREE FILE(FT11F001)
FREE FILE(FT16F001)
FREE FILE(FT20F001)
FREE ATTRLIST(A1 B2 C3 D4)
ATTRIB A1 BLKSIZE(844) RECFM(V B) LRECL(844)
ATTRIB B2 BLKSIZE(5000) RECFM(V B S) LRECL(5000)
ATTRIB C3 BLKSIZE(8404) RECFM(V B S) LRECL(8404)
ATTRIB D4 BLKSIZE(3990) RECFM(F B A) LRECL(133)
DELETE DD1
DELETE DD2
DELETE DD3
DELETE DD4
DELETE DDA
DELETE DDB
ALLOC DS(DD1) F(FT01F001) NEW SPACE(844,200) BLOCK(844) +
    USING(A1) CATALOG
ALLOC DS(DD2) F(FT02F001) NEW SPACE(200,200) BLOCK(5000)+
    USING(B2) CATALOG
ALLOC DS(DD3) F(FT03F001) NEW SPACE(200,200) BLOCK(8404) +
    USING(C3) CATALOG
ALLOC DS(DD4) F(FT04F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C3) CATALOG
ALLOC DS(ESCM2C.DATA) F(FT05F001)
ALLOC DS(OUTX.DATA) F(FT06F001) NEW SPACE(200,200) BLOCK(3120) +
    USING(D4) CATALOG
ALLOC DS(DDA) F(FT10F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C3) CATALOG
ALLOC DS(DDB) F(FT11F001) NEW SPACE(200,200) BLOCK(8408) +
    USING(C3) CATALOG
ALLOC DS(PLOTL.DATA) F(FT16F001) NEW SPACE(200,200) BLOCK(8408) +
    UNIT(TSOWRKB) USING(C3) CATALOG
ALLOC DS(*) F(FT20F001)
CALL 'ENG.G15.LM(G189L2C)'
END
```

Appendix B

Files For Plotting

- EPLLOT
- GPLLOT



EPLLOT.CNTL

```
//TSOG15PD      JOB (X,8888,99,08,,,,01,,60,G189,15603,0100,E),
//              'J. YANOSY',NOTIFY-TSOG15P,
//              CLASS-E,MSGLEVEL=(1,1),MSGCLASS=8
//*
/*JOBPARM      LINES=15
/*ROUTE PRINT LOCAL
//GO EXEC PGM=GLOT,REGION=1024K
//STEPLIB DD DSN=ENG.G15.LM,DISP=SHR
//FT01F001 DD UNIT=SYSDA,DISP=(NEW,DELETE),SPACE=(8408,(200,200)),
//          DCB=(RECFM=VBS,LRECL=8404,BLKSIZE=8408)
//FT02F001 DD UNIT=SYSDA,DISP=(NEW,DELETE),SPACE=(8408,(200,200)),
//          DCB=(RECFM=VBS,LRECL=8404,BLKSIZE=8408)
//FT04F001 DD UNIT=SYSDA,DISP=(NEW,DELETE),SPACE=(8408,(200,200)),
//          DCB=(RECFM=VBS,LRECL=8404,BLKSIZE=8408)
/* SET UP TO RUN ESCM CHECKOUT MODEL DATA "ESM.DATA" NOW
//FT05F001 DD UNIT=TSOWRKB,DSN=TSOG15P.GLOT.DATA,DISP=(OLD,KEEP)
//FT06F001 DD SYSOUT=A
//FT08F001 DD DSN=TSOG15P.TRES.DATA,UNIT=TSOWRKB,DISP=(NEW,CATLG),
//          DCB=(RECFM=FB,LRECL=80,BLKSIZE=3120),
//          SPACE=(3120,(200,200),RLSE)
//FT09F001 DD DSN=TSOG15P.BRES.CNTL,UNIT=TSOWRKB,DISP=(NEW,CATLG),
//          DCB=(RECFM=FB,LRECL=80,BLKSIZE=3120),
//          SPACE=(3120,(200,200),RLSE)
//FT16F001 DD DSN=TSOG15P.PLOT.DATA,UNIT=TSOWRKB,DISP=(OLD,KEEP),
//          DCB=(RECFM=VBS,LRECL=8404,BLKSIZE=8408),
//          SPACE=(8408,(200,200),RLSE)
//*
//PETE3 EXEC MPRES,MACH=B
//MPRS.ICML5 DD DSN=TSOG15P.BRES.CNTL,DISP=(OLD,DELETE)
//MPRS.INDT9 DD DSN=TSOG15P.TRES.DATA,DISP=(OLD,DELETE)
//*
```

Appendix C

Sample Problem Input and Output

This appendix contains an abridged output from the following sample problem.
The principal input parameters are:

- (1) Number of men = 3
- (2) Cabin volume = 8,000 ft³
- (3) Cabin temperature = 70°F
- (4) Equipment heat load = 17065 Btu/hr
- (5) Cabin leakage = 0.08333 lbm/hr
- (6) A variable metabolic load representative of a work, eat, sleep schedule

The output is abridged by showing only a representative number of output schematic printouts for the transient portion of the analysis.

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VARY	2	29	303.76	OXYGEN FLOW (LB/HR)
VARY	2	30	1063.67	NITROGEN FLOW (LB/HR)
VARY	2	31	9.45	CO2 FLOW (LB/HR)
VARY	2	65	17065.	TOTAL HEAT ADDED TO CABIN GAS MIXTURE (BTU/HR)
VARY	2	71		CABIN HEAT LOSS DUE TO OUTBOARD LEAKAGE (BTU/HR)
VARY	2	72		HEAT LOSS DUE TO MASS ADDITIONS (BTU/HR)
VARY	2	73		HEAT LOSS DUE TO FLASH ENTRAINMENT (BTU/HR)
VARY	2	74		FLASH EVAPORATION RATE OF ENTRAINMENT (4 NEH)
VARY	2	66	70.0	CABIN GAS DESIGN TEMP (F) (4 NEH)
VARY	2	68	10.0	CABIN GAS RELATIVE HUMIDITY (DECIMAL)
VARY	2	69		DESIGN TOTAL PRESSURE (PSIA)
VARY	2	91	0.5	DESIGN TOTAL PRESSURE TOL (PSIA)
VARY	2	92	0.9	DESIGN OXYGEN PRESSURE (PSIA)
VARY	2	93	0.5	DESIGN OXYGEN PRESSURE TOL (PSIA)
VARY	2	94		CABIN GAS OXYGEN PRESSURE (PSIA)
VARY	2	95		CABIN GAS NITROGEN PRESSURE (PSIA)
VARY	2	86	50.0	DESIGN DEW POINT (F)
VARY	2	97	30.0	DESIGN DEW POINT TOL (F)
VARY	2	98		CABIN GAS DEW POINT (F)
VARY	2	99	20.	MAX ALLOWABLE CO2 PRESSURE (MM HG)
VARY	2	100		CABIN GAS CO2 PRESSURE (MM HG)
VARY	2	101	250.	MAX ALLOWABLE TRACE CONTAMINANT LEVEL (PPM)
VARY	2	102		CABIN GAS TRACE CONTAMINANT LEVEL (PPM)
VARY	2	103		CABIN GAS MIXTURE, TOTAL MASS (LB)
VARY	2	104		CABIN GAS MIXTURE, TEMPERATURE (F)
VARY	2	105		CABIN GAS MIXTURE, TOTAL PRESSURE (PSIA)
VARY	2	107		CABIN GAS MIXTURE, NON-CONDENSABLES MASS (LB)
VARY	2	103		CABIN GAS MIXTURE, H2O VAPOR MASS (LB)
VARY	2	109		CABIN GAS MIXTURE, ENTRAINMENT H2O MASS (LB)
VARY	2	110		CABIN GAS MIXTURE, NON-COND. SPECIFIC HEAT (BTU/LB-F)
VARY	2	111		CABIN GAS MIXTURE, NON-COND. MOL WEIGHT (LB/MOL)
VARY	2	112		CABIN GAS MIXTURE, OXYGEN MASS (LB)
VARY	2	113		CABIN GAS MIXTURE, NITROGEN MASS (LB)
VARY	2	114		CABIN GAS MIXTURE, CO2 MASS (LB)
VARY	2	115		CABIN GAS MIXTURE, TRACE CONTAMINANTS MASS (LB)
VARY	2	122	0.0833	OUTBOARD LEAKAGE RATE (LB/HR)
VARY	2	123		NON-CONDENSABLES LEAKAGE RATE (LB/HR)
VARY	2	124		H2O VAPOR LEAKAGE RATE (LB/HR)
VARY	2	125		ENTRAINED H2O LEAKAGE RATE (LB/HR)
VARY	2	126		TOTAL MASS ADDITION RATE (LB/HR)
VARY	2	127		NON-COND. ADDITION RATE (LB/HR)
VARY	2	129	0.233	H2O VAPOR ADDITION RATE (LB/HR)
VARY	2	129	0.	ENTRAINED H2O ADDITION RATE (LB/HR)
VARY	2	130		AVERAGE TEMPERATURE OF MASS ADDITIONS (F)
VARY	2	132	70.0	ADD COND VAPOR TEMP
VARY	2	135		NET TOTAL FLOW INTO CABIN (LB/HR)
VARY	2	136		NET NON-COND. FLOW INTO CABIN (LB/HR)
VARY	2	137		NET H2O VAPOR FLOW INTO CABIN - CALC IN GPOLY2
VARY	2	139	8000.	CABIN FREE VOL (FT3)
VARY	2	170	70.0	OXYGEN ADDITION TEMP (F)
VARY	2	171	70.0	NITROGEN ADDITION TEMP (F)
VARY	2	172	70.0	CO2 ADDITION TEMP (F)
VARY	2	173	70.0	TRACE CONTAMINANTS ADDITION TEMP (F)
VARY	2	174	70.0	SPECIAL FLOW NO. 1 ADDITION TEMP (F)
VARY	2	175		NET O2 ADDITION (LB/HR) - GPOLY2 CALC
VARY	2	176		NET N2 ADDITION (LB/HR) - GPOLY2 CALC
VARY	2	177	0.0	NET CO2 ADDITION (LB/HR)
VARY	2	178	0.0	NET TRACE CONTAMINANTS ADDITION (LB/HR)



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VARY 12	84	1.0	FAN ON/OFF SWITCH (1.0=ON,0.0=OFF)		
VARY 12	91	140.	FAN HEAT ADDITION (WATTS)		
ID** 13			GASHIX - SAND-II AND COND HX FAN	30	2
LEAS 13	6		12		
HSTR 13					
ID** 14			SPLIT - MAIN CABIN TO SAND BED #1, SAND BED #2	27	2
KEAS 14	10		-3		
HSTR 14					
VARY 14	65	0.0	SPLIT RATIO - GFOLY1 CALC		
VARY 14			STEAM OR CABIN GAS TO SAND BED #1 INLET	16	2
ID** 15	6		14		
LEAS 15					
HSTR 15					
ID** 16			SAND BED #1 SIMULATION - ALICOM	17	2
LEAS 16	73	0	0		
HSTR 16					
KARY 16	16		ASSORB/DESORB FLAG (0 = ABSORB, 1 = DESORB)		
KARY 16	17		COMPLEMENTARY BED'S COMPONENT NO.		
KARY 16	18		DESORBING FLOW REVERSAL FLAG: 1=YES, 0=NO		
KARY 16	19		NUMBER OF BED SEGMENTS		
KARY 16	20		DOWNSTREAM COMPONENT NUMBER		
VARY 16	60	70.0	15		
VARY 16	61	0.8	INLET TEMPERATURE (F)		
VARY 16	62	0.8	CAN-TO-AMBIENT KA/X (BTU/HR-F)		
VARY 16	63	70.0	EXTERIOR SURFACE TEMPERATURE, (DEG-F)		
VARY 16	64	0.800	CONDUCTANCE BETWEEN BED AND EXTERIOR, (BTU/HR-F)		
VARY 16	65	1270.	HEAT OF CO2 REACTION WITH RESIN BED (BTU/LB)		
VARY 16	66	0.314	SPECIFIC HEAT OF DRY IR45 RESIN, (BTU/LB-F)		
VARY 16	67	32.70	DENSITY OF DRY RESIN BED, (PCF)		
VARY 16	68	0.319	RESIN BED VOID VOLUME FRACTION		
VARY 16	69	10.0	TIME REQUIRED TO COMPLETE STEAM DESORB (SEC)		
VARY 16	70		GAS STREAM TOTAL SENSIBLE HEAT CHANGE (BTU/HR)		
VARY 16	71		GAS STREAM TOTAL LATENT HEAT CHANGE (BTU/HR)		
VARY 16	72		TOTAL CO2 ABSORPTION(+)/DESORPTION(-) RATE (PPH)		
VARY 16	73		TOTAL H2O EVAPORATION(+)/CONDENSATION(-) RATE (PPH)		
VARY 16	74	1.500	ABSORPTION/DESORPTION RATE (PPH OF CO2/LB-BED/PSI)		
VARY 16	75	0.400	AVG. STEADY STATE DESORPTION STEAM RATE (PPH)		
VARY 16	76	0.604	AVG. STEADY STATE BED TEMPERATURE, (DEG-F)		
VARY 16	77	70.00	AVG. STEADY STATE BED HEIGHT (LBN)		
VARY 16	78	8.500	TOTAL DRY RESIN BED HEIGHT (LBN)		
VARY 16	79	7.400	TOTAL CARHISTER HEIGHT (LBN)		
VARY 16	80	2.550	TOTAL WATER IN BED (LBN)		
VARY 16	81	0.005	TOTAL CO2 IN BED (LBN)		
VARY 16	82		TOTAL BED H2O LOADING (LB H2O/LB BED)		
VARY 16	83		TOTAL BED CO2 LOADING (LB CO2/LB BED)		
VARY 16	84	0.120	SPECIFIC HEAT OF CARHISTER (BTU/LB-F)		
VARY 16	85	100.0	EXIT TEMPERATURE TO END DESORPTION, DEG-F		
VARY 16	86	2280.	TIME TO END ABSORPTION, SECONDS		
VARY 16	87	240.	TIME LAG FOR OUTLET TEMPERATURE, SECONDS		
VARY 16	88		BED INLET DOW POINT, DEG-F		
VARY 16	89		BED EXIT DOW POINT, DEG-F		
VARY 16	90		BED INLET CO2 PARTIAL PRESSURE, MM-HG		
VARY 16	91		BED EXIT CO2 PARTIAL PRESSURE, MM-HG		
VARY 16	92		TOTAL BED EXIT FLOW, CFM		
VARY 16	93	0.470	TOTAL HEIGHT OF FOAM IN BED, LBN		
VARY 16	94	0.330	SPECIFIC HEAT OF FOAM (BTU/LB-F)		
VARY 16	95	100000.	TIME TO BEGIN DEBUG PRINTOFF, SECONDS.		
ID** 17			SPLIT - SAND BED #1 TO COND HX OR CO2 RECOVERY	20	2
KEAS 17	10		16		
HSTR 17					
VARY 17	65	0.0	SPLIT RATIO - GFOLY1 CALC		
ID** 18			GASHIX - SAND BED #1, SAND BED #2		



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ID** 22	SPLIT - SAHD BED #2 TO COND HX OR CO2 RECOVERY	23	2
KEAS 22	10		
HSIR 22			
VARY 22	65 1.0 SPLIT RATIO - GPOLY1 CALC		
ID** 23	GASHIX - SAHD BED #1 EXIT GAS, SAHD BED #2 EXIT GAS	24	2
KEAS 23	6		
HSIR 23	-22 2		
ID** 24	SPLIT - SAHD EXIT GAS TO PREHEAT OR TO CO2 ACCUMULATOR	18	2
KEAS 24	10		
HSIR 24			
VARY 24	65 0.0 SPLIT RATIO - GPOLY1 CALC		
ID** 25	GASHIX - STEAM GENERATOR AND PREHEAT STEAMS	26	2
KEAS 25	6		
HSIR 25	29 2		
ID** 26	SPLIT - STEAM TO SAHD BED #1 OR #2.	15	2
KEAS 26	10		
HSIR 26			
VARY 26	65 1.0 SPLIT RATIO - GPOLY1 CALC		
ID** 27	HCO SUPPLY TANK FOR STEAM GENERATOR	28	2
KEAS 27	30 3		
HSIR 27	0 1		
VARY 27	1191		
KEAS 27	1 2.55 INITIAL HCO FLOW (LB/HR)		
VARY 27	69 169.3 HCO TANK MAX CAPACITY (LB)		
VARY 27	69 169.3 HCO TANK INITIAL FILL (LB)		
VARY 27	70 70.0 HCO TEMPERATURE (F)		
VARY 27	71 TANK VOLUME (FT3)		
VARY 27	72 30.0 TANK PRESSURE (PSIA)		
VARY 27	99 WATER USED FROM TANK (LB)		
VARY 27	99 WATER ADDED TO TANK (LB)		
VARY 27	100 2.55 HCO FLOW (PPH)	29	2
ID** 28	HCO SUPPLY PUMP FOR STEAM GENERATOR		
KEAS 28	27 0 1		
HSIR 28			
VARY 28	0002		
VARY 28	79 1.0 PUMP ON/OFF FLAG (1.0=ON)		
VARY 28	85 10.0 HEAT ADDITION (WATTS)		
ID** 29	STEAM GENERATOR FOR SAHD BED DESORPTION	25	2
KEAS 29	27		
HSIR 29	1		
VARY 29	66 40.0		
VARY 29	67		
VARY 29	69		
ID** 30	SPLIT - DESORBED GAS TO CABIN OR CO2 ACCUMULATOR.	32	2
KEAS 30	10		
HSIR 30			
VARY 30	65 1.0 SPLIT RATIO - GPOLY1 CALC	7	2
ID** 31	GASHIX - CABIN AIR AND SAHD AIR TO HUMID CONTROL HX		
KEAS 31	6		
HSIR 31			
ID** 32	CO2 ACCUMULATOR TANK	31	2
KEAS 32	30		
HSIR 32	01900		
VARY 32	16		
VARY 32	70 70.0		
VARY 32	71 2.0		
VARY 32	72 30.0		
VARY 32	80 0.4644		
VARY 32	80 0.4644		
TABL 1	1 2		
TABL 1	2		
TITL 1	2 CREWMAN METABOLIC RATE (BTU/HR) VS MISSION TIME (SEC)	1960E+05	
TITL 1	20	3600.	1870E+05
TITL 1	21	2700.	450.0
TITL 1	22	450.0	650.0
TITL 1	23	500.0	650.0
TITL 1	24	450.0	650.0
VALU	1 11 2D	450.0	650.0



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TITL	33	2	ABSORPTION CYCLE TIME (SEC) VS. SAID FAN FLOW (CFM)	7.90	11.00	12.80	13.95
VALU	33	10	21	0.10	5.00	7.90	11.00
VALU	33	11	21	0	60.	120.	240.
VALU	33	12	21	14.60	15.0	15.0	360.
VALU	33	13	21	600.	720.	900.	7200.
TACL	41	1	2	0	LOG	LIN	
TITL	41	2	HOLE FRACTION OF CO2 IN BED SEGMENT VERSUS LOADING.	0.02	0.03	0.04	0.05
VALU	41	10	21	0.01	0.0046	0.0019	0.0050
VALU	41	11	21	0.06	0.07	0.0800	0.0825
VALU	41	12	21	0.0225	0.054	0.068	0.1100
VALU	41	13	21	0.00052	0.094	1.0	0.250
VALU	41	14	21	0.0005	0.090	1.0	
VALU	41	15	21	0.5100	0.630	1.0	
TACL	51	1	2	0	LOG	LIN	
TITL	51	2	TEMPERATURE FACTOR ON CALCULATION OF EQUIL YCO2.	77.	90.	110.	150.
VALU	51	10	21	55.	1.00	0.670	0.790
VALU	51	11	21	1.20	190.	210.0	250.
VALU	51	12	21	170.	0.060	0.0300	0.0150
VALU	51	13	21	0.2750	0.1550	0.0300	0.0001
TACL	61	1	2	0	LOG	LIN	
TITL	61	2	WATER LOADING FACTOR ON CALCULATION OF EQUIL YCO2.	0.09	0.105	0.125	0.157
VALU	61	10	21	0.0	0.550	0.571	0.745
VALU	61	11	21	0.551	0.225	0.250	0.275
VALU	61	12	21	0.200	1.410	1.429	1.440
VALU	61	13	21	1.360	0	0	0
TACL	71	1	2	0	LOG	LIN	
TITL	71	2	INFLUENCE OF RELATIVE HUMIDITY ON EQUILIBRIUM WATER LOADING	0.000	0.010	0.035	0.060
VALU	71	10	21	-10.00	0.000	0.100	0.300
VALU	71	11	21	0.00	0.165	0.190	0.230
VALU	71	12	21	0.104	0.600	0.700	0.800
VALU	71	13	21	0.500			
VALU	71	14	21	1.000			
VALU	71	15	21	1.000			
PLOT0				2	181		
PLOT1				2	182		
PLOT2				1	66		
PLOT2				1	67		
PLOT2				1	69		
PLOT2				1	69		
PLOT2				2	59		
PLOT2				2	94		
PLOT2				2	95		
PLOT2				2	98		
PLOT2				2	100		
PLOT2				2	104		
PLOT2				2	105		
PLOT2				2	165		
PLOT2				2	166		
PLOT2				15	6		
PLOT2				16	6		
PLOT2				15	12		
PLOT2				16	12		
PLOT2				16	2		
PLOT2				16	82		
PLOT2				16	63		
PLOT2				20	6		
PLOT2				21	6		
PLOT2				20	12		

ESCM DEMONSTRATION MODEL

- MISSION TIME (SEC)
- MISSION TIME (MIN)
- CRENHAN SEN (BTU/HR)
- CRENHAN LAT (BTU/HR)
- O2 USE RATE (LB/HR)
- CO2 GEN RATE (LB/HR)
- CRENHAN NET (BTU/HR)
- REL HUMIDITY (DEC)
- O2 PRESSURE (PSIA)
- HC PRESSURE (PSIA)
- DEW POINT TEMP (F)
- CO2 P'PRESS (MM HG)
- DRY BULB TEMP (F)
- TOTAL PRESS (PSIA)
- O2 MAKEUP (LB/HR)
- HC MAKEUP (LB/HR)
- SA-1 HCO IH (LB/HR)
- SA-1 HCO OH (LB/HR)
- SA-1 CO2 IH (LB/HR)
- SA-1 CO2 OH (LB/HR)
- SA-1 EXIT TEMP (F)
- SA-1 HCO LOAD (LB/LB)
- SA-1 CO2 LOAD (LB/LB)
- SA-2 HCO IH (LB/HR)
- SA-2 CO2 IH (LB/HR)



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BASIC CASE DATA

ESCM: BASELINE, VOL = 8000 FT-3, PCO2 = 2.5, .275 PPH AVERAGE

ARS DEMO MODEL FOR SAND II GENERAL NOTES:

ID**	0	1	2	3	4	5	14	2
101000	ID**	10	FLUID TYPE CODES	1	NO TESTS, SS CALCS			
101010	ID**	11	1 = WATER	2	TEMP (F)			
101011	ID**	12	2 = CO2 GAS @ 70 F, 3 MM HG	3	PRESS (PSIA)			
101012	ID**	1		4	H2O VAPOR FLOW (LB/HR)			
101090	ID**	1	90	5	OXYGEN FLOW (LB/HR)			
101100	ID**	1	100	6	NITROGEN FLOW (LB/HR)			
102000	KRAS	1	0	7	CO2 FLOW (LB/HR)			
103000	HSTR	1	00	8	TOTAL METABOLIC HEAT - ALL CREWMEN (BTU/HR)			
104016	N:RY	1	16	9	SENSIBLE HEAT PER CREWMAN (BTU/HR)			
105002	VARY	1	2	10	LATENT HEAT PER CREWMAN (BTU/HR)			
105003	VARY	1	3	11	TOTAL OXYGEN USE RATE (LB/HR)			
105006	VARY	1	6	12	TOTAL H2O VAPOR GENERATION RATE (LB/HR)			
105010	V:RY	1	10	13	INLET GAS RELATIVE HUMIDITY (DECIMAL)			
105011	V:RY	1	11	14	INLET GAS RELATIVE HUMIDITY (DECIMAL)			
105012	VARY	1	12	15	OUTLET GAS RELATIVE HUMIDITY (DECIMAL)			
105065	VARY	1	65	16	OUTLET GAS RELATIVE HUMIDITY (DECIMAL)			
105065	VARY	1	66	17	TOTAL METABOLIC RATE PER CREWMAN (BTU/HR)			
105067	VARY	1	67	18	TOTAL OXYGEN USE RATE (LB/HR)			
105068	VARY	1	68	19	TOTAL H2O VAPOR GENERATION RATE (LB/HR)			
105069	VARY	1	69	20	INLET GAS RELATIVE HUMIDITY (DECIMAL)			
105070	VARY	1	70	21	INLET GAS RELATIVE HUMIDITY (DECIMAL)			
105075	VARY	1	75	22	OUTLET GAS RELATIVE HUMIDITY (DECIMAL)			
105076	VARY	1	76	23	OUTLET GAS RELATIVE HUMIDITY (DECIMAL)			
105077	VARY	1	77	24	TOTAL METABOLIC RATE PER CREWMAN (BTU/HR)			
105078	VARY	1	78	25				
105082	VARY	1	82	26				
201000	ID**	2	0	27				
202000	KBAS	2	0	28				
203000	HSTR	2	0151011000	29				
205002	VARY	2	2	30				
205003	VARY	2	3	31				
205006	VARY	2	6	32				
205010	VARY	2	10	33				
205011	VARY	2	11	34				
205012	VARY	2	12	35				
205021	VARY	2	21	36				
205022	VARY	2	22	37				
205025	VARY	2	25	38				
205029	VARY	2	29	39				
205030	VARY	2	30	40				
205031	VARY	2	31	41				
205065	VARY	2	65	42				
205066	V:RY	2	66	43				
205071	VARY	2	71	44				
205072	VARY	2	72	45				
205073	VARY	2	73	46				
205074	VARY	2	74	47				
205007	VARY	2	87	48				
205009	V:PY	2	89	49				
205009	V:PY	2	90	50				
205091	VARY	2	91	51				
205092	VARY	2	92	52				



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405076	VARY	4	76	2100.	CABIN FAN VOLUMETRIC FLOW RATE (CFM)						
405084	VARY	4	8	1.0	FAN ON/OFF SWITCH (1.0=ON, 0.0=OFF)						
405091	VARY	4	91	833.	FAN HEAT ADDITION (WATTS)						
501000	ID**	5	0	0	MAIN CABIN SENSIBLE HX - SENSIBLE HEAT REMOVAL ONLY					1	2
502000	KBAS	5	0	4	COUNTERFLOW, PRI=GAS, SEC=LIQ, SS CALC						
503000	HSTR	5	0	0	HX COUNTERFLOW UA (BTU/HR-F)						
505006	VARY	5	66	6240.							
601000	ID**	6	0	0	COOLING FLUID BOUNDARY COND - CABIN SENSIBLE HX					2	
602000	KBAS	6	0	49							
603000	HSTR	6	0	0							
604016	KARY	6	16	0	KPRINT VALUE AT START OF TRANSIENT (GPOLY1)						
604017	KARY	6	17	0	KCHOUT VALUE AT START OF TRANSIENT (GPOLY1)						
605001	VARY	6	1	1350.	COOLANT FLOW (LB/HR) - GPOLY1 CALC						
605002	VARY	6	2	60.0	COOLANT TEMP (F)						
605003	VARY	6	3	50.0	COOLANT FLOW (PSIA)						
701000	ID**	7	0	0	MAIN CABIN CONDENSING HX					9	2
702000	KBAS	7	0	4							
703000	HSTR	7	0	2	INPUT EFF, PRI=GAS, SEC=LIQ, SS CALCS						
705066	VARY	7	66	1000.	COUNTERFLOW HX UA (BTU/HR-F) - GPOLY1 CALC						
801000	ID**	8	0	0	COOLING FLUID BOUNDARY COND - CABIN COND HX					2	
802000	KBAS	8	0	49							
803000	HSTR	8	0	0							
805001	VARY	8	1	950.	COOLANT FLOW (LB/HR)						
805002	VARY	8	2	45.0	COOLANT TEMP (F)						
805003	VARY	8	3	50.0	COOLANT FLOW (PSIA)						
901000	ID**	9	0	0	SPLIT - COND HX TO WATER SEPARATOR BYPASS, WATER SEPARATOR					10	2
902000	KBAS	9	0	10							
903000	HSTR	9	0	01	SPECIFY INDIVIDUAL SPLIT RATIOS						
905005	VARY	9	66	0.03	SPLIT RATIO - COND VAPOR						
905007	VARY	9	67	1.00	SPLIT RATIO - COND LIQUID						
905008	VARY	9	68	0.03	SPLIT RATIO - OXYGEN						
905009	VARY	9	69	0.03	SPLIT RATIO - NITROGEN						
905010	VARY	9	70	0.03	SPLIT RATIO - CARBON DIOXIDE						
905071	VARY	9	71	0.03	SPLIT RATIO - TRACE CONTAMINANTS						
905072	VARY	9	72	0.03	SPLIT RATIO - SPECIAL FLOW #1						
1001000	ID**	10	0	0	WATER SEPARATOR - CABIN COND HX					11	2
1002000	KBAS	10	0	49							
1003000	HSTR	10	0	02	CALC EXIT TREP GIVEN Q						
1005005	VARY	10	65		HEAT ADDED (BTU/HR) - GPOLY1 CALC						
1005057	VARY	10	67		CONDENSATE REMOVED (LB/HR) - GPOLY1 CALC						
1101000	ID**	11	0	0	GASHIX - COND HX WATER SEPARATOR, WATER SEPARATOR BYPASS					12	2
1102000	KBAS	11	0	6							
1103000	HSTR	11	0	0							
1201000	ID**	12	0	0	COND HX FAN					13	2
1202000	KBAS	12	0	23							
1203000	HSTR	12	0	01	INPUT CFM & Q						
1205076	VARY	12	76	300.	CABIN FAN VOLUMETRIC FLOW RATE (CFM)						
1205084	VARY	12	8	1.0	FAN ON/OFF SWITCH (1.0=ON, 0.0=OFF)						
1205091	VARY	12	91	140.	FAN HEAT ADDITION (WATTS)						
1301000	ID**	13	0	0	GASHIX - SAHD-II AND COND HX FAN					30	2
1302000	KBAS	13	0	6							



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ID**	18	0	GASHIX - SAND BED #1, SAND BED #2	-22 2	19	2
1801000	18	0	GASHIX - SAND BED #1, SAND BED #2	-22 2	19	2
1802000	18	0		17 2		
1803000	18	0				
1901000	19	0	SAND BED FAN	18 2	30	2
1902000	19	0	INPUT Q ONLY			
1903000	19	0003	CABIN GAS MIXTURE: INITIAL TEMP (F)			
1904000	19	2 70.	4 TOTAL PRESSURE (PSIA)			
1905003	19	3 16.7	HCO VAPOR FLOW (LB/HR)			
1906006	19	6 0.78	OXYGEN FLOW (LB/HR)			
1907010	19	10 20.55	NITROGEN FLOW (LB/HR)			
1908011	19	11 71.07	CO2 FLOW (LB/HR)			
1909012	19	12 0.30	CABIN FAN VOLUMETRIC FLOW RATE (CFM)			
1910076	19	76 15.	FAN ON/OFF SWITCH (1.0=ON, 0.0=OFF)			
1910054	19	84 1.0	FAN HEAT ADDITION (WATTS)			
1915071	19	91 50.				
2001000	20	0	GASHIX - STEAM CR CABIN GAS TO SAND BED #2 INLET	26 2	21	2
2002000	20	0 6		-14 2		
2003000	20	02				
2101000	21	0	SAND BED #2 SIMULATION - ALTCOM	20 2	22	2
2102000	21	0 73 0 0				
2103000	21	0	1 ABSORB/DESORB FLAG (0 = ABSORB, 1 = DESORB)			
2104016	21	16	16 COMPLEMENTARY BED'S COMPONENT NO.			
2104017	21	17	0 DESORBING FLOW REVERSAL FLAG: 1=YES, 0=NO			
2104018	21	18	0 NUMBER OF BED SEGMENTS			
2104019	21	19	5 DOWNSTREAM COMPONENT NUMBER			
2104020	21	20	20 AMBIENT TEMPERATURE (F)			
2105060	21	60 70.0	CAN-TO-AMBIENT K/A/X (BTU/HR-F)			
2105061	21	61 0.9	EXTERIOR SURFACE TEMPERATURE, (DEG-F)			
2105063	21	63 70.0	CONDUCTANCE BETWEEN BED AND EXTERIOR, (BTU/HR-F)			
2105064	21	64 0.990	HEAT OF CO2 REACTION WITH RESIN BED (BTU/LB)			
2105065	21	65 1270.	HEAT OF CO2 REACTION WITH IR45 RESIN, (BTU/LB-F)			
2105066	21	66 0.314	SPECIFIC HEAT OF DRY RESIN BED, (PCF)			
2105067	21	67 32.70	DENSITY OF DRY RESIN BED, (PCF)			
2105068	21	68 0.319	RESIN BED VOID VOLUME FRACTION			
2105069	21	69 10.0	TIME REQUIRED TO COMPLETE STEAM DESORB (SEC)			
2105070	21	70	GAS STREAM TOTAL SENSIBLE HEAT CHANGE (BTU/HR)			
2105071	21	71	GAS STREAM TOTAL LATENT HEAT CHANGE (BTU/HR)			
2105072	21	72	TOTAL CO2 ABSORPTION(+)/DESORPTION(-) RATE (PPH)			
2105073	21	73	TOTAL H2O EVAPORATION(+)/CONDENSATION(-) RATE (PPH)			
2105074	21	74 1.500	AVG. STEADY STATE DESORPTION STEAM RATE (PPH)			
2105075	21	75 0.400	AVG. STEADY STATE CO2 REMOVAL EFFICIENCY			
2105076	21	76 0.604	AVG. STEADY STATE BED TEMPERATURE, (DEG-F)			
2105077	21	77 70.00	TOTAL DRY RESIN BED WEIGHT (LBM)			
2105078	21	78 8.500	TOTAL CANISTER WEIGHT (LBM)			
2105079	21	79 7.400	TOTAL WATER IN BED (LBM)			
2105080	21	80 2.080	TOTAL CO2 IN BED (LBM)			
2105081	21	81 0.300	TOTAL BED H2O LOADING (LB H2O/LB BED)			
2105082	21	82	TOTAL BED CO2 LOADING (LB CO2/LB BED)			
2105083	21	83	SPECIFIC HEAT OF CANISTER (BTU/LB-F)			
2105084	21	84 0.120	EXIT TEMPERATURE TO END DESORPTION, DEG-F			
2105085	21	85 180.0	TIME TO END ABSORPTION, SECONDS			
2105086	21	86 2090.	TIME LAG FOR OUTLET TEMPERATURE, SECONDS			
2105087	21	87 240.	BED INLET DEM POINT, DEG-F			
2105088	21	88	BED EXIT DEM POINT, DEG-F			
2105089	21	89	BED INLET CO2 PARTIAL PRESSURE, MM-HG			
2105090	21	90	BED EXIT CO2 PARTIAL PRESSURE, MM-HG			
2105091	21	91				

ID**	0	6	3	2	7	2
3102000	KZAS	31	0	6		
3103000	HSIR	31	0			
3201000	ID**	32	0	CO2 ACCUMULATOR TANK		
3202000	KEAS	32	0	30	1	30 2
3203000	HSIR	32	001000			
3204016	KARY	32	16			
3205070	VARY	32	70 70.			
3205071	VARY	32	71 2.0			
3205072	VARY	32	72 30.0			
3205073	VARY	32	80 0.4644			
100102010	TASL	1	10 ¹	2	0	LIN LIN
100110020	TITL	1	COGRENHAN METAEOIC RATE (DTU/HR) VS MISSION TIME (SEC)			
100111100	VALU	1	1002I	0	2700.	7200. .1800E+05
100111110	VALU	1	1102D	450.0	520.0	650.0 450.0
100111120	VALU	1	1202I	.2340E+05	.3960E+05	.4140E+05 .4320E+05
100111130	VALU	1	1302D	450.0	650.0	520.0 450.0
100111140	VALU	1	1402I	.5040E+05	.5560E+05	.8640E+05
100111150	VALU	1	1502D	390.0	300.0	300.0
100102020	TASL	10	10	2	3	LIN STP
100102030	TITL	10	20	PRESSURE CONTROL SYSTEM OPERATION		
1001010030	TITL	10	30	PRESSURE MODE VS MISSION TIME (SEC)		
1001010040	TITL	10	40	= 14.5 PSI CONTROLLER USED		
1001010050	TITL	10	50	= 8.0 PSI CONTROLLER USED		
100101100	VALU	10	1002I	-8400.	15300.	427864.
100101110	VALU	10	1102D	0.0	0.0	0.0
100209010	TASL	20	10	2	6	LIN LIN
1002010020	TITL	20	20	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE		
1002010030	TITL	20	3002	OPENING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)		
1002010040	TITL	20	4002	OPENING FLOWS VS TOTAL PRESSURE (PSIA)		
100201100	VALU	20	1002I	0.0	14.510	14.585 14.666
100201110	VALU	20	1102D	10.0	10.0	0.2 0.0
100209020	TASL	21	10	2	6	LIN LIN
100210020	TITL	21	20	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE		
100210030	TITL	21	3002	CLOSING FLOWS VS TOTAL PRESSURE (PSIA)		
100211100	VALU	21	1002I	0.0	14.605	14.672 14.745
100211110	VALU	21	1102D	10.0	10.0	0.6 0.25
100209030	TASL	22	10	2	8	LIN LIN
100221020	TITL	22	20	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE		
100221030	TITL	22	3002	OPENING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)		
100221040	TITL	22	4002	OPENING FLOWS VS TOTAL PRESSURE (PSIA)		
100221100	VALU	22	1002I	0.0	14.500	14.583 14.583
100221110	VALU	22	1102D	67.0	67.0	7.0 1.0
100221120	VALU	22	1202I	14.748	100.0	0.0
100221130	VALU	22	1302D	0.0	0.0	0.0
1002309010	TASL	23	10	2	8	LIN LIN
1002310020	TITL	23	20	PRESSURE CONTROL SUBSYSTEM REGULATOR FLOWRATE CURVE		
1002310030	TITL	23	3002	CLOSING FLOWS (FROM JULY 1980 PCS TESTING AT JSC)		
100231100	VALU	23	1002I	0.0	14.590	14.625 14.658
100231110	VALU	23	1102D	67.0	67.0	7.0 0.8
100231120	VALU	23	1202I	14.813	100.0	0.0
100231130	VALU	23	1302D	0.0	0.0	0.0
1003009010	TASL	30	10	2	12	0

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COMPONENT NO. =	0	1	2	3	4	5	6	7	8
SER. TYPE =	SUITS	CASIN	SPLIT	FAN	ANYHX	ALTCOM	ANYHX	ALTCOM	ALTCOM
VR 1-TOTAL FRI FLOM P	.0	.0	.0	.0	.0	.0	.0	.0	950.000
2-TEMPERATURE R	50.0000	70.0000	.0	.0	.0	.0	.0	.0	45.0000
3-DUCT OUTLET P I	14.7000	14.7000	.0	.0	.0	.0	.0	.0	50.0000
4-COMP OUTLET P H	14.7000	14.7000	.0	.0	.0	.0	.0	.0	50.0000
5-REF-COOL FLOM A	.0	.0	.0	.0	.0	.0	.0	.0	.0
6-COOL VAP FLOM R	87.8000	89.7000	.0	.0	.0	.0	.0	.0	.0
7-COOL LIQ FLOM Y	.0	.0	.0	.0	.0	.0	.0	.0	.0
8-R-C SP HEAT	.0	.0	.0	.0	.0	.0	.0	.0	.0
9-R-C HOL WT	.0	.0	.0	.0	.0	.0	.0	.0	.0
10-OXIGEN FLOM I	2046.80	2046.80	.0	.0	.0	.0	.0	.0	.0
11-DILUENT FLOM D	7200.70	7189.40	.0	.0	.0	.0	.0	.0	.0
12-CO2 FLOM E	46.7000	46.3000	.0	.0	.0	.0	.0	.0	.0
13-TRACE CTH FLOM	.0	.0	.0	.0	.0	.0	.0	.0	.0
14-SFCL FLOM 1	D	.0	.0	.0	.0	.0	.0	.0	.0
15-SFCL FLOM 2	A	.0	.0	.0	.0	.0	.0	.0	.0
16-SFCL FLOM 3	T	.0	.0	.0	.0	.0	.0	.0	.0
17-SFCL FLOM 4	A	.0	.0	.0	.0	.0	.0	.0	.0
18-SFCL FLOM 5	A	.0	.0	.0	.0	.0	.0	.0	.0
19-SFCL FLOM 6	A	.0	.0	.0	.0	.0	.0	.0	.0
20-TOTAL SEC FLOM S	.0	.0	.0	.0	.0	.0	.0	.0	.0
21-TEMPERATURE E	.0	70.0000	.0	.0	.0	.0	.0	.0	.0
22-DUCT OUTLET P C	.0	14.7000	.0	.0	.0	.0	.0	.0	.0
23-COMP OUTLET P O	.0	14.7000	.0	.0	.0	.0	.0	.0	.0
24-NON-COOL FLOM N	.0	.0	.0	.0	.0	.0	.0	.0	.0
25-COOL VAP FLOM D	.0	13.8000	.0	.0	.0	.0	.0	.0	.0
26-COOL LIQ FLOM A	.0	.0	.0	.0	.0	.0	.0	.0	.0
27-R-C SP HEAT	.0	.0	.0	.0	.0	.0	.0	.0	.0
28-R-C HOL WT	.0	.0	.0	.0	.0	.0	.0	.0	.0
29-OXIGEN FLOM	.0	303.760	.0	.0	.0	.0	.0	.0	.0
30-DILUENT FLOM S	.0	1068.67	.0	.0	.0	.0	.0	.0	.0
31-CO2 FLOM I	.0	9.45000	.0	.0	.0	.0	.0	.0	.0
32-TRACE CTH FLOM D	.0	.0	.0	.0	.0	.0	.0	.0	.0
33-SFCL FLOM 1	E	.0	.0	.0	.0	.0	.0	.0	.0
34-SFCL FLOM 2	D	.0	.0	.0	.0	.0	.0	.0	.0
35-SFCL FLOM 3	D	.0	.0	.0	.0	.0	.0	.0	.0
36-SFCL FLOM 4	A	.0	.0	.0	.0	.0	.0	.0	.0
37-SFCL FLOM 5	T	.0	.0	.0	.0	.0	.0	.0	.0
39-SFCL FLOM 6	A	.0	.0	.0	.0	.0	.0	.0	.0
39-OH, C, DP PRI P	.0	.0	.0	.0	.0	.0	.0	.0	.0
40-LE, N, K DUCT R	.0	.0	.0	.0	.0	.0	.0	.0	.0
41-FF AREA	E	.0	.0	.0	.0	.0	.0	.0	.0
42-OH, C, DP PRI S	.0	.0	.0	.0	.0	.0	.0	.0	.0
43-LE, N, K COMP S	.0	.0	.0	.0	.0	.0	.0	.0	.0
44-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0
45-OH, C, DP SEC C	.0	.0	.0	.0	.0	.0	.0	.0	.0
46-LE, N, K DUCT O	.0	.0	.0	.0	.0	.0	.0	.0	.0
47-FF AREA	E	.0	.0	.0	.0	.0	.0	.0	.0
48-OH, C, DP SEC F	.0	.0	.0	.0	.0	.0	.0	.0	.0
49-LE, N, K COMP F	.0	.0	.0	.0	.0	.0	.0	.0	.0
50-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0
51-COMP SOURCE TEMP	.0	.0	.0	.0	.0	.0	.0	.0	.0



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COMPONENT NO. = SER. TYPE =	1 SUITS	2 CABIN	3 SPLIT	4 FAN	5 ANYHX	6 ALTCOM	7 ANYHX	8 ALTCOM
1-SUBR NO./EXV/EXK	2001000	1025000	10000000	23000000	4000000	49000002	4000000	49000000
2-FYI 90R/FLO CODE	502	102	-202	202	402	0	3102	0
3-FRI SPFL TYP 1-3	0	0	0	0	0	10000	0	10000
4-FRI SPFL TYP 4-6	0	0	0	0	0	0	0	0
5-SEC 502/FLO CODE	0	-1302	2	0	-600	0	-800	0
6-SEC SPFL TYP 1-3	0	0	0	0	10000	0	10000	0
7-SEC SPFL TYP 4-6	0	0	0	0	0	0	0	0
8-NEXT COMP/CABIN	1400002	300002	400002	500002	100002	2	900002	2
9-COMP NSTR 1-9	0	151011000	0	100000000	200000000	0	200000000	0
10-COMP NSTR 10-16	100	0	0	0	100	0	100	0
11-RCFL/HFL/HPASS	0	0	0	0	0	0	0	0
12-PRI VISC/DENSITY	0	0	0	0	0	0	0	0
13-PRI OP/DP/OP/DP	0	0	0	0	0	0	0	0
14-SEC VISC/DENSITY	0	0	0	0	0	0	0	0
15-SEC OP/DP/OP/DP	0	0	0	0	0	0	0	0

SUBROUTINE DEPENDENT K ARRAY DATA - - -

KR(1, 16)=	3	KR(2, 16)=	0	KR(2, 17)=	0	KR(4, 16)=	0	KR(4, 17)=	0
KR(4, 18)=	0	KR(5, 16)=	0	KR(6, 16)=	0	KR(6, 17)=	0	KR(7, 16)=	0



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DESCRIPTION	QTY	UNIT	PRICE	TOTAL	REMARKS
53-EFF SURFED COND	.0			.0	
53-COND QUOTOL LOSS	.0			.0	
54-AGENT GAS TEMP	.0			.0	
55-AGENT UA	.0			.0	
56-ARA CCNV Q LOSS	.0			.0	
57-ARA BALL TEMP	.0			.0	
58-ARA SCRIP(F)*A	.0			.0	
59-ARA R49 Q LOSS	.0			.0	
60-STRUCTURE TEMP	.0			.0	
61-STRUCTURE N/A/X	.0			.0	
62-STRUCTURE Q LOSS	.0			.0	
63-REGULATION TEMP	.0			.0	
64-REGULATION N/A/X	.0			.0	
SUBROUTINE DEPENDENT V ARRAY DATA - - -					
VR(9, 65)=	.0	VR(9, 66)=	.30000E-01	VR(9, 67)=	1.0000
VR(9, 70)=	.30000E-01	VR(9, 71)=	.30000E-01	VR(9, 72)=	.30000E-01
VR(10, 67)=	.0	VR(11, 65)=	.0	VR(12, 65)=	.0
VR(12, 69)=	.0	VR(12, 69)=	.0	VR(12, 70)=	.0
VR(12, 73)=	.0	VR(12, 73)=	.0	VR(12, 75)=	.0
VR(12, 79)=	.0	VR(12, 79)=	.0	VR(12, 80)=	.0
VR(12, 83)=	.0	VR(12, 83)=	.0	VR(12, 85)=	.0
VR(12, 89)=	.0	VR(12, 89)=	.0	VR(12, 90)=	.0
VR(12, 93)=	.0	VR(13, 65)=	.0	VR(14, 65)=	.0
VR(12, 96)=	.31400	VR(16, 67)=	32.700	VR(16, 68)=	.31900
VR(16, 71)=	.0	VR(16, 72)=	.0	VR(16, 73)=	.0
VR(16, 76)=	.60400	VR(16, 77)=	70.000	VR(16, 78)=	8.5000
VR(16, 81)=	.50000E-02	VR(16, 82)=	.0	VR(16, 83)=	.0
VR(16, 86)=	2230.0	VR(16, 87)=	240.00	VR(16, 89)=	.47000
VR(16, 91)=	.0	VR(16, 92)=	.0	VR(16, 93)=	.0
VR(16, 96)=	.0	VR(16, 97)=	.0	VR(16, 103)=	.0
VR(16, 101)=	.0	VR(16, 102)=	.0	VR(16, 108)=	.0
VR(16, 106)=	.0	VR(16, 107)=	.0	VR(16, 113)=	.0
VR(16, 111)=	.0	VR(16, 112)=	.0	VR(16, 118)=	.0
VR(16, 116)=	.0	VR(16, 117)=	.0	VR(16, 123)=	.0
VR(16, 121)=	.0	VR(16, 122)=	.0	VR(16, 129)=	.0
VR(16, 126)=	.0	VR(16, 127)=	.0	VR(16, 133)=	.0
VR(16, 131)=	.0	VR(16, 132)=	.0	VR(16, 139)=	.0
VR(16, 136)=	.0	VR(16, 141)=	.0	VR(16, 143)=	.0
VR(16, 141)=	.0	VR(16, 142)=	.0	VR(16, 148)=	.0
VR(16, 145)=	.0	VR(16, 147)=	.0	VR(16, 153)=	.0
VR(16, 151)=	.0	VR(16, 152)=	.0	VR(16, 159)=	.0
VR(16, 156)=	.0	VR(16, 157)=	.0	VR(16, 163)=	.0
VR(16, 161)=	.0	VR(16, 162)=	.0	VR(16, 168)=	.0
VR(16, 166)=	.0	VR(16, 167)=	.0	VR(16, 173)=	.0
VR(16, 171)=	.0	VR(16, 172)=	.0	VR(16, 178)=	.0
VR(16, 176)=	.0	VR(16, 177)=	.0	VR(16, 183)=	.0
VR(16, 181)=	.0	VR(16, 182)=	.0	VR(16, 188)=	.0
VR(16, 186)=	.0	VR(16, 197)=	.0	VR(16, 193)=	.0
VR(16, 199)=	.0	VR(16, 192)=	.0	VR(16, 198)=	.0
VR(16, 195)=	.0	VR(16, 197)=	.0	VR(16, 203)=	.0
VR(16, 201)=	.0	VR(16, 202)=	.0	VR(16, 209)=	.0
VR(16, 206)=	.0	VR(16, 207)=	.0	VR(16, 213)=	.0
VR(16, 211)=	.0	VR(16, 212)=	.0	VR(16, 218)=	.0
VR(16, 216)=	.0	VR(16, 217)=	.0	VR(16, 223)=	.0
VR(16, 221)=	.0	VR(16, 222)=	.0	VR(16, 229)=	.0
VR(16, 226)=	.0	VR(16, 227)=	.0	VR(16, 233)=	.0
VR(16, 231)=	.0	VR(16, 232)=	.0	VR(16, 237)=	.0
VR(16, 236)=	.0	VR(16, 237)=	.0	VR(16, 239)=	.0



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COMPONENT NO. =	17	18	19	20	21	22	23	24
SUBTYPE =	SPLIT	GAS MIX	FAN	GAS MIX	IR45	SPLIT	GAS MIX	SPLIT
VR								
1-TOTAL FRI FLOW P	.0	.0	.0	.0	.0	.0	.0	.0
2-TEMPERATURE R	.0	.0	70.0000	.0	.0	.0	.0	.0
3-DUCT OUTLET P I	.0	.0	14.7000	.0	.0	.0	.0	.0
4-COOL OUTLET P M	.0	.0	14.7000	.0	.0	.0	.0	.0
5-NON-COOL FLOW A	.0	.0	.0	.0	.0	.0	.0	.0
6-COOL VAP FLOW R	.0	.0	.780000	.0	.0	.0	.0	.0
7-COOL LIQ FLOW Y	.0	.0	.0	.0	.0	.0	.0	.0
8-H-C SP HEAT	.0	.0	.0	.0	.0	.0	.0	.0
9-H-C HOL HT	.0	.0	.0	.0	.0	.0	.0	.0
10-OXYGEN FLOW I	.0	.0	20.5500	.0	.0	.0	.0	.0
11-DILUENT FLOW D	.0	.0	71.6700	.0	.0	.0	.0	.0
12-COOL FLOW E	.0	.0	.300000	.0	.0	.0	.0	.0
13-TRACE CTH FLOW	.0	.0	.0	.0	.0	.0	.0	.0
14-SFCL FLOW 1	.0	.0	.0	.0	.0	.0	.0	.0
15-SFCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0
16-SFCL FLOW 3	.0	.0	.0	.0	.0	.0	.0	.0
17-SFCL FLOW 4	.0	.0	.0	.0	.0	.0	.0	.0
18-SFCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0
19-SFCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0
20-TOTAL SEC FLOW S	.0	.0	.0	.0	.0	.0	.0	.0
21-TEMPERATURE E	.0	.0	.0	.0	.0	.0	.0	.0
22-DUCT OUTLET P C	.0	.0	.0	.0	.0	.0	.0	.0
23-COOL OUTLET P O	.0	.0	.0	.0	.0	.0	.0	.0
24-HOOL-COOL FLOW H	.0	.0	.0	.0	.0	.0	.0	.0
25-COOL VAP FLOW D	.0	.0	.0	.0	.0	.0	.0	.0
26-COOL LIQ FLOW A	.0	.0	.0	.0	.0	.0	.0	.0
27-H-C SP HEAT	.0	.0	.0	.0	.0	.0	.0	.0
28-H-C HOL HT	.0	.0	.0	.0	.0	.0	.0	.0
29-OXYGEN FLOW I	.0	.0	.0	.0	.0	.0	.0	.0
30-DILUENT FLOW S	.0	.0	.0	.0	.0	.0	.0	.0
31-COOL FLOW I	.0	.0	.0	.0	.0	.0	.0	.0
32-TRACE CTH FLOW D	.0	.0	.0	.0	.0	.0	.0	.0
33-SFCL FLOW 1	.0	.0	.0	.0	.0	.0	.0	.0
34-SFCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0
35-SFCL FLOW 3	.0	.0	.0	.0	.0	.0	.0	.0
36-SFCL FLOW 4	.0	.0	.0	.0	.0	.0	.0	.0
37-SFCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0
38-SFCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0
39-DH, C, DP FRI P	.0	.0	.0	.0	.0	.0	.0	.0
40-LE, N, K DUCT R	.0	.0	.0	.0	.0	.0	.0	.0
41-FF AREA E	.0	.0	.0	.0	.0	.0	.0	.0
42-RH, C, DP FRI S	.0	.0	.0	.0	.0	.0	.0	.0
43-LE, N, K COHP S	.0	.0	.0	.0	.0	.0	.0	.0
44-FF AREA A	.0	.0	.0	.0	.0	.0	.0	.0
45-DH, C, DP SEC C	.0	.0	.0	.0	.0	.0	.0	.0
46-LE, N, K DUCT O	.0	.0	.0	.0	.0	.0	.0	.0
47-FF AREA E	.0	.0	.0	.0	.0	.0	.0	.0
48-DH, C, DP SEC F	.0	.0	.0	.0	.0	.0	.0	.0
49-LE, N, K COHP F	.0	.0	.0	.0	.0	.0	.0	.0
50-FF AREA A	.0	.0	.0	.0	.0	.0	.0	.0
51-COOL SOURCE TEMP	.0	.0	.0	.0	.0	.0	.0	.0



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VR(29, 65) = .0 VR(

COMPONENT NO. =	17	18	19	20	21	22	23	24
SUFR. TYPE =	SPLIT	GAS MIX	FAN	GAS MIX	IR45	SPLIT	GAS MIX	SPLIT
1-SUFR NO./EXV/ENK	10000000	6000000	23000000	6000000	73000000	10000000	6000000	10000000
2-PRI SOR/FLO CODE	1692	1702	1802	-1402	2002	2102	-2202	2302
3-PRI SPFL TYP 1-3	0	0	0	0	0	0	0	0
4-PRI SPFL TYP 4-6	0	0	0	0	0	2	1700	2
5-SEC SOR/FLO CODE	2	-2200	0	2600	0	0	0	0
6-SEC SPFL TYP 1-3	0	0	0	0	0	0	0	0
7-SEC SPFL TYP 4-6	0	0	0	0	0	0	0	0
9-NEXT COMP/CABIN	2000002	1900002	3000002	2100002	2200002	2300002	2400002	1600002
9-COMP NSTR 1-9	0	0	3000000	200000000	0	0	0	0
10-COMP NSTR 10-18	0	0	0	0	0	0	0	0
11-NCFL/NLFL/NPASS	0	0	0	0	0	0	0	0
12-PRI VISC/DENSITY	0	0	0	0	0	0	0	0
13-PRI OP/DP/OP/DP	0	0	0	0	0	0	0	0
14-SEC VISC/DENSITY	0	0	0	0	0	0	0	0
15-SEC OP/DP/OP/DP	0	0	0	0	0	0	0	0

SUBROUTINE DEPENDENT K ARRAY DATA - - -

KR(19, 16) = 0 KR(19, 17) = 0 KR(19, 18) = 0 KR(19, 16) = 1 KR(21, 17) = 16

KR(21, 18) = 0 KR(21, 19) = 5 KR(21, 20) = 20 KR(21, 17) = 1 KR(21, 17) = 16



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Component No.	SUER.	TYPE	Value
52-EFF SURFED COND	0		0.0
53-COIP QIOTOL LOSS	0		0.0
54-AMBIENT GAS TEMP	0		0.0
55-AMBIENT UA	0		0.0
56-AMB COV Q LOSS	0		0.0
57-AMB WALL TEMP	0		0.0
58-AMB SCRIPT(L)*A	0		0.0
59-AMB PAD Q LOSS	0		0.0
60-STRUCTURE TEMP	0		0.0
61-STRUCTURE KA/X	0		0.0
62-STRUCTURE Q LOSS	0		0.0
63-INSULATION TEMP	0		0.0
64-INSULATION KA/X	0		0.0

SUBROUTINE DEPENDENT V ARRAY DATA --

Component No.	SUER.	TYPE	Value
VR(25, 65)=	0		0
VR(26, 65)=	1.0000		1.0000
VR(27, 68)=	168.30		168.30
VR(27, 73)=	0		0
VR(27, 74)=	0		0
VR(27, 79)=	0		0
VR(27, 84)=	0		0
VR(27, 83)=	0		0
VR(27, 87)=	0		0
VR(27, 93)=	0		0
VR(27, 94)=	0		0
VR(27, 99)=	0		0
VR(28, 68)=	0		0
VR(28, 73)=	0		0
VR(28, 78)=	0		0
VR(28, 83)=	0		0
VR(28, 88)=	0		0
VR(29, 66)=	0		0
VR(29, 68)=	0		0
VR(30, 65)=	1.0000		1.0000
VR(32, 73)=	0		0
VR(32, 79)=	0		0
VR(32, 83)=	0		0
VR(32, 89)=	0		0
VR(32, 93)=	0		0

Component No.	SUER.	TYPE	25 GASHIX	26 SPLIT	27 TANKG	28 PUMP	29 SHGEN	30 SPLIT	31 GASHIX	32 TANKG
1-SUER NO./EXY/EXK	6000000		6000000	10000000	30003000	22000000	27000000	10000000	6000000	30000000
2-FPI SOP/FLO CODE	2902		2902	2502	0	2700	2802	2402	302	3002
3-FPI SPFL TYP 1-3	0		0	0	10000	10000	0	0	0	0
4-FPI SPFL TYP 4-6	0		0	0	0	0	0	0	-1900	0
5-SEC SCR/FLO CODE	2400		2400	2	0	0	0	2	0	0
6-SEC SPFL TYP 1-3	0		0	0	0	0	0	0	0	0
7-SEC SPFL TYP 4-6	0		0	0	0	0	0	0	0	0
8-NEXT COMP/CAETH	2600002		2600002	15000002	28000002	29000002	25000002	32000002	700002	31000002
9-COIP NSTR 1-9	0		0	0	110100000	200000	10000000	0	0	10000000
10-COIP NSTR 10-13	0		0	0	0	0	0	0	0	0
11-NCFL/NLFL/NP/ASS	0		0	0	0	0	0	0	0	0



SVHSER 9503

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START OF STEADY STATE SOLUTION RESULTS

COMP NO	2	CABIN	SUBR NO	1	PRI	SOR	1	SEC	SOR	-13	ELAPSED TIME IN MILLISEC	COMP PASS NO	1	CP=****	PP=	0.0 SEC
VR(1)	9392.2		VR(2)	70.000	VR(3)	14.700	VR(4)	14.700	VR(5)	9292.5	VR(6)	89.700				
VR(7)	.0		VR(8)	.24314	VR(9)	28.857	VR(10)	2046.8	VR(11)	7199.4	VR(12)	46.300				
VR(13)	.0		VR(14)	.0	VR(15)	13.000	VR(16)	70.000	VR(17)	14.700	VR(18)	14.700				
VR(19)	.0		VR(20)	1394.9	VR(21)	70.000	VR(22)	28.876	VR(23)	28.876	VR(24)	303.76				
VR(25)	.0		VR(26)	.0	VR(27)	.0	VR(28)	17318.0	VR(29)	17318.0	VR(30)	17065.0				
VR(31)	1063.7		VR(32)	.0	VR(33)	.0	VR(34)	2.0018	VR(35)	2.0018	VR(36)	254.62				
VR(37)	.0		VR(38)	.0	VR(39)	.0	VR(40)	.0	VR(41)	.0	VR(42)	.0				
VR(43)	.0		VR(44)	.0	VR(45)	.0	VR(46)	.0	VR(47)	.0	VR(48)	.0				
VR(49)	.0		VR(50)	.0	VR(51)	.0	VR(52)	.0	VR(53)	.0	VR(54)	14.700				
VR(55)	.0		VR(56)	.0	VR(57)	.0	VR(58)	.0	VR(59)	.0	VR(60)	50.000				
VR(59)	.0		VR(60)	.0	VR(61)	.0	VR(62)	.0	VR(63)	.0	VR(64)	.0				
VR(65)	.0		VR(66)	.0	VR(67)	.0	VR(68)	.0	VR(69)	.0	VR(70)	.0				
VR(69)	.0		VR(70)	.0	VR(71)	.0	VR(72)	.0	VR(73)	.0	VR(74)	.0				
VR(71)	.0		VR(72)	.0	VR(73)	.0	VR(74)	.0	VR(75)	.0	VR(76)	.0				
VR(73)	.0		VR(74)	.0	VR(75)	.0	VR(76)	.0	VR(77)	.0	VR(78)	.0				
VR(75)	.0		VR(76)	.0	VR(77)	.0	VR(78)	.0	VR(79)	.0	VR(80)	.0				
VR(77)	.0		VR(78)	.0	VR(79)	.0	VR(80)	.0	VR(81)	.0	VR(82)	.0				
VR(79)	.0		VR(80)	.0	VR(81)	.0	VR(82)	.0	VR(83)	.0	VR(84)	.0				
VR(81)	.0		VR(82)	.0	VR(83)	.0	VR(84)	.0	VR(85)	.0	VR(86)	.0				
VR(83)	.0		VR(84)	.0	VR(85)	.0	VR(86)	.0	VR(87)	.0	VR(88)	.0				
VR(85)	.0		VR(86)	.0	VR(87)	.0	VR(88)	.0	VR(89)	.0	VR(90)	.0				
VR(87)	.0		VR(88)	.0	VR(89)	.0	VR(90)	.0	VR(91)	.0	VR(92)	.0				
VR(89)	.0		VR(90)	.0	VR(91)	.0	VR(92)	.0	VR(93)	.0	VR(94)	.0				
VR(91)	.0		VR(92)	.0	VR(93)	.0	VR(94)	.0	VR(95)	.0	VR(96)	.0				
VR(93)	.0		VR(94)	.0	VR(95)	.0	VR(96)	.0	VR(97)	.0	VR(98)	.0				
VR(95)	.0		VR(96)	.0	VR(97)	.0	VR(98)	.0	VR(99)	.0	VR(100)	.0				
VR(97)	.0		VR(98)	.0	VR(99)	.0	VR(100)	.0	VR(101)	.0	VR(102)	.0				
VR(101)	.0		VR(102)	.0	VR(103)	.0	VR(104)	.0	VR(105)	.0	VR(106)	.0				
VR(103)	.0		VR(104)	.0	VR(105)	.0	VR(106)	.0	VR(107)	.0	VR(108)	.0				
VR(109)	.0		VR(110)	.0	VR(111)	.0	VR(112)	.0	VR(113)	.0	VR(114)	.0				
VR(115)	.0		VR(116)	.0	VR(117)	.0	VR(118)	.0	VR(119)	.0	VR(120)	.0				
VR(121)	.0		VR(122)	.0	VR(123)	.0	VR(124)	.0	VR(125)	.0	VR(126)	.0				
VR(127)	.0		VR(128)	.0	VR(129)	.0	VR(130)	.0	VR(131)	.0	VR(132)	.0				
VR(133)	.0		VR(134)	.0	VR(135)	.0	VR(136)	.0	VR(137)	.0	VR(138)	.0				
VR(135)	.0		VR(136)	.0	VR(137)	.0	VR(138)	.0	VR(139)	.0	VR(140)	.0				
VR(145)	.0		VR(146)	.0	VR(147)	.0	VR(148)	.0	VR(149)	.0	VR(150)	.0				
VR(151)	.0		VR(152)	.0	VR(153)	.0	VR(154)	.0	VR(155)	.0	VR(156)	.0				
VR(157)	.0		VR(158)	.0	VR(159)	.0	VR(160)	.0	VR(161)	.0	VR(162)	.0				
VR(163)	.0		VR(164)	.0	VR(165)	.0	VR(166)	.0	VR(167)	.0	VR(168)	.0				
VR(169)	.0		VR(170)	.0	VR(171)	.0	VR(172)	.0	VR(173)	.0	VR(174)	.0				
VR(175)	.0		VR(176)	.0	VR(177)	.0	VR(178)	.0	VR(179)	.0	VR(180)	.0				
VR(181)	.0		VR(182)	.0	VR(183)	.0	VR(184)	.0	VR(185)	.0	VR(186)	.0				
VR(181)	15.000		VR(182)	25003	VR(183)	1.0000	VR(184)	8.0000	VR(185)	74172E-01	VR(186)	44000				
			VR(187)	254507	VR(188)	28.692	VR(189)	74229E-01	VR(190)	44000	VR(191)	14600				
			VR(189)	24495	VR(190)	23.714	VR(191)	8.0000	VR(192)	44000	VR(193)	14600				
			VR(192)	24495	VR(193)	23.714	VR(194)	8.0000	VR(195)	44000	VR(196)	14600				

1 SPACE STATION AIR REVITALIZATION SUBSYSTEM SAHD II DEMONSTRATION MODEL. MISSION TIME: 0. SEC (0.0 HR) DATE: 01/26/85

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XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
4 X      CREW (2)      CREW (1)      FROM CABIN      *****      TO CABIN
5 X      = 8000. CU-FT      NO OF MEN = 3      M= 9392.      *      H= 9346.
6 X      ***** LEN      TOTAL Q      T= 70.0      *      T= 65.1
7 X      = 70.1 F      METABOLIC Q = 450.0 B/HR/MAN      A      *      *
8 X      = 55.5 F      SENSIBLE      = 324.4 B/HR/MAN      A      | SENSIBLE |      A
9 X      = 14.70 PSIA      LATENT      = 125.6 B/HR/MAN      A      | IHX FAN (4) | T= 71.2 | IHX (5) |      A
10 X      = 2.89 PSIA      O2 USAGE      = 0.2200 PPH      AAAAAAAAAAAQ = 2843. | AAAAAAAAAAAQ = -14148. | AAAAAAAAAAAAAAAAAA
11 X      = 2.56 H2O-HG      CO2 PROD      = 0.2592 PPH      -----> |CFM= 2100.1 | ----->
12 X      = 0.063 PPH      FROM
13 X      = 0.000 PPH      M= 1327.      *****
14 X      = 0.000 PPH      *      T= 70.0      *
15 X      = 260. B/HR      A      *      *      *
16 X      = 17065. B/HR      A      *      *      *
17 X      = 260. B/HR      A      *      *      *
18 X      = 644. B/HR      A      *      *      *
19 X      = 129. B/HR      A      *      *      *
20 X      = 59.68 FCT      REL HUMIDITY = 59.68 FCT
21 X
22 X
23 X
24 X
25 X      FROM CABIN
26 X      M= 66.81
27 X      T= 70.0
28 X      A
29 X      A
30 X      A
31 X      A
32 X      A
33 X      A
34 X      A
35 X      A
36 X      A
37 X      A
38 X      A
39 X      A
40 X      A
41 X      A
42 X      A
43 X      A
44 X      A
45 X      A
46 X      A
47 X      A
48 X      A
49 X      A
50 X      A
51 X      A
52 X      A
53 X      A
54 X      A
55 X      A
56 X      A
57 X      A
58 X      A
59 X      A
XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX

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ORIGINAL PAGE IS
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SVHSR 9503

0. SEC (0.0 HR) MISSION TIME: DATE: 01/26/85

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1 SPACE STATION AIR REVITALIZATION SUBSYSTEM SAND II DEMONSTRATION MODEL.
2
3 ***** FROM CABIN TO CABIN *****
4 X M= 9359. M= 9360.
5 X T= 69.5. T= 64.4
6 X
7 X *****
8 X
9 X *****
10 X *****
11 X *****
12 X *****
13 X *****
14 X *****
15 X *****
16 X *****
17 X *****
18 X *****
19 X *****
20 X *****
21 X *****
22 X *****
23 X *****
24 X *****
25 X *****
26 X *****
27 X *****
28 X *****
29 X *****
30 X *****
31 X *****
32 X *****
33 X *****
34 X *****
35 X *****
36 X *****
37 X *****
38 X *****
39 X *****
40 X *****
41 X *****
42 X *****
43 X *****
44 X *****
45 X *****
46 X *****
47 X *****
48 X *****
49 X *****
50 X *****
51 X *****
52 X *****
53 X *****
54 X *****
55 X *****
56 X *****
57 X *****
58 X *****
59 X *****
60 X *****

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SVHSER 9503

CONGRATULATIONS - THE RUN WAS A HOWLING SUCCESS.

NONE OF THE COMPONENTS HAVE FAILURE FLAGS.



SVHSR 9503

ORIGINAL PAGE IS
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COMPONENT NO. =	1	2	3	4	5	6	7	8
SUBTYPE =	SUITS	CABIN	SPLIT	FAN	ANYHX	ALTCOM	ANYHX	ALTCOM
VR								
1-TOTAL FRI FLOW P	9359.93	9359.87	1324.12	9359.54	9359.54	1483.83	1391.16	950.000
2-TEMPATURE R	64.3754	69.5328	69.5328	70.7732	64.4484	60.0000	49.2122	45.0000
3-DUCT OUTLET P I	14.7000	14.7000	14.7000	14.7000	14.7000	50.0000	14.7000	50.0000
4-COMP OUTLET P M	14.7000	14.7000	14.7000	14.7000	14.7000	50.0000	1378.65	.0
5-HM-CO-D FLOW A	9278.05	9277.35	1312.58	9278.01	9278.01	.0	10.2333	.0
6-CO-D VAP FLOW R	81.5399	81.5394	11.5351	81.5362	81.5362	.0	2.28426	.0
7-CO-D LIQ FLOW Y	.0	.0	.0	.0	.0	.0	.243129	.0
8-H-C SP HEAT	.243129	.243129	.243129	.243129	.243129	.0	28.8586	.0
9-N-C SOL HT	28.8601	28.8601	28.8601	28.8601	28.8601	.0	303.751	.0
10-OXYGEN FLOW I	2043.65	2043.73	2043.87	2043.87	2043.87	.0	1067.88	.0
11-DILUENT FLOW D	7185.52	7185.01	1016.55	7185.52	7185.52	.0	7.01553	.0
12-CO2 FLOW E	48.8784	48.6138	6.87801	48.6172	48.6172	.0	.0	.0
13-TRACE CTH FLOW	.0	.0	.0	.0	.0	.0	.0	.0
14-SPCL FLOW 1 D	.0	.0	.0	.0	.0	.0	.0	.0
15-SPCL FLOW 2 A	.0	.0	.0	.0	.0	.0	.0	.0
16-SPCL FLOW 3 T	.0	.0	.0	.0	.0	.0	.0	.0
17-SPCL FLOW 4 A	.0	.0	.0	.0	.0	.0	.0	.0
18-SPCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0
19-SPCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0
20-TOTAL SEC FLOW S	.0	1391.24	66.8540	.0	1483.83	.0	950.000	.0
21-TEMPATURE E	.0	69.5328	69.5328	.0	69.7598	.0	54.5742	.0
22-DUCT OUTLET P C	.0	14.7000	14.7000	.0	50.0000	.0	50.0000	.0
23-COMP OUTLET P O	.0	14.7000	14.7000	.0	50.0000	.0	50.0000	.0
24-NON-CO-D FLOW N	.0	1379.12	66.5336	.0	.0	.0	.0	.0
25-CO-D VAP FLOW D	.0	12.1199	.534705	.0	.0	.0	.0	.0
26-CO-D LIQ FLOW A	.0	.0	.0	.0	.0	.0	.0	.0
27-N-C SP HEAT R	.0	.243129	.243129	.0	.0	.0	.0	.0
28-N-C MOL HT Y	.0	28.8601	28.8601	.0	.0	.0	.0	.0
29-OXYGEN FLOW S	.0	303.609	14.6568	.0	.0	.0	.0	.0
30-DILUENT FLOW I	.0	1068.09	51.5281	.0	.0	.0	.0	.0
31-CO2 FLOW	.0	7.22665	.348640	.0	.0	.0	.0	.0
32-TRACE CTH FLOW D	.0	.0	.0	.0	.0	.0	.0	.0
33-SPCL FLOW 1 E	.0	.0	.0	.0	.0	.0	.0	.0
34-SPCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0
35-SPCL FLOW 3 D	.0	.0	.0	.0	.0	.0	.0	.0
36-SPCL FLOW 4 A	.0	.0	.0	.0	.0	.0	.0	.0
37-SPCL FLOW 5 T	.0	.0	.0	.0	.0	.0	.0	.0
38-SPCL FLOW 6 A	.0	.0	.0	.0	.0	.0	.0	.0
39-OH, C, DP PRI P	.0	.0	.0	.0	.0	.0	.0	.0
40-LE, N, K DUCT R	.0	.0	.0	.0	.0	.0	.0	.0
41-FF AREA E	.0	.0	.0	.0	.0	.0	.0	.0
42-OH, C, DP PRI S	.0	.0	.0	.0	.0	.0	.0	.0
43-LE, N, K COMP S	.0	.0	.0	.0	.0	.0	.0	.0
44-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0
45-OH, C, DP SEC C	.0	.0	.0	.0	.0	.0	.0	.0
46-LE, N, K DUCT O	.0	.0	.0	.0	.0	.0	.0	.0
47-FF AREA E	.0	.0	.0	.0	.0	.0	.0	.0
48-OH, C, DP SEC F	.0	.0	.0	.0	.0	.0	.0	.0
49-LE, N, K COMP F	.0	.0	.0	.0	.0	.0	.0	.0
50-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0
51-COMP SOURCE TEMP	.0	.0	.0	.0	.0	.0	.0	.0



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COMPONENT NO. =	1	2	3	4	5	6	7	8
SUBR. TYPE =	SUITS	CABIN	SPLIT	FAN	ANYHX	ALTCOH	ANYHX	ALTCOH
KR 1-SUER NO./EXV/EXK	2001000	1025000	10000000	23000000	4000000	490000002	4000000	490000000
2-PRI SOR/FLO CODE	502	102	-202	202	402	0	3102	0
3-PRI SPFL TYP 1-3	0	0	0	0	0	10000	0	10000
4-PRI SPFL TYP 4-6	0	0	0	0	0	0	0	0
5-SEC SOR/FLO CODE	0	-1302	2	0	-600	0	-600	0
6-SEC SPFL TYP 1-3	0	0	0	0	10000	0	10000	0
7-SEC SPFL TYP 4-6	0	0	0	0	0	0	0	0
8-NEXT COMP/CABIN	1400002	300002	400002	500002	100002	2	900002	2
9-COMP NSTR 1-9	0	101011000	0	100000000	200000000	0	200000000	0
10-COMP NSTR 10-18	100	0	0	0	100	0	100	0
11-NCFL/HFL/NPASS	10	10	10	10	10	0	10	0
12-PRI VISC/DENSITY	0	0	0	0	0	0	0	0
13-PRI OP/DP/OP/DP	0	0	0	0	0	0	0	0
14-SEC VISC/DENSITY	0	0	0	0	0	0	0	0
15-SEC OP/DP/OP/DP	0	0	0	0	0	0	0	0

SUBROUTINE DEPENDENT K ARRAY DATA - - -
 KRI 1, 16)= 3 KRI 2, 16)= 0
 KRI 4, 18)= 0 KRI 5, 16)= 0



**UNITED
TECHNOLOGIES
HAMILTON
STANDARD**

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COMPONENT NO. =	10	17	18	19	20	21	22	23	24
SUER. TYPE =	KSPAS=	TIME= .0	GASHIX	FAN	GASHIX	IR45	SPLIT	GASHIX	SPLIT
1-TOTAL PRI FLOW P	67.0442	67.0442	67.0442	67.0442	2.55000	.209749	.0	.209749	.209749
2-TEMPERATURE R	59.6547	59.6547	59.6547	69.9042	290.123	70.0000	70.0000	70.0000	70.0000
3-DUCT OUTLET P I	14.7000	14.7000	14.7000	14.7000	29.9997	29.9997	29.9997	29.9997	29.9997
4-COMP OUTLET P M	14.7000	14.7000	14.7000	14.7000	29.9997	29.9997	29.9997	29.9997	29.9997
5-KOH-CO2 FLOW A	66.0618	66.0618	66.0618	66.0618	.0	.209749	.0	.0	.209749
6-CO2 VAP FLOW R	726703	726703	726703	726703	2.55000	.0	.0	.0	.0
7-CO2 LIQ FLOW Y	255697	255697	255697	255697	.0	.0	.0	.0	.0
8-H-C SP HEAT	243266	243266	243266	243266	.0	.0	.0	.0	.0
9-H-C NOL HT	28.6286	28.6286	28.6286	28.6286	.0	.0	.0	.0	.0
10-OXYGEN FLOW I	14.5991	14.5991	14.5991	14.5991	.0	.0	.0	.0	.0
11-DILUENT FLOW D	51.3252	51.3252	51.3252	51.3252	.0	.209749	.0	.209749	.209749
12-CO2 FLOW E	137518	137518	137518	137518	.0	.0	.0	.0	.0
13-TRACE CTH FLOW D	.0	.0	.0	.0	.0	.0	.0	.0	.0
14-SFCL FLOW 1	.0	.0	.0	.0	.0	.0	.0	.0	.0
15-SFCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0	.0
16-SFCL FLOW 3	.0	.0	.0	.0	.0	.0	.0	.0	.0
17-SFCL FLOW 4	.0	.0	.0	.0	.0	.0	.0	.0	.0
18-SFCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0	.0
19-SFCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0	.0
20-TOTAL SEC FLOW S	.0	.0	.0	.0	.0	.0	.209749	.0	.0
21-TEMPERATURE E	59.6547	59.6547	.0	.0	.0	.0	70.0000	.0	70.0000
22-DUCT OUTLET P C	14.7000	14.7000	.0	.0	.0	.0	29.9997	.0	29.9997
23-COMP OUTLET P O	14.7000	14.7000	.0	.0	.0	.0	29.9997	.0	29.9997
24-NON-CO2 FLOW N	.0	.0	.0	.0	.0	.0	.0	.0	.0
25-CO2 VAP FLOW D	.0	.0	.0	.0	.0	.0	.0	.0	.0
26-CO2 LIQ FLOW A	.0	.0	.0	.0	.0	.0	.0	.0	.0
27-H-C SP HEAT	.0	.0	.0	.0	.0	.0	.0	.0	.0
28-H-C NOL HT	.0	.0	.0	.0	.0	.0	.0	.0	.0
29-OXYGEN FLOW	.0	.0	.0	.0	.0	.0	.0	.0	.0
30-DILUENT FLOW S	.0	.0	.0	.0	.0	.0	.0	.0	.0
31-CO2 FLOW I	.0	.0	.0	.0	.0	.0	.0	.0	.0
32-TRACE CTH FLOW D	.0	.0	.0	.0	.0	.0	.0	.0	.0
33-SFCL FLOW 1	.0	.0	.0	.0	.0	.0	.0	.0	.0
34-SFCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0	.0
35-SFCL FLOW 3	.0	.0	.0	.0	.0	.0	.0	.0	.0
36-SFCL FLOW 4	.0	.0	.0	.0	.0	.0	.0	.0	.0
37-SFCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0	.0
38-SFCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0	.0
39-DH, C, DP PRI P	.0	.0	.0	.0	.0	.0	.0	.0	.0
40-LE, N, K DUCT R	.0	.0	.0	.0	.0	.0	.0	.0	.0
41-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0
42-DH, C, DP PRI S	.0	.0	.0	.0	.0	.0	.0	.0	.0
43-LE, N, K COMP S	.0	.0	.0	.0	.0	.0	.0	.0	.0
44-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0
45-DH, C, DP SEC C	.0	.0	.0	.0	.0	.0	.0	.0	.0
46-LE, N, K DUCT O	.0	.0	.0	.0	.0	.0	.0	.0	.0
47-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0
48-DH, C, DP SEC F	.0	.0	.0	.0	.0	.0	.0	.0	.0
49-LE, N, K COMP F	.0	.0	.0	.0	.0	.0	.0	.0	.0
50-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0
51-COMP SOURCE TEMP	.0	.0	.0	.0	.0	.0	.0	.0	.0



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VR(24, 65) = .0

COMPONENT NO. = SUCR. TYPE =	17 SPLIT	18 GASHIX	19 FAN	20 GASHIX	21 IR45	22 SPLIT	23 GASHIX	24 SPLIT
KR 1-SUCR NO./ENV/EXK	10000000	6000000	23000000	6000000	73000000	10000000	6000000	10000000
2-PRI SOR/FLO CODE	1602	1702	1802	-1402	2002	2102	-2202	2302
3-PRI SFLL TYP 1-3	0	0	0	0	0	0	0	0
4-PRI SFLL TYP 4-6	0	0	0	0	0	0	0	0
5-SEC SOR/FLO CODE	2	-2200	0	2600	0	2	1700	2
6-SEC SFLL TYP 1-3	0	0	0	0	0	0	0	0
7-SEC SFLL TYP 4-6	0	0	0	0	0	0	0	0
8-REXT COMP/CADIN	20000002	19000002	30000002	21000002	22000002	23000002	24000002	18000002
9-COMP NSTR 1-9	0	0	30000000	200000000	0	0	0	0
10-COMP NSTR 10-18	0	0	0	0	0	0	0	0
11-NCFL/NLFL/NFASS	10	10	10	10	10	10	10	10
12-PRI VISC/DENSITY	0	0	0	0	0	0	0	0
13-PRI OP/DP/OP/DP	0	0	0	0	0	0	0	0
14-SEC VISC/DENSITY	0	0	0	0	0	0	0	0
15-SEC OP/DP/OP/DP	0	0	0	0	0	0	0	0

SUBROUTINE DEPENDENT K ARRAY DATA - - -

KR(19, 16) = 0 KR(19, 17) = 0 KR(21, 16) = 1 KR(21, 17) = 16
 KR(21, 18) = 0 KR(21, 19) = 5 KR(21, 20) = 20 KR(21, 21) = 0

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	25	26	27	28	29	30	31	32
	GAS MIX	SPLIT	TANKG	PUMP	SMGEN	SPLIT	GAS MIX	TANKG
52-EFF SUMMED COND	.0	.0	.0	.0	.0	.0	.0	.0
53-COMP OTIOL LOSS	.0	.0	.0	.0	.0	.0	.0	.0
54-MICENT GAS TEMP	.0	.0	.0	.0	.0	.0	.0	.0
55-MICENT UA	.0	.0	.0	.0	.0	.0	.0	.0
56-AIR COMV Q LOSS	.0	.0	.0	.0	.0	.0	.0	.0
57-AIR HALL TEMP	.0	.0	.0	.0	.0	.0	.0	.0
58-AIR SCRIPT(F)A	.0	.0	.0	.0	.0	.0	.0	.0
59-AIR R-0 Q LOSS	.0	.0	.0	.0	.0	.0	.0	.0
60-STRUCTURE TEMP	.0	.0	.0	.0	.0	.0	.0	.0
61-STRUCTURE KAX	.0	.0	.0	.0	.0	.0	.0	.0
62-STRUCTURE Q LOSS	.0	.0	.0	.0	.0	.0	.0	.0
63-IRCULATION TEMP	.0	.0	.0	.0	.0	.0	.0	.0
64-IRCULATION KAX	.0	.0	.0	.0	.0	.0	.0	.0

	25	26	27	28	29	30	31	32
	GAS MIX	SPLIT	TANKG	PUMP	SMGEN	SPLIT	GAS MIX	TANKG
VR(25, 65)=	250.12	1.0000	VR(27, 65)=	70.000	VR(27, 66)=	.0	VR(27, 67)=	.0
VR(27, 69)=	159.30	160.30	VR(27, 70)=	70.000	VR(27, 71)=	2.6971	VR(27, 72)=	30.000
VR(27, 73)=	.0	.0	VR(27, 75)=	.0	VR(27, 76)=	.0	VR(27, 77)=	.0
VR(27, 79)=	.0	.0	VR(27, 80)=	.0	VR(27, 81)=	.0	VR(27, 82)=	.0
VR(27, 83)=	.0	.0	VR(27, 85)=	.0	VR(27, 86)=	.0	VR(27, 87)=	.0
VR(27, 89)=	1.0000	62.400	VR(27, 90)=	2.4200	VR(27, 91)=	18.016	VR(27, 92)=	.0
VR(27, 93)=	.0	.0	VR(27, 95)=	.0	VR(27, 96)=	.0	VR(27, 97)=	-2.5500
VR(28, 69)=	.0	.0	VR(28, 71)=	.0	VR(28, 72)=	.0	VR(28, 73)=	.0
VR(28, 72)=	.0	.0	VR(28, 74)=	.0	VR(28, 75)=	.0	VR(28, 76)=	.0
VR(28, 77)=	.0	.0	VR(28, 79)=	1.0000	VR(28, 80)=	.0	VR(28, 81)=	.0
VR(28, 83)=	.0	.0	VR(29, 84)=	.0	VR(29, 85)=	10.000	VR(29, 86)=	.0
VR(29, 82)=	.0	.0	VR(29, 87)=	851.20	VR(29, 88)=	.0	VR(29, 89)=	.0
VR(29, 92)=	40.000	250.12	VR(29, 93)=	.0	VR(29, 94)=	.0	VR(32, 67)=	.0
VR(30, 69)=	.0	54.510	VR(32, 65)=	70.000	VR(32, 66)=	.0	VR(32, 68)=	30.000
VR(32, 73)=	4.6436	4.6436	VR(32, 69)=	.0	VR(32, 70)=	2.0000	VR(32, 71)=	44.010
VR(32, 78)=	.0	.0	VR(32, 75)=	.0	VR(32, 76)=	.0	VR(32, 77)=	.0
VR(32, 83)=	.0	.0	VR(32, 80)=	4.6436	VR(32, 81)=	.0	VR(32, 82)=	.0
VR(32, 89)=	20.000	.23218	VR(32, 85)=	.0	VR(32, 86)=	.0	VR(32, 87)=	.0
VR(32, 93)=	.0	.0	VR(32, 90)=	4.4000	VR(32, 91)=	44.010	VR(32, 92)=	.0
VR(32, 95)=	.0	.0	VR(32, 95)=	.0	VR(32, 96)=	.0	VR(32, 97)=	.0

COMPONENT NO. =	25	26	27	28	29	30	31	32
SUER. TYPE =	GAS MIX	SPLIT	TANKG	PUMP	SMGEN	SPLIT	GAS MIX	TANKG
1-SUER NO./EXV/EXK	6000000	1000000	30003000	22000000	27000000	10000000	6000000	30000001
2-FPI SOR/FLO CODE	2902	2502	.0	2700	2802	2402	302	3002
3-FPI SFPL TYP 1-3	0	0	10000	10000	0	0	0	0
4-FPI SPFL TYP 4-6	0	0	0	0	0	0	0	0
5-SEC SOR/FLO CODE	2400	2	0	0	0	2	-1900	0
6-SEC SFPL TYP 1-3	0	0	0	0	0	0	0	0
7-SEC SPFL TYP 4-6	0	0	0	0	0	0	0	0
8-HEXT COMP/CABIN	2600002	1500002	2800002	2900002	2500002	3200002	700002	3100002
9-COMP HSTR 1-9	0	0	110100000	200000	10000000	0	0	10000000
10-COMP HSTR 10-19	0	0	0	0	0	0	0	0
11-NCFL/NLFL/NPASS	10	10	10	10	10	10	10	10

BEGINNING OF TRANSIENT CASE

ESCM: BASELINE, VOL = 8000 FT-3, PC02 = 2.5, .275 PPH AVERAGE

COMP NO 12 FAN		SUBR NO 23		PRI SOR 11		SEC SOR 0		COMP PASS NO 1		TIME = 15.0 SEC	
VR(1)= 1394.3		FAILURE FLAGS -- COMP= 1		VR(3)= 14.700		LOOP= 0		ELAPSED TIME IN MILLISEC		465 PP= 0	
VR(7)= .0	VR(2)= 50.338	VR(8)= .24295	VR(9)= 28.901	VR(10)= 14.700	VR(4)= 14.700	VR(5)= 1384.2	VR(6)= 10.137	VR(11)= 1067.6	VR(12)= 12.909	VR(13)= .0	VR(14)= 10.137
VR(13)= .0	VR(14)= .0	VR(15)= .0	VR(16)= .0	VR(17)= .0	VR(18)= .0	VR(19)= .0	VR(20)= .0	VR(21)= .0	VR(22)= .0	VR(23)= .0	VR(24)= .0
VR(65)= 477.82	VR(66)= .0	VR(67)= .0	VR(68)= .0	VR(69)= .0	VR(70)= .0	VR(71)= .0	VR(72)= .0	VR(73)= .0	VR(74)= .0	VR(75)= .0	VR(76)= 300.00
VR(71)= .0	VR(72)= .0	VR(73)= .0	VR(74)= .0	VR(75)= .0	VR(76)= .0	VR(77)= .0	VR(78)= .0	VR(79)= .0	VR(80)= .0	VR(81)= .0	VR(82)= .0
VR(77)= .0	VR(78)= .0	VR(79)= .0	VR(80)= .0	VR(81)= .0	VR(82)= .0	VR(83)= .0	VR(84)= .0	VR(85)= .0	VR(86)= .0	VR(87)= .0	VR(88)= .0
VR(83)= .0	VR(84)= .0	VR(85)= .0	VR(86)= .0	VR(87)= .0	VR(88)= .0	VR(89)= .0	VR(90)= .0	VR(91)= 140.00	VR(92)= .0	VR(93)= .0	VR(94)= .0
VR(89)= .0	CPS= .24442	VR(90)= .0	VR(91)= .0	VR(92)= .0	VR(93)= .0	VR(94)= .0	VR(95)= .0	RHOP= .77251E-01	VR(96)= .0	VR(97)= .0	VR(98)= .0
								MTMS= .0	VISCP= .44000	XKP= .14600	
									VISCS= .0	XKS= .0	



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MISSION TIME: 3615. SEC (1.00 HR) DATE: 01/26/85

1 SPACE STATION AIR REVITALIZATION SUBSYSTEM SAND II DEMONSTRATION MODEL. *****

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TO CABIN
M= 9357.
T= 69.4

FROM CABIN
M= 9357.
T= 69.4

CABIN (1)
NO OF MEN = 3
TOTAL Q = 1561.6 B/HR
METABOLIC Q = 520.5 B/HR/HAN
SENSIBLE = 330.6 B/HR/HAN
LATENT = 189.9 B/HR/HAN
O2 USAGE = 0.2545 PPH
CO2 PROD = 0.2998 PPH

CABIN (2)
VOLUME = 8000. CU-FT
AIR MASS = 594.07 LEM
TEMP = 69.4 F
DEW PT = 51.2 F
TOTAL PRESS = 14.69 PSIA
O2 PRESS = 2.99 PSIA
CO2 PRESS = 2.58 MM-HG
GAS LEAKAGE = 0.083 PPH
O2 MAKEUP = 0.000 PPH
H2 MAKEUP = 0.000 PPH
NON ECLSS Q = 17065. B/HR
SENSIBLE = 255. B/HR
LATENT = 5401. B/HR
ECLSS Q = 561. B/HR
REL HUMIDITY = 51.95 PCT

REL. HUMD. = 1389.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 950.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
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CFM = 300.

REL. HUMD. = 1390.
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CFM = 15.

REL. HUMD. = 1390.
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CFM = 2100.

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CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.

REL. HUMD. = 1390.
HX FAN (4) = 70.7.
CFM = 2100.

REL. HUMD. = 1391.
HX FAN (12) = 478.
CFM = 300.

REL. HUMD. = 1390.
HX FAN (7) = 877.
CFM = 15.



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ESCH DEMONSTRATION MODEL

PLOT0	2 181	MISSION TIME (SEC)
PLOT1	2 182	MISSION TIME (MIN)
PLOT2	1 66	CREWMAN SEN (BTU/HR)
PLOT2	1 67	CREWMAN LAT (BTU/HR)
PLOT2	1 69	O2 USE RATE (LB/HR)
PLOT2	1 69	CO2 GEN RATE (LB/HR)
PLOT2	1 62	CREWMAN MET (BTU/HR)
PLOT2	2 89	REL HUMIDITY (DEC)
PLOT2	2 94	O2 PRESSURE (PSIA)
PLOT2	2 95	N2 PRESSURE (PSIA)
PLOT2	2 99	DEW POINT TEMP (F)
PLOT2	2 100	CO2 PRESS (MM HG)
PLOT2	2 104	DRY BULB TEMP (F)
PLOT2	2 106	TOTAL PRESS (PSIA)
PLOT2	2 165	O2 MAKEUP (LB/HR)
PLOT2	2 166	N2 MAKEUP (LB/HR)
PLOT2	15 6	SA-1 H2O IN (LB/HR)
PLOT2	16 6	SA-1 H2O OUT (LB/HR)
PLOT2	15 12	SA-1 CO2 IN (LB/HR)
PLOT2	16 12	SA-1 CO2 OUT (LB/HR)
PLOT2	16 82	SA-1 EXIT TEMP (F)
PLOT2	16 83	SA-1 H2O LOAD(LB/LB)
PLOT2	16 83	SA-1 CO2 LOAD(LB/LB)
PLOT2	20 6	SA-2 H2O IN (LB/HR)
PLOT2	21 6	SA-2 H2O OUT (LB/HR)
PLOT2	20 12	SA-2 CO2 IN (LB/HR)
PLOT2	21 12	SA-2 CO2 OUT (LB/HR)
PLOT2	21 2	SA-2 EXIT TEMP (F)
PLOT2	21 82	SA-2 H2O LOAD(LB/LB)
PLOT2	21 83	SA-2 CO2 LOAD(LB/LB)
PLOT2	21 101	BED 2, SEGMENT 1, TEMP
PLOT2	21 131	BED 2, SEGMENT 2
PLOT2	21 131	BED 2, SEGMENT 3
PLOT2	21 161	BED 2, SEGMENT 4
PLOT2	21 191	BED 2, SEGMENT 5
PLOT2	21 221	BED 2, SEGMENT 1, H2O LOAD
PLOT2	21 126	BED 2, SEGMENT 2
PLOT2	21 155	BED 2, SEGMENT 3
PLOT2	21 156	BED 2, SEGMENT 4
PLOT2	21 216	BED 2, SEGMENT 5
PLOT2	21 246	BED 2, SEGMENT 1, CO2 LOAD
PLOT2	21 125	BED 2, SEGMENT 2
PLOT2	21 155	BED 2, SEGMENT 3
PLOT2	21 185	BED 2, SEGMENT 4
PLOT2	21 215	BED 2, SEGMENT 5
PLOT2	21 245	

5000 LOCATIONS ALLOTTED IN MAIN PROGRAM (G189) FOR K AND V ARRAY
THE RECOMMENDED MINIMUM IS 5000 FOR THE K AND V ARRAY

2029 LOCATIONS USED FOR COMP. K AND V DATA

2447 IS LAST LOCATION USED FOR TABLE DATA

THERE ARE 2553 UNUSED K AND V ARRAY LOCATIONS



**UNITED
TECHNOLOGIES**
HAMILTON
STANDARD

SVHSER 9503

EDITED COMPONENT DATA AT BEGINNING OF STEADY STATE

ESCH1: BASELINE, VOL = 8000 FT-3, PCO2 = 2.5, .275 PPH AVERAGE

IFM CLOCK TIME(HH-MM-SS) = 15:57:53



1 SPACE STATION AIR REVITALIZATION SUBSYSTEM SAND II DEMONSTRATION MODEL. MISSION TIME: 72015. SEC (20.00 HR) DATE: 01/26/85

2 XXX	X
3 XXX	X
4 X	TO CABIN
5 X	M= 9367.
6 X	T= 64.6
7 X	A
8 X	*****
9 X	* * * * *
10 X	*****
11 X	* * * * *
12 X	*****
13 X	* * * * *
14 X	*****
15 X	* * * * *
16 X	*****
17 X	* * * * *
18 X	*****
19 X	* * * * *
20 X	*****
21 X	* * * * *
22 X	*****
23 X	* * * * *
24 X	*****
25 X	* * * * *
26 X	*****
27 X	* * * * *
28 X	*****
29 X	* * * * *
30 X	*****
31 X	*****
32 X	*****
33 X	*****
34 X	*****
35 X	*****
36 X	*****
37 X	*****
38 X	*****
39 X	*****
40 X	*****
41 X	*****
42 X	*****
43 X	*****
44 X	*****
45 X	*****
46 X	*****
47 X	*****
48 X	*****
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58 X	*****
59 X	*****
60 X	*****

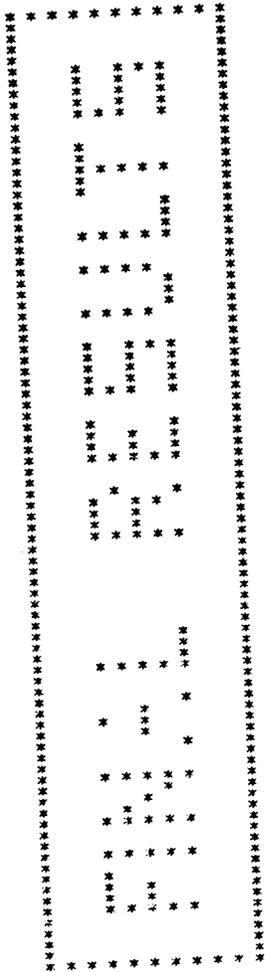


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1 SPACE STATION AIR REVITALIZATION SUBSYSTEM SAVID II DEMONSTRATION MODEL. MISSION TIME: 79215. SEC (22.00 HR) DATE: 01/26/85

3
4 X CABIN (2) ... CRCH (1)
5 X TO CABIN
6 X FROM CABIN
7 X H2O OF MEN = 3
8 X TOTAL Q = 900.0 B/HR
9 X METABOLIC Q = 300.0 B/HR/MAN
10 X SENSIBLE IHX FAN (4) T= 70.4
11 X LATENT IHX FAN (5)
12 X CO2 PRODUCTION = 0.1467 PPH
13 X CO2 LEAKAGE = 0.083 PPH
14 X O2 MAKEUP = 0.000 PPH
15 X O2 MAKEUP = 0.000 PPH
16 X NON ECLSS Q: = 17065. B/HR
17 X SENSIBLE = 5495. B/HR
18 X LATENT = 420. B/HR
19 X REL HUMIDITY = 50.70 PCT
20 X FROM CABIN
21 X M= 1326.
22 X T= 69.2
23 X FROM CABIN
24 X M= 1393.
25 X T= 70.0
26 X REL HUMID. = 1351.
27 X T= 48.9
28 X VAAQ = 13. |AAA T= 50.2
29 X ICFM = 9. |
30 X FROM CABIN
31 X M= 67.19
32 X T= 86.6
33 X M= 950.
34 X T= 45.0
35 X FROM CABIN
36 X M= 171.
37 X T= 15.
38 X FROM CABIN
39 X M= 0.0
40 X T= 290.3
41 X H2O INTERFACE
42 X M= 20.574
43 X M= 1.73
44 X T= 70.0
45 X FROM CABIN
46 X M= 67.07
47 X T= 69.2
48 X ICFM = 1956. |
49 X M= 34. |
50 X T= 70.0
51 X FROM CABIN
52 X M= 9336.
53 X T= 69.2
54 X FROM CABIN
55 X M= 9336.
56 X T= 65.1
57 X FROM CABIN
58 X M= 1395.
59 X T= 50.3
60 X FROM CABIN
61 X M= 1225.
62 X T= 60.0
63 X FROM CABIN
64 X M= 1392.
65 X T= 48.9
66 X FROM CABIN
67 X M= 0.0
68 X T= 172.7
69 X FROM CABIN
70 X M= 0.0
71 X T= 172.7
72 X FROM CABIN
73 X M= 0.0
74 X T= 172.7
75 X FROM CABIN
76 X M= 0.0
77 X T= 172.7
78 X FROM CABIN
79 X M= 0.0
80 X T= 172.7
81 X FROM CABIN
82 X M= 0.0
83 X T= 172.7
84 X FROM CABIN
85 X M= 0.0
86 X T= 172.7
87 X FROM CABIN
88 X M= 0.0
89 X T= 172.7
90 X FROM CABIN
91 X M= 0.0
92 X T= 172.7
93 X FROM CABIN
94 X M= 0.0
95 X T= 172.7
96 X FROM CABIN
97 X M= 0.0
98 X T= 172.7
99 X FROM CABIN
100 X M= 0.0
101 X T= 172.7



ESCM: BASELINE, VOL = 8000 FT-3, PCO2 = 2.5, .275 PPH AVERAGE



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SVHSER 9503

COMPONENT SOLUTION RESULTS AT END OF TRANSIENT, TIME = 86400.0 SEC SYSTEM PASS = 5760

ESCH: BASELINE, VOL = 8000 FT-3, PCO2 = 2.5, .275 PPH AVERAGE



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SVHSER 9503

ORIGINAL PAGE IS
OF POOR QUALITY

COMPONENT NO. =	1	2	3	4	5	6	7	8
SUBJ. TYPE =	SUITS	CABIN	SPLIT	FAN	ANYHX	ALTCOM	ANYHX	ALTCOM
VR								
1-TOTAL FRI FLOW P	9391.99	9388.71	1326.52	9391.59	9391.59	1438.53	1393.77	950.000
2-TEMPERATURE R	64.9568	69.4055	69.4055	70.6439	64.5301	60.0000	48.9429	45.0000
3-DUCT OUTLET P I	14.7228	14.7228	14.7228	14.7228	14.7228	50.0000	14.7228	50.0000
4-COMP OUTLET P H	14.7228	14.7228	14.7228	14.7228	14.7228	50.0000	14.7228	50.0000
5-NHP-CO2 FLOW A	9319.47	9316.53	1316.33	9319.43	9319.43	.0	1382.62	.0
6-CO2 VAP FLOW R	72.1513	72.1405	10.1927	72.1626	72.1626	.0	10.1305	.0
7-CO2 LIQ FLOW Y	.0	.0	.0	.0	.0	.0	1.02096	.0
8-H-C SP HEAT	.242897	.242898	.242898	.242898	.242898	.0	.242896	.0
9-H-C FOL HT	28.8393	28.8395	20.6896	28.8396	28.8396	.0	28.8876	.0
10-OXYGEN FLOW I	2129.63	2129.44	300.726	2129.10	2129.10	.0	315.933	.0
11-DILUENT FLOW D	7142.16	7139.97	1008.80	7142.16	7142.16	.0	1059.81	.0
12-CO2 FLOW E	48.4414	48.1675	6.80554	48.1823	48.1823	.0	6.87158	.0
13-TRACE CTH FLOW	.0	.0	.0	.0	.0	.0	.0	.0
14-SFCL FLOW 1	.0	.0	.0	.0	.0	.0	.0	.0
15-SFCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0
16-SFCL FLOW 3	.0	.0	.0	.0	.0	.0	.0	.0
17-SFCL FLOW 4	.0	.0	.0	.0	.0	.0	.0	.0
18-SFCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0
19-SFCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0
20-TOTAL SEC FLOW S	.0	1395.46	67.0828	.0	1438.53	.0	950.000	.0
21-TEMPERATURE E	.0	69.4055	69.4055	.0	69.7442	.0	53.8414	.0
22-DUCT OUTLET P C	.0	14.7228	14.7228	.0	50.0000	.0	50.0000	.0
23-COMP OUTLET P O	.0	14.7228	14.7228	.0	50.0000	.0	50.0000	.0
24-NHP-CO2 FLOW N	.0	1384.74	68.4081	.0	.0	.0	.0	.0
25-CO2 VAP FLOW D	.0	10.7224	.529700	.0	.0	.0	.0	.0
26-CO2 LIQ FLOW A	.0	.0	.0	.0	.0	.0	.0	.0
27-H-C SP HEAT	.0	.242897	.242897	.0	.0	.0	.0	.0
28-H-C FOL HT	.0	28.8396	28.8396	.0	.0	.0	.0	.0
29-OXYGEN FLOW	.0	316.354	15.6284	.0	.0	.0	.0	.0
30-DILUENT FLOW S	.0	1061.23	52.4261	.0	.0	.0	.0	.0
31-CO2 FLOW I	.0	7.15921	.353676	.0	.0	.0	.0	.0
32-TRACE CTH FLOW D	.0	.0	.0	.0	.0	.0	.0	.0
33-SFCL FLOW 1	.0	.0	.0	.0	.0	.0	.0	.0
34-SFCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0
35-SFCL FLOW 3	.0	.0	.0	.0	.0	.0	.0	.0
36-SFCL FLOW 4	.0	.0	.0	.0	.0	.0	.0	.0
37-SFCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0
38-SFCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0
39-DH, C, DP PRI P	.0	.0	.0	.0	.0	.0	.0	.0
40-LE, H, K DUCT R	.0	.0	.0	.0	.0	.0	.0	.0
41-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0
42-DH, C, DP PPI S	.0	.0	.0	.0	.0	.0	.0	.0
43-LE, H, K COMP S	.0	.0	.0	.0	.0	.0	.0	.0
44-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0
45-DH, C, DP SEC C	.0	.0	.0	.0	.0	.0	.0	.0
46-LE, H, K DUCT O	.0	.0	.0	.0	.0	.0	.0	.0
47-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0
48-DH, C, DP SEC F	.0	.0	.0	.0	.0	.0	.0	.0
49-LE, H, K COMP F	.0	.0	.0	.0	.0	.0	.0	.0
50-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0
51-COMP SOURCE TEMP	.0	.0	.0	.0	.0	.0	.0	.0



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COMPONENT NO. =	1	2	3	4	5	6	7	8
SUBR. TYPE =	SUITS	CABIN	SPLIT	FAN	ANYHX	ALTCOM	ANYHX	ALTCOM
KR 1-SUER NO./EXV/EXK	2001000	1025000	10000000	23000000	4000000	49000000	4000000	49000000
2-PRI SOR/FLO CODE	502	102	-202	202	402	0	3102	0
3-PRI SPFL TYP 1-3	0	0	0	0	0	10000	0	10000
4-PRI SPFL TYP 4-6	0	0	0	0	0	0	0	0
5-SEC SOR/FLO CODE	0	-1302	2	0	-600	0	-800	0
6-SEC SPFL TYP 1-3	0	0	0	0	10000	0	10000	0
7-SEC SPFL TYP 4-6	0	0	0	0	0	0	0	0
8-HEXT COMP/CABIN	1400002	300002	400002	500002	100002	2	900002	2
9-COMP NSTR 1-9	0	101011000	0	100000000	200000000	0	200000000	0
10-COMP NSTR 10-10	100	0	0	0	100	0	100	0
11-NCFL/HFL/NPASS	5760	5760	5760	5760	5760	0	5760	0
12-PRI VISC/DENSITY	0	0	0	0	0	0	0	0
13-PRI OP/DP/OP/DP	0	0	0	0	0	0	0	0
14-SEC VISC/DENSITY	0	0	0	0	0	0	0	0
15-SEC OP/DP/OP/DP	0	0	0	0	0	0	0	0

SUBROUTINE DEPENDENT K ARRAY DATA - - -

KR(1, 16) =	3	KR(2, 16) =	0	KR(2, 17) =	0	KR(4, 16) =	0	KR(4, 17) =	0
KR(4, 18) =	0	KR(5, 16) =	0	KR(6, 16) =	0	KR(6, 17) =	0	KR(7, 16) =	0



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	9, 65)=	9, 70)=	9, 71)=	9, 66)=	30000E-01	9, 67)=	1.0000	VR(9, 68)=	30000E-01	VR(9, 69)=	30000E-01
52-EFF SUMMED COND	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
53-COMP Q1010L LOSS	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
54-ARRIVENT GAS TEMP	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
55-ALUMINUM OA	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
56-ALU CRW Q LOSS	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
57-AMB HALL TEMP	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
58-ALU SCPIPT(F)A	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
59-AMB RAD Q LOSS	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
60-STRUCTURE TEMP	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
61-STRUCTURE KAZX	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
62-STRUCTURE Q LOSS	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
63-INSULATION TEMP	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0
64-INSULATION KAZX	.0	.0	.0	.0	.0	.0	.0	VR(.0	.0	VR(.0	.0

SUBROUTINE DEPENDENT V ARRAY DATA

VR(9, 65)=	9, 70)=	9, 71)=	9, 66)=	30000E-01	9, 67)=	1.0000	VR(9, 68)=	30000E-01	VR(9, 69)=	30000E-01
VR(9, 65)=	.0	.0	.0	.0	.0	.0	.0	VR(10, 65)=	13.106	.0	VR(10, 66)=	.0	.0
VR(10, 67)=	.30000E-01	.0	.0	.0	.0	.0	.0	VR(12, 66)=	.0	.0	VR(12, 67)=	.0	.0
VR(12, 68)=	1.0210	.0	.0	.0	.0	.0	.0	VR(12, 71)=	.0	.0	VR(12, 72)=	.0	.0
VR(12, 73)=	.0	.0	.0	.0	.0	.0	.0	VR(12, 76)=	300.00	.0	VR(12, 77)=	.0	.0
VR(12, 78)=	.0	.0	.0	.0	.0	.0	.0	VR(12, 81)=	.0	.0	VR(12, 82)=	.0	.0
VR(12, 79)=	.0	.0	.0	.0	.0	.0	.0	VR(12, 86)=	.0	.0	VR(12, 87)=	.0	.0
VR(12, 80)=	.0	.0	.0	.0	.0	.0	.0	VR(12, 91)=	140.00	.0	VR(12, 92)=	.0	.0
VR(12, 81)=	1.0000	.0	.0	.0	.0	.0	.0	VR(15, 65)=	247.63	.0	VR(16, 65)=	1270.0	.0
VR(12, 82)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 69)=	15.000	.0	VR(16, 70)=	-1544.3	.0
VR(13, 65)=	45.845	.0	.0	.0	.0	.0	.0	VR(16, 74)=	1.5000	.0	VR(16, 75)=	40000	.0
VR(16, 67)=	32.700	.0	.0	.0	.0	.0	.0	VR(16, 79)=	7.4000	.0	VR(16, 80)=	2.7156	.0
VR(16, 72)=	4.5669	.0	.0	.0	.0	.0	.0	VR(16, 84)=	.0	.0	VR(16, 85)=	180.00	.0
VR(16, 77)=	70.000	.0	.0	.0	.0	.0	.0	VR(16, 89)=	.0	.0	VR(16, 90)=	.10000E+06	.0
VR(16, 82)=	.31848	.0	.0	.0	.0	.0	.0	VR(16, 94)=	.33000	.0	VR(16, 95)=	.106400E-02	.0
VR(16, 87)=	240.00	.0	.0	.0	.0	.0	.0	VR(16, 99)=	.0	.0	VR(16, 100)=	.106400E-02	.0
VR(16, 92)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 104)=	.45238E-07	.0	VR(16, 105)=	.43517E-24	.0
VR(16, 97)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 109)=	.12665E-24	.0	VR(16, 110)=	.0	.0
VR(16, 102)=	14.700	.0	.0	.0	.0	.0	.0	VR(16, 114)=	.0	.0	VR(16, 115)=	.0	.0
VR(16, 107)=	.20000	.0	.0	.0	.0	.0	.0	VR(16, 119)=	243.95	.0	VR(16, 120)=	.12277E-02	.0
VR(16, 112)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 124)=	.0	.0	VR(16, 125)=	.0	.0
VR(16, 117)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 129)=	.0	.0	VR(16, 130)=	.10693E-02	.0
VR(16, 122)=	1.7000	.0	.0	.0	.0	.0	.0	VR(16, 134)=	.0	.0	VR(16, 135)=	.10604E-02	.0
VR(16, 127)=	.94000E-01	.0	.0	.0	.0	.0	.0	VR(16, 139)=	.14944E-24	.0	VR(16, 140)=	.50157E-24	.0
VR(16, 132)=	14.700	.0	.0	.0	.0	.0	.0	VR(16, 144)=	.0	.0	VR(16, 145)=	.0	.0
VR(16, 137)=	.20000	.0	.0	.0	.0	.0	.0	VR(16, 149)=	.0	.0	VR(16, 150)=	.15475E-02	.0
VR(16, 142)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 154)=	243.91	.0	VR(16, 155)=	.0	.0
VR(16, 147)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 159)=	.0	.0	VR(16, 160)=	.10916E-02	.0
VR(16, 152)=	1.7000	.0	.0	.0	.0	.0	.0	VR(16, 164)=	.0	.0	VR(16, 165)=	.10904E-02	.0
VR(16, 157)=	.94000E-01	.0	.0	.0	.0	.0	.0	VR(16, 169)=	.11441E-05	.0	VR(16, 170)=	.53045E-21	.0
VR(16, 162)=	14.700	.0	.0	.0	.0	.0	.0	VR(16, 174)=	.0	.0	VR(16, 175)=	.0	.0
VR(16, 167)=	.20000	.0	.0	.0	.0	.0	.0	VR(16, 179)=	.0	.0	VR(16, 180)=	.26893E-02	.0
VR(16, 172)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 184)=	245.47	.0	VR(16, 185)=	.0	.0
VR(16, 177)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 189)=	.0	.0	VR(16, 190)=	.15302E-02	.0
VR(16, 182)=	1.7000	.0	.0	.0	.0	.0	.0	VR(16, 194)=	.0	.0	VR(16, 195)=	.10031E-02	.0
VR(16, 187)=	.94000E-01	.0	.0	.0	.0	.0	.0	VR(16, 199)=	.52706E-03	.0	VR(16, 200)=	.18143E-16	.0
VR(16, 192)=	14.700	.0	.0	.0	.0	.0	.0	VR(16, 204)=	.54055E-17	.0	VR(16, 205)=	.0	.0
VR(16, 197)=	.20000	.0	.0	.0	.0	.0	.0	VR(16, 209)=	.0	.0	VR(16, 210)=	.55183E-01	.0
VR(16, 202)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 214)=	171.39	.0	VR(16, 215)=	.0	.0
VR(16, 207)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 219)=	.16584E-01	.0	VR(16, 220)=	.27912E-02	.0
VR(16, 212)=	1.7000	.0	.0	.0	.0	.0	.0	VR(16, 224)=	.0	.0	VR(16, 225)=	.21336E-03	.0
VR(16, 217)=	.94000E-01	.0	.0	.0	.0	.0	.0	VR(16, 229)=	.25779E-02	.0	VR(16, 230)=	.64933E-15	.0
VR(16, 222)=	14.700	.0	.0	.0	.0	.0	.0	VR(16, 234)=	.0	.0	VR(16, 235)=	.0	.0
VR(16, 227)=	.20000	.0	.0	.0	.0	.0	.0	VR(16, 239)=	.161.40	.0	VR(16, 240)=	.77787E-01	.0
VR(16, 232)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 244)=	.0	.0	VR(16, 245)=	.0	.0
VR(16, 237)=	.0	.0	.0	.0	.0	.0	.0	VR(16, 249)=	161.40	.0	VR(16, 250)=	.0	.0



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ORIGINAL PAGE IS
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COMPONENT NO. =	5760	TIME =	66400.0	17	19	20	21	22	23	24
SUCC. TYPE =				SPLIT	GASHIX	FAN	IR45	SPLIT	GASHIX	SPLIT
1-TOTAL PRI FLOW P	R	.0	67.2456	.0	67.0628	67.2456	67.2456	67.2456	.0	.0
2-TEMPERATURE	R	157.310	79.6027	157.310	69.4055	79.6027	79.6027	79.6027	157.013	157.013
3-DUCT OUTLET P	I	28.4045	14.7228	14.7228	14.7228	14.7228	14.7228	14.7228	14.7228	14.7228
4-COMP OUTLET P	M	28.4045	14.7228	14.7228	14.7228	14.7228	14.7228	14.7228	14.7228	14.7228
5-NON-CO2 FLOW A	R	.0	66.2868	66.2868	66.5674	66.2868	66.2868	66.2868	.0	.0
6-CO2 VAP FLOW R	A	.0	.958824	.958824	.515447	.958824	.958824	.958824	.0	.0
7-CO2 LIQ FLOW Y	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
8-N-C SP HEAT	S	.242193	.243067	.243067	.242888	.243067	.243067	.243067	.0	.0
9-N-C NOL HT	S	29.0517	28.8480	29.8460	28.8480	28.8480	28.8480	28.8480	.0	.0
10-OXYGEN FLOW I	.0	.0	15.2072	15.2072	15.2078	15.2072	15.2072	15.2072	.0	.0
11-DILUENT FLOW D	.0	.0	51.0136	51.0136	51.0154	51.0136	51.0136	51.0136	.0	.0
12-CO2 FLOW E	.0	.0	.660405E-01	.660405E-01	.344159	.660405E-01	.660405E-01	.660405E-01	.0	.0
13-TRACE CTH FLOW	D	.0	.0	.0	.0	.0	.0	.0	.0	.0
14-SFCL FLOW 1	D	.0	.0	.0	.0	.0	.0	.0	.0	.0
15-SFCL FLOW 2	A	.0	.0	.0	.0	.0	.0	.0	.0	.0
16-SFCL FLOW 3	T	.0	.0	.0	.0	.0	.0	.0	.0	.0
17-SFCL FLOW 4	A	.0	.0	.0	.0	.0	.0	.0	.0	.0
19-SFCL FLOW 5	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
19-SFCL FLOW 6	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
20-TOTAL SEC FLOW S	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
21-TEMPERATURE E	157.310	.0	.0	.0	.0	.0	.0	.0	.0	.0
22-DUCT OUTLET P C	28.4045	.0	.0	.0	.0	.0	.0	.0	.0	.0
23-COMP OUTLET P O	28.4045	.0	.0	.0	.0	.0	.0	.0	.0	.0
24-NON-CO2 FLOW N	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
25-CO2 VAP FLOW D	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
26-CO2 LIQ FLOW A	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
27-N-C SP HEAT	R	.200128	.0	.0	.0	.0	.0	.0	.0	.0
28-N-C NOL HT	Y	43.9413	.0	.0	.0	.0	.0	.0	.0	.0
29-OXYGEN FLOW	S	.0	.0	.0	.0	.0	.0	.0	.0	.0
30-DILUENT FLOW S	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
31-CO2 FLOW I	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
32-TRACE CTH FLOW I	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
33-SFCL FLOW 1 E	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
34-SFCL FLOW 2	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
35-SFCL FLOW 3	D	.0	.0	.0	.0	.0	.0	.0	.0	.0
36-SFCL FLOW 4	A	.0	.0	.0	.0	.0	.0	.0	.0	.0
37-SFCL FLOW 5	T	.0	.0	.0	.0	.0	.0	.0	.0	.0
39-SFCL FLOW 6	A	.0	.0	.0	.0	.0	.0	.0	.0	.0
39-DH, C, DP	PRI P	.0	.0	.0	.0	.0	.0	.0	.0	.0
40-LE, N, K	DUCT R	.0	.0	.0	.0	.0	.0	.0	.0	.0
41-FF AREA	E	.0	.0	.0	.0	.0	.0	.0	.0	.0
42-DH, C, DP	PRI S	.0	.0	.0	.0	.0	.0	.0	.0	.0
43-LE, N, K	COMP S	.0	.0	.0	.0	.0	.0	.0	.0	.0
44-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
45-DH, C, DP	SEC C	.0	.0	.0	.0	.0	.0	.0	.0	.0
46-LE, N, K	DUCT O	.0	.0	.0	.0	.0	.0	.0	.0	.0
47-FF AREA	E	.0	.0	.0	.0	.0	.0	.0	.0	.0
48-DH, C, DP	SEC F	.0	.0	.0	.0	.0	.0	.0	.0	.0
49-LE, N, K	COMP F	.0	.0	.0	.0	.0	.0	.0	.0	.0
50-FF AREA	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0
51-COMP SOURCE TEMP	.0	.0	.0	.0	.0	.0	.0	.0	.0	.0



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VRI (24, 65) = .0 VRI

COMPONENT NO. = SEQR. TYPE =	17 SPLIT	18 GASHIX	19 FAN	20 GASHIX	21 IR45	22 SPLIT	23 GASHIX	24 SPLIT
KR 1-SUCR NO./EXV/EXK	10000000	60000000	23000000	60000000	73000000	10000000	60000000	10000000
2-PRI SOR/FLO CODE	1602	1702	1802	-1402	2002	2102	-2202	2302
3-PRI SFPL TYP 1-3	0	0	0	0	0	0	0	0
4-PRI SFPL TYP 4-6	0	0	0	0	0	0	1700	2
5-SEC SOR/FLO CODE	2	-2200	0	2600	0	2	0	0
6-SEC SFPL TYP 1-3	0	0	0	0	0	0	0	0
7-SEC SFPL TYP 4-6	0	0	0	0	0	0	0	0
8-HEMT COMP/CABIN	2000002	1900002	3000002	2100002	2200002	2300002	2400002	1800002
9-COMP NSTR 1-9	0	0	3000000	20000000	0	0	0	0
10-COMP NSTR 10-18	0	0	0	0	0	0	0	0
11-NGFL/HLFL/HPASS	5760	5760	5760	5760	5760	5760	5760	5760
12-PRI VISC/DENSITY	0	0	0	0	0	0	0	0
13-PRI OP/DP/OP/DP	0	0	0	0	0	0	0	0
14-SEC VISC/DENSITY	0	0	0	0	0	0	0	0
15-SEC OP/DP/OP/DP	0	0	0	0	0	0	0	0

SUBROUTINE DEPENDENT K ARRAY DATA - - -

KR(19, 16) = 0 KR(19, 17) = 0 KR(19, 18) = 0 KR(21, 16) = 0 KR(21, 17) = 16
 KR(21, 18) = 0 KR(21, 19) = 5 KR(21, 20) = 20 KR(21, 21) = 0



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52-EFF SURFED COND .0
53-COOP QIOTOL LOSS .0
54-ADJACENT GAS TEMP .0
55-ADJACENT UA .0
56-ADJ COHV Q LOSS .0
57-ADJ HALL TEMP .0
58-MID SCRIPTIFMA .0
59-ADJ RAD Q LOSS .0
60-STRUCTURE TEMP .0
61-STRUCTURE KA/X .0
62-STRUCTURE Q LOSS .0
63-INSULATION TEMP .0
64-INSULATION KA/X .0

SHEROUTINE DEPENDENT V ARRAY DATA - -

VR(25, 65)=	247.83	VR(26, 65)=	.0	VR(27, 65)=	.0	VR(27, 66)=	.0	VR(27, 67)=	.0
VR(27, 68)=	168.30	VR(27, 69)=	146.21	VR(27, 70)=	70.000	VR(27, 71)=	2.6971	VR(27, 72)=	28.817
VR(27, 73)=	.0	VR(27, 74)=	.0	VR(27, 75)=	.0	VR(27, 76)=	.0	VR(27, 77)=	.0
VR(27, 78)=	.0	VR(27, 79)=	.0	VR(27, 80)=	.0	VR(27, 81)=	.0	VR(27, 82)=	.0
VR(27, 83)=	.0	VR(27, 84)=	.0	VR(27, 85)=	.0	VR(27, 86)=	.0	VR(27, 87)=	.0
VR(27, 89)=	1.0000	VR(27, 89)=	62.400	VR(27, 90)=	2.4200	VR(27, 91)=	18.016	VR(27, 92)=	.0
VR(27, 93)=	.0	VR(27, 94)=	.0	VR(27, 95)=	.0	VR(27, 96)=	.0	VR(27, 97)=	-1.7270
VR(27, 98)=	22.061	VR(27, 98)=	38.213	VR(27, 100)=	1.7270	VR(28, 65)=	34.130	VR(28, 66)=	.0
VR(28, 67)=	.0	VR(28, 68)=	.0	VR(28, 69)=	.0	VR(28, 70)=	.0	VR(28, 71)=	.0
VR(28, 72)=	.0	VR(28, 73)=	.0	VR(28, 74)=	.0	VR(28, 75)=	.0	VR(28, 76)=	.0
VR(28, 77)=	.0	VR(28, 78)=	.0	VR(28, 79)=	1.0000	VR(28, 80)=	.0	VR(28, 81)=	.0
VR(28, 82)=	.0	VR(28, 83)=	.0	VR(28, 84)=	.0	VR(28, 85)=	.0	VR(29, 65)=	.0
VR(29, 66)=	40.000	VR(29, 67)=	247.83	VR(29, 68)=	572.75	VR(29, 69)=	.0	VR(29, 70)=	.0
VR(30, 65)=	.0	VR(31, 65)=	51.448	VR(32, 65)=	.0	VR(32, 66)=	.0	VR(32, 67)=	.0
VR(32, 73)=	.25242	VR(32, 69)=	.32559	VR(32, 70)=	70.000	VR(32, 71)=	2.0000	VR(32, 72)=	28.592
VR(32, 78)=	.50143E-02	VR(32, 74)=	.73079E-01	VR(32, 75)=	.93537E-04	VR(32, 76)=	.20373	VR(32, 77)=	42.092
VR(32, 83)=	.0	VR(32, 79)=	.16849E-01	VR(32, 80)=	.23055	VR(32, 81)=	.0	VR(32, 82)=	.0
VR(32, 89)=	.25812	VR(32, 84)=	.0	VR(32, 85)=	.0	VR(32, 86)=	.0	VR(32, 87)=	.0
VR(32, 93)=	.0	VR(32, 89)=	.16409	VR(32, 90)=	.44000	VR(32, 91)=	32.377	VR(32, 92)=	.0
		VR(32, 94)=	.0	VR(32, 95)=	.0			VR(32, 97)=	-27500

COMPONENT NO. = SUBR. TYPE =	25 GASHIX	26 SPLIT	27 TANKG	28 PUMP	29 SHGEN	30 SPLIT	31 GASHIX	32 TANKG
NR 1-SUBR NO./EXY/EXX	6000000	10000000	30003000	22000000	27000000	10000000	60000000	30000001
2-PRI SOR/FLO CODE	2902	2502	0	2700	2802	2402	302	3002
3-PRI SPFL TYP 1-3	0	0	10000	10000	0	0	0	0
4-PRI SPFL TYP 4-6	0	0	0	0	0	0	0	0
5-SEC SOR/FLO CODE	2400	2	0	0	0	2	-1900	0
6-SEC SPFL TYP 1-3	0	0	0	0	0	0	0	0
7-SEC SPFL TYP 4-6	0	0	0	0	0	0	0	0
8-NEXT COMP/CABIN	2600002	1500002	2800002	2900002	2500002	3200002	700002	3100002
9-COMP NSTR 1-9	0	0	110100000	200000	10000000	0	0	10000000
10-COMP NSTR 10-18	0	0	0	0	0	0	0	0
11-HEFL/NLFI/NPASS	5760	5760	5760	5760	5760	5760	5760	5760



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IDM CLOCK TIME(HH-MM-SS) = 16:03:25

C-3



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INPUT CARD IMAGES LISTED BELOW

ICUT = 0 IPRT = 0
E:DR



Appendix D

Sample Plots



The following plots in this Appendix were obtained from the data generated by the sample problem of Appendix C. The Hamilton Standard MERIAM program was used to generate a tape for use on the CALCOMP plotter. The procedure described in Section 4.3 was used with the plotting files shown in Appendix B.

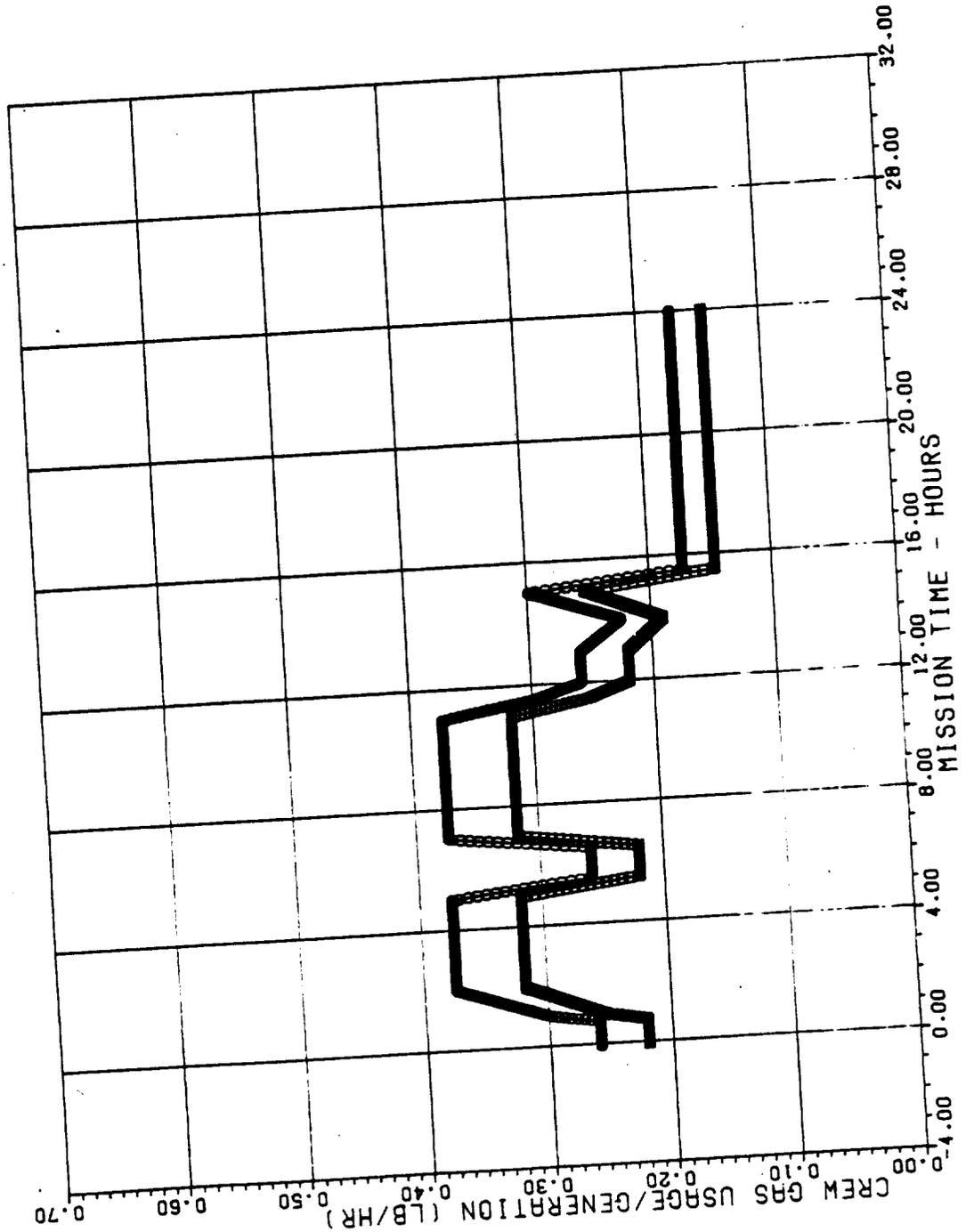


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- O2 USE RATE
- CO2 GENERATION RATE

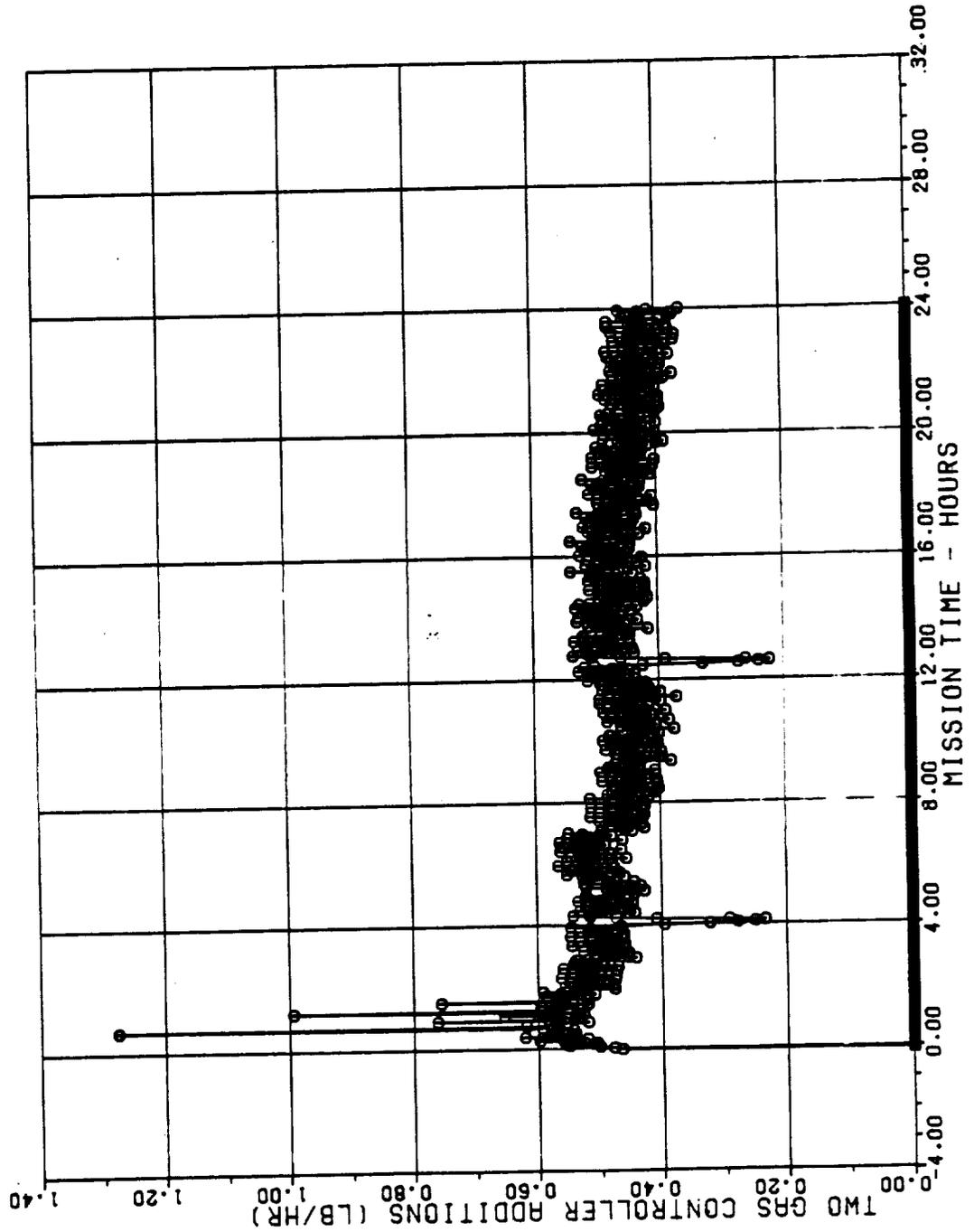
ESCM DEMONSTRATION. VOL = 8000. K = 1.5





■ NITROGEN MAKEUP
● OXYGEN MAKEUP

ESCH DEMONSTRATION. VOL = 8000, K = 1.5

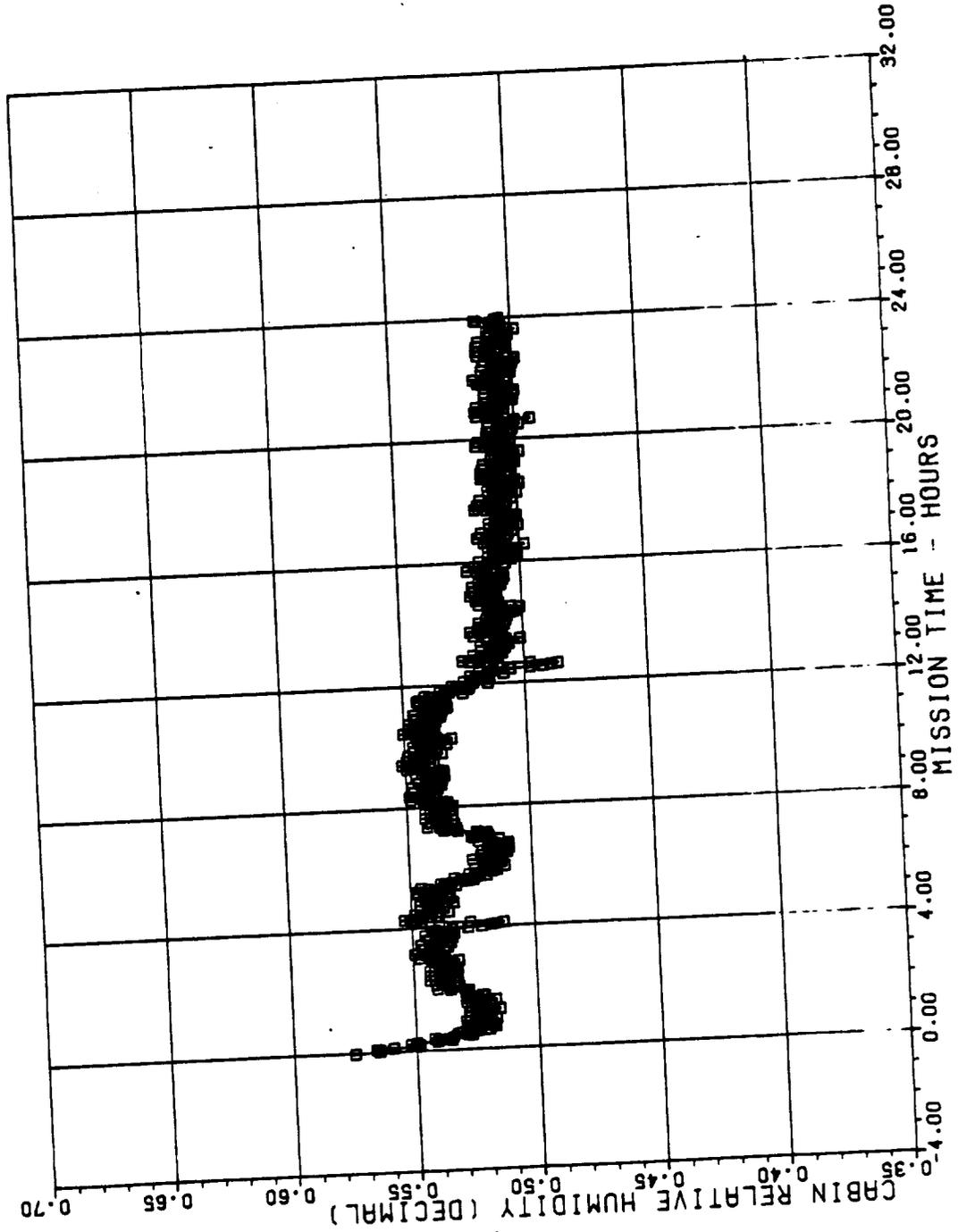




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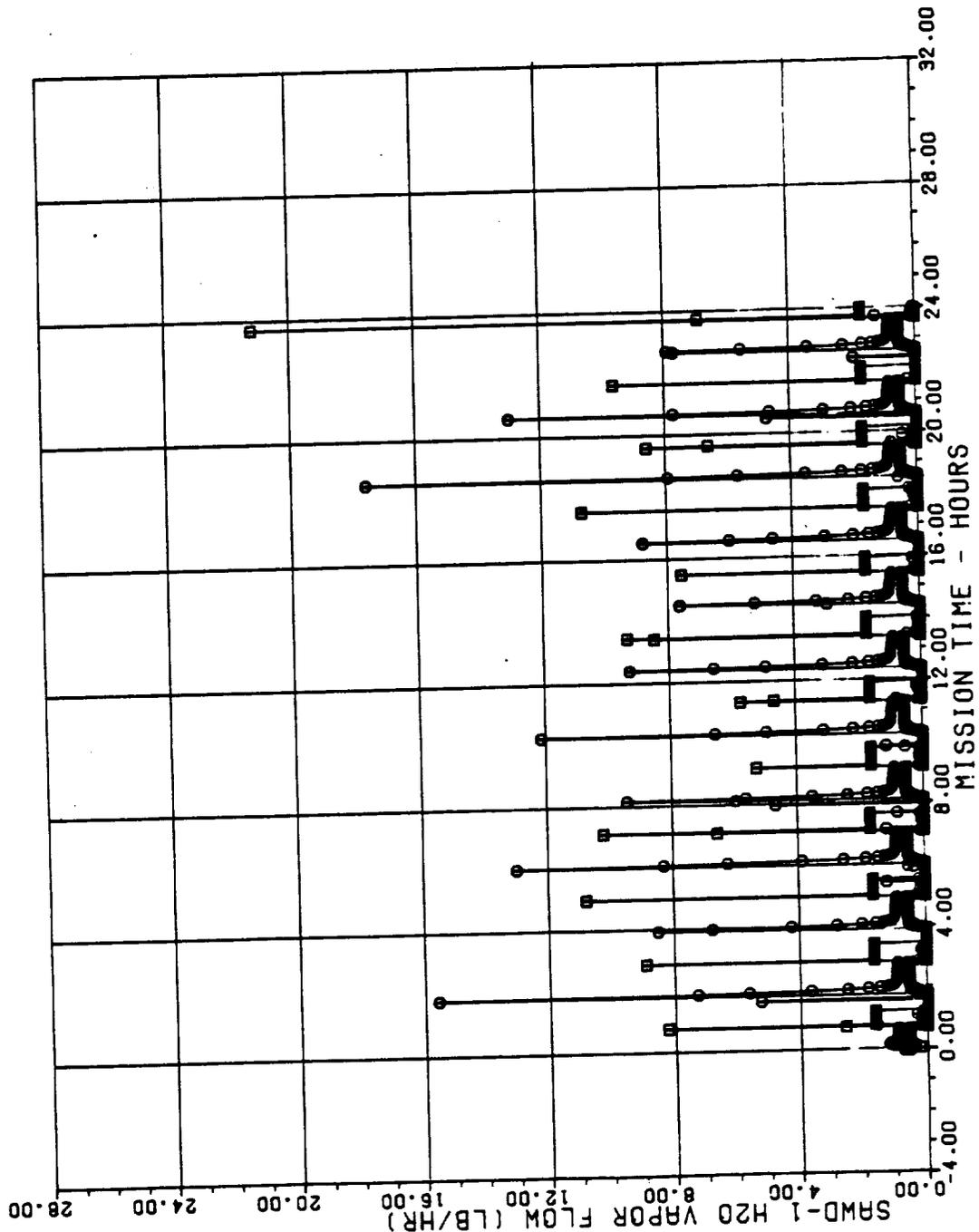
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ESCM DEMONSTRATION. VOL = 8000. K = 1.5



■ INLET H2O VAPOR
 ● EXIT H2O VAPOR

ESCM DEMONSTRATION, VOL = 8000. K = 1.5

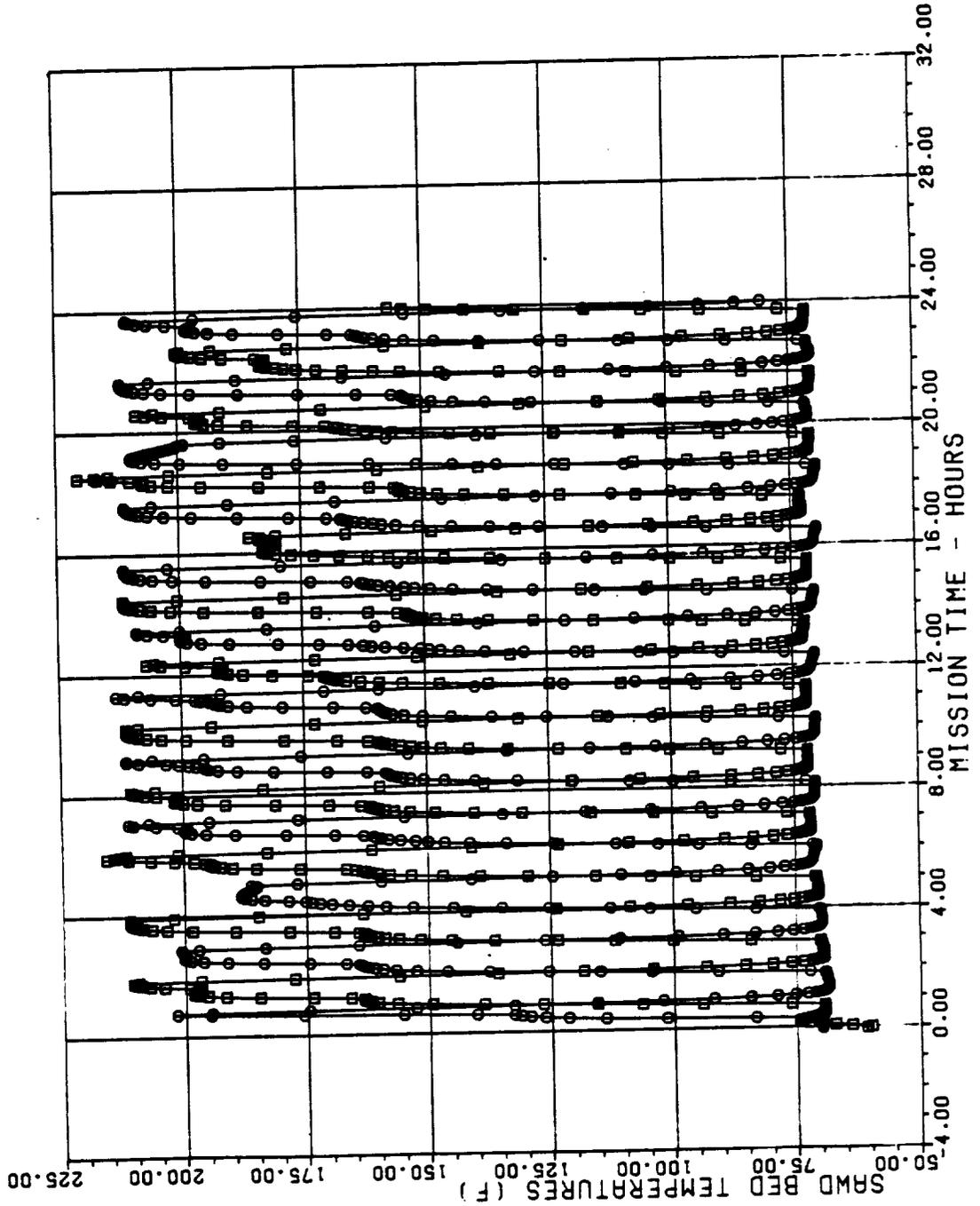




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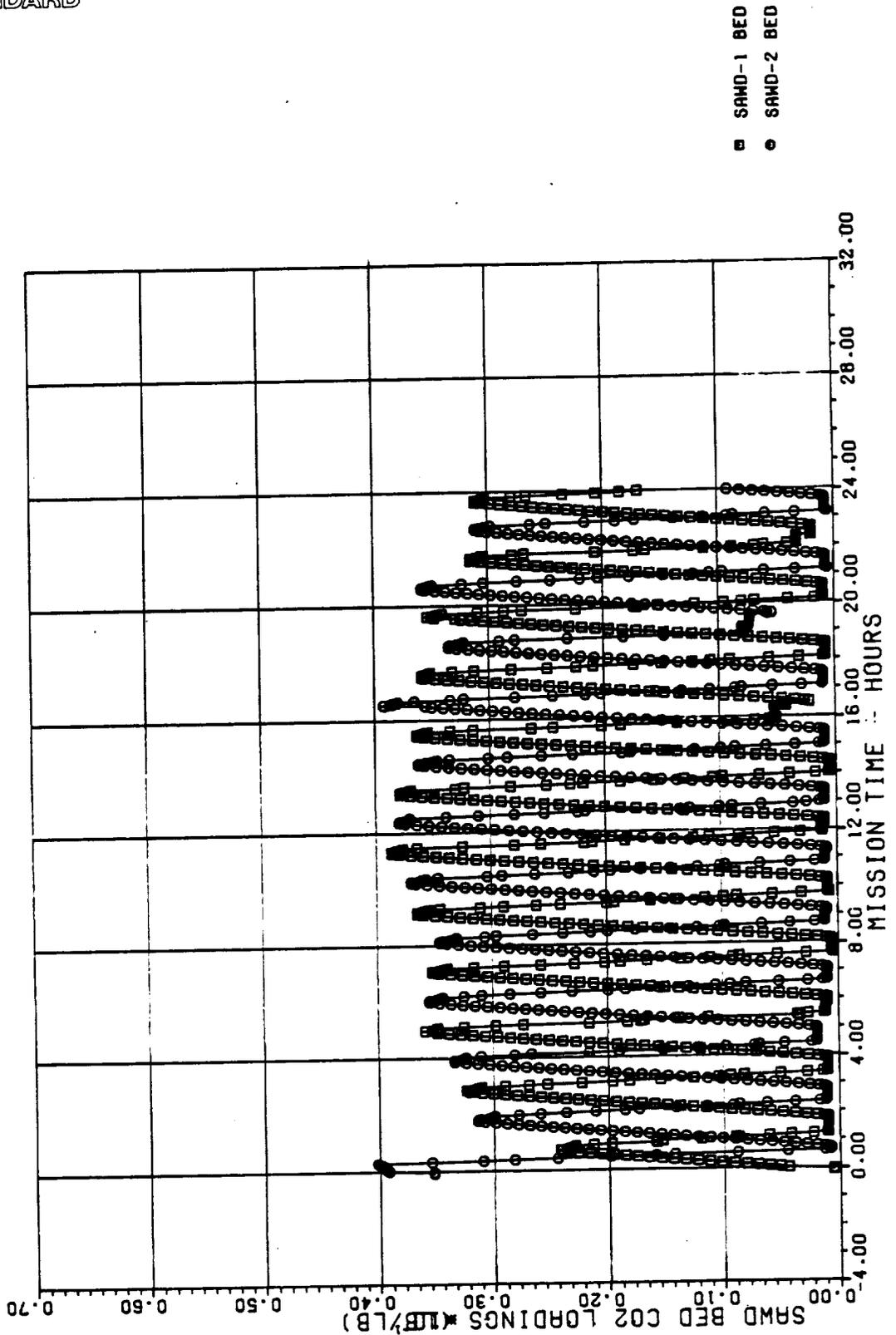
■ SAND-1 BED
● SAND-2 BED

ESCM DEMONSTRATION. VOL = 8000. K = 1.5

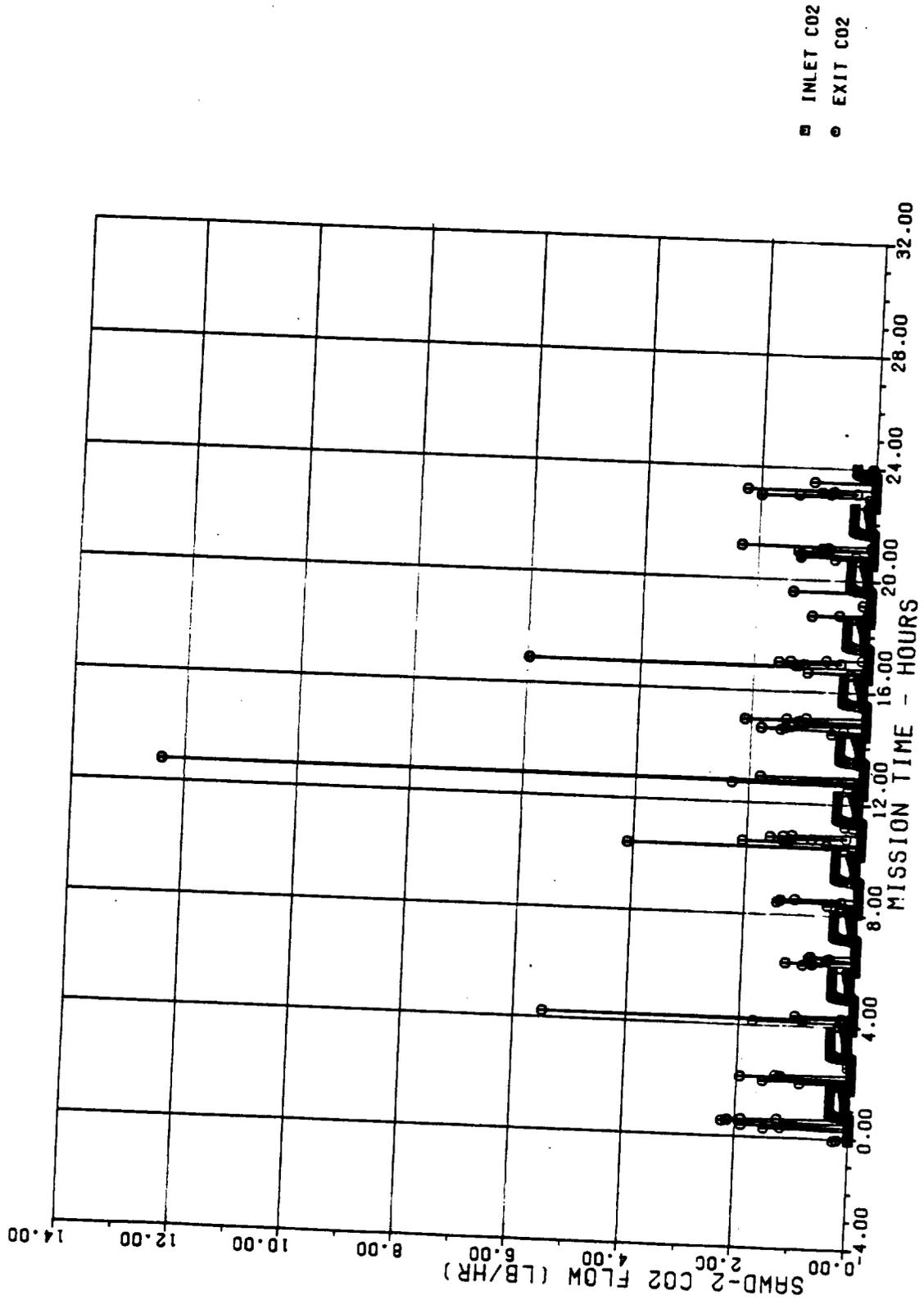




ESCM DEMONSTRATION. VOL = 8000, K = 1.5



ESCM DEMONSTRATION, VOL = 8000, K = 1.5





Report Documentation Page

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16. Abstract This manual describes how to use the Emulation/Simulation Computer Model, ESCM. Based on G189A, ESCM computes the transient performance of a Space Station atmospheric revitalization subsystem (ARS) with CO ₂ removal provided by a solid amine water desorbed subsystem called SAWD. Many performance parameters are computed some of which are cabin CO ₂ partial pressure, relative humidity, temperature, O ₂ partial pressure, and dew point. The program allows the user to simulate various possible combinations of man loading, metabolic profiles, cabin volumes and certain hypothesized failures that could occur.			
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